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# NITROGEN TETROXIDE FLOW DECAY STUDY

## FOR THE ORBITAL WORKSHOP PROPULSION SYSTEM

CASE FILE COPY

**CONTRACT NAS 8-21489** 

FINAL REPORT 12243-6002-R000

**JUNE 1969** 

#### PREPARED FOR

NATIONAL AERONAUTICS AND SPACE ADMINISTRATION

GEORGE C. MARSHALL SPACE FLIGHT CENTER

ALABAMA 35812





ONE SPACE PARK . REDONDO BEACH . CALIFORNIA

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#### **FOREWORD**

This report was prepared by TRW Systems Group, Redondo Beach, California, and describes the results of a nitrogen tetroxide flow decay study performed on the Orbital Workshop Propulsion System. The work described was accomplished between December 26, 1968 and May 26, 1969 for the George C. Marshall Space Flight Center, Huntsville, Alabama. The NASA technical manager was Mr. Keith Coates.

The work performed on the program was accomplished by TRW Systems Group, Science and Technology Division. Mr. M. J. Makowski of the Applied Research Section of the Applied Technology Department was the program manager. The technical efforts provided by several TRW Systems Group personnel are acknowledged:

Mr. C. Armstrong	Applied Technology Department, Technology Laboratory
Dr. E. Burns	Chemistry & Chemical Engineering Department, Science and Technology Division
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Mr. J. Reger	Materials Science Department, Physical Research Center
Mr. D. Wells	Chemistry & Chemical Engineering Department, Science and Technology Division

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#### ABSTRACT

This report describes the results of a flow decay study performed on the  $N_2O_4$  feed lines, valves, and filters of the Orbital Workshop Propulsion System. The system was exposed to off limit (high and low) environmental temperatures during the course of the flow experiments. Additional efforts were directed toward the effect of oxidizer compatibility with the braze alloy planned for system assembly, and upon the effects of artificial propellant aging.

Engine flow variations did not exceed 10 percent when operating between 90°F and 50°F using specification grade nitrogen tetroxide, and 12 percent when using artificially aged propellant. Isolation valve variations did not exceed 9 percent when operating between 90°F and 50°F using specification grade and 7 percent when using artificially aged nitrogen tetroxide.

Engine flow decay did not exceed 10 percent when operating between 90°F and 50°F using specification grade nitrogen tetroxide, and 5 percent when using artificially aged propellant. Isolation valve flow decay did not exceed 4 percent when operating between 90°F and 50°F using specification grade nitrogen tetroxide, and 5 percent when using artificially aged propellant.

Of the twenty-seven runs performed with the feed tank and test system between 90°F and 50°F, eight runs exhibited engine flow decays greater than 2 percent, and ten runs exhibited isolation valve flow decays greater than 2 percent.

These results cannot be indiscriminately applied to other systems or other operating conditions as significant differences in flow decay characteristics due to geometry or service environment could occur.

Several potential flow decay problem solution concepts are presented, however, no completely reliable method of flow decay control is presently available.

Recommendations are made for further flow decay related testing of the OWPS.

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#### 1.0 INTRODUCTION

This report presents the results of a Flow Decay Study for the Orbital Workshop Propulsion System sponsored by the NASA George C. Marshall Space Flight Center. The presentation includes a description of the test apparatus and test procedure, as well as test data and results of chemical analysis and compatibility studies performed. Conclusions, recommended problem solutions and recommendations for further work are presented.

#### 1.1 BACKGROUND

Flow decay and flow stoppage have occurred in nitrogen tetroxide (NTO) flow systems containing fine filters and small clearances. This flow degradation has been investigated by TRW Systems under NASA Contracts NAS 7-107 and NAS 7-549. The clogging mechanism has been postulated to be the solvation, coagulation and final precipitation of complex iron colloids from the solution with eventual drying of the gel resulting in a crystalline powder-like residue. The phenomenon appears as an increase in NTO viscosity in high velocity flow and seems to occur in areas of turbulence and constriction such as entrances to valves, filters, orifices and capillaries. Flow blockage was observed in both capillary and filter flow tests using MSC-PPD-2A NTO as well as propellant doped with metal ions likely to be found in an aged system. The blockage was caused by a gel-like material found at the entrance to the capillary and filter which dried to a powdery crystalline residue. Changes in propellant temperature appear to be an important factor in inducing the flow decay process. The clogging material has been analyzed and found to contain iron complexes resulting from reactions between NTO, soluble impurities, and ferrous alloys used in constructing the system. Organic material has also been detected, which may synergistically contribute to the flow decay phenomenon. These analyses were performed utilizing infrared spectrometric, X-ray fluorescence and atomic absorption techniques.

The NTO flow decay phenomenon has been observed by other investigators at Rocketdyne, NASA, Aerospace, and McDonnell Douglas. Publications relating to this problem are found in References 1 through 6.

Flow decay in NTO systems may be caused by gel formation, formation of solids, static accumulation of corrosion products and gas saturation of the propellant.

TRW Systems Group has demonstrated flow decay due to gel formation under Contract NAS 7-549 (References 2 and 9). The gel is postulated to form from a colloidal solution brought about by physico-mechanical means (References 7, 8, 9). Particles in colloidal dispersions (0.001 micron to 0.1 micron) are larger than most molecules in solution but not large enough to settle out because of gravity, or be seen with a conventional microscope. These colloidal particles can become solvated, and form gelatinous precipitates. In the process of going from a colloidal particle to a solvated precipitable particle, the diameter may increase on the order of a thousand times or more, and may be capable of being filtered or clogging small clearances. It is readily apparent that such a process can have profound effects on the rheological properties of the propellant.

Solids have been found to form in NTO flow systems during studies performed by Rocketdyne (Reference 4). In these flow tests solids were observed to be deposited on a valve pintle during a flow run.

Corrosion products are formed due to NTO interaction with the storage tank and flow system materials. When system temperatures are reduced these dissolved contaminants precipitate out of solution. An increase in system temperature causes further interaction with system materials resaturating the solution. Thus, temperature cycling causes an accumulation of solid corrosion products in the system which could clog filters, orifices and capillaries. In addition to the effects of temperature cycling, high static temperatures have been shown to cause substantial growth of a gelatinous material when  $N_2O_4$  is exposed to stainless steels and other nickel bearing alloys (Reference 10).

Nitrogen saturation of NTO may cause flow decay (Reference 10), however, this mechanism is beyond the scope of this program and was not considered further; therefore, precautions were taken to minimize NTO gas saturation during the flow runs.

TRW Systems has identified and isolated the NTO flow decay phenomena on two NASA programs, NAS 7-107 and NAS 7-549, and is currently engaged in further work in this area. It is felt that flow tests of actual systems, valves, and components, as performed during this study, are a logical extension of previous and existing programs.

#### 1.2 PROGRAM APPROACH

Prior to this program, flow decay investigations were performed on components and test sections simulating components, rather than on complete systems. This test program was undertaken to systematically test an entire propellant feed system over a range of temperatures in order to identify those conditions which could cause flow degradation. Thus, while the actual interaction of system components, in a flow decay sense, might not be fully understood the possibility of flow decay in the full operating system might be assessed. In order to identify which part of the system was the major contributor to overall system flow degradation, all system components were instrumented to provide temperature, differential pressure and flow information. Temperature conditioning and data taking were automated as much as possible to minimize the chance of error.

The data was processed to eliminate as many variables as possible from consideration before being examined for flow decay trends. As much of the basic and processed data as possible has been presented in this report to allow independent assessment of the results obtained. Both equivalent area and percent corrected flow presentations are utilized for the convenience of the user.

Chemical analyses were applied to the propellant at every stage of testing and these results are likewise presented as fully as possible to allow independent evaluation.

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#### 2.0 ORBITAL WORKSHOP PROPULSION SYSTEM EXPERIMENTAL APPARATUS

The test apparatus used on the program consisted of the government furnished Orbital Workshop Propulsion System (OWPS) components assembled on a holding fixture, the test instrumentation, the propellant feed and catch systems, and the system environmental temperature control box.

The OWPS, as supplied, consisted of two Marquardt Model R-IE-002, 22 pound thrust rocket engines, a dual redundant isolation valve assembly per Marquardt drawing 231350, two 15 micron absolute Wintec filters, NASA Part No. SK 20-4612, and connecting manifolds as described in NASA MSFC drawing No. SK 20-4458. The engines are more fully described in Marquardt Report MIR No. 272, which is summarized in Appendix I.

The above components were assembled to a supporting frame as described in NASA drawing No. SK 20-4458. The system, as installed in the environmental box for test, is shown in Figure 2-1. The test instrumentation was assembled into the OWPS and consisted of a differential pressure transducer across each system valve and filter, thermocouples at each system component inlet and outlet, and a system pressure transducer mounted to the engine feed manifold. In addition to the instrumentation mounted on the OWPS itself, pressure transducers were mounted to the feed and catch tanks, thermocouples were attached to the surface of the feed tank, and a thermocouple probe was inserted into the bulk propellant. Instrumentation location and type is detailed in the schematic diagram of the test setup, Figure 2-2. The instrumentation used is listed in Appendix II. Instrumentation accuracies and data reduction uncertainties are presented in Sections 3.3.1 and 4.1.1, respectively.

The propellant feed system consisted of a 60 gallon stainless steel tank with provision for regulated pressurization and for heating and cooling the NTO for temperature conditioning. Heating was accomplished through the use of electrical strip heaters bonded to the tank's surface and cooling was provided by injecting cold nitrogen gas from a liquid nitrogen vessel between

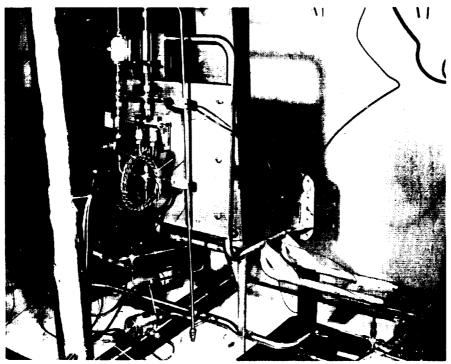


Figure 2-1a. Installed Test Hardware

Figure 2-la. Installed Test Hardware

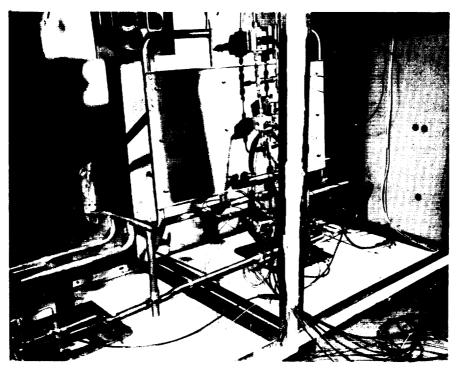
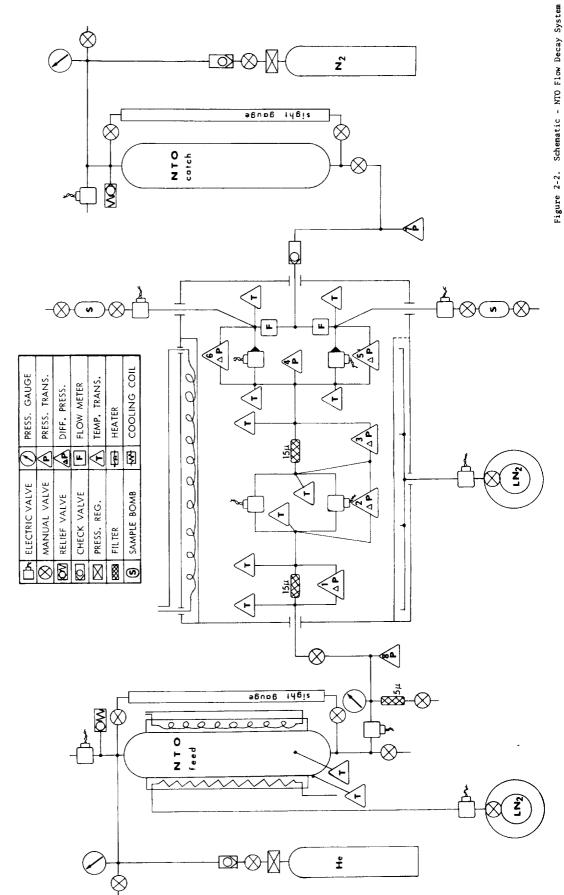


Figure 2-1b. Installed Test Hardware

Figure 2-1b. Installed Test Hardware



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a cooling shroud and the tank. Figure 2-3 shows the general test cell arrangement and the feed tank with the cooling shroud in place before the shroud was insulated with spun fiberglass insulation. A high temperature "thermal blanket" type insulation was used over the heaters separating them from the cooling shroud. The nitrogen cooling gas was flowed through the passages formed between the heaters and insulation, and was enclosed by the cooling shroud. A cross-section of the arrangement is shown in Figure 2-4.

The propellant catch system consisted of a stainless steel tank identical to the feed tank but without heating and cooling provisions. Pressurization and vent provisions were made to allow maintaining the catch tank at a predetermined pressure to simulate engine chamber pressure.

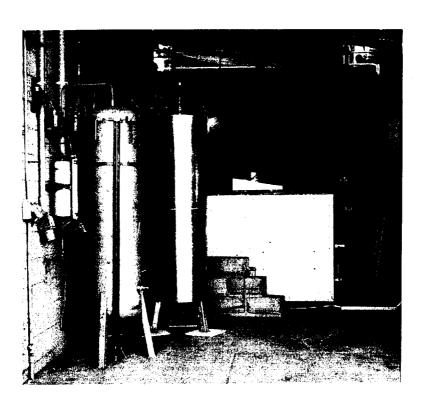


Figure 2-3. Test Cell

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The environmental temperature control box was an insulated chamber provided with electrical heating and cold nitrogen cooling.

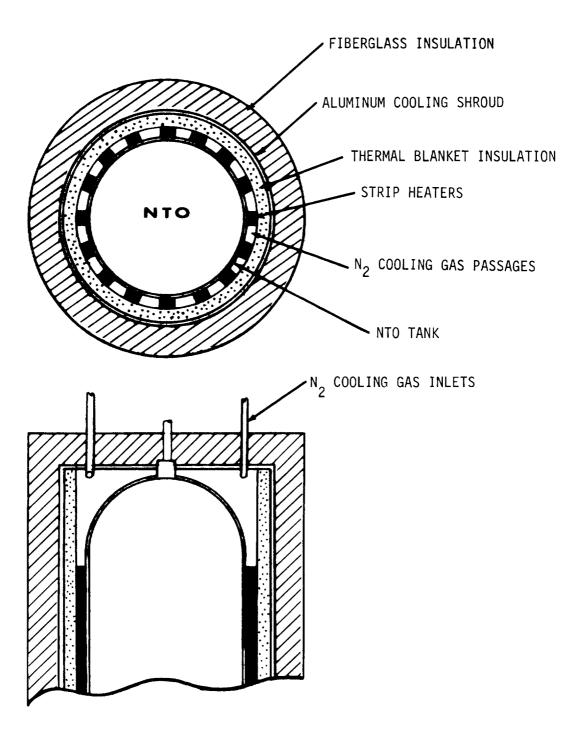


Figure 2-4. Propellant Feed Tank Heat and Cooling Configuration

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## 3.0 ORBITAL WORKSHOP PROPULSION SYSTEM EXPERIMENTAL PROCEDURE

The experimental procedure was designed to maximize the amount of data collected while minimizing the number of runs required. The basic procedure followed is described in the Test Plan and Procedure presented as Appendix II.

#### 3.1 FLOW TEST PROCEDURE

The testing proceeded as follows: The system feed tank was filled with NTO per MSC-PPD-2 and a sample was drawn for chemical analysis. The feed tank was temperature conditioned to the propellant temperature planned for the next test run and the system conditioned to its test temperature. After the required temperature conditions were well stabilized, the feed tank and catch tank pressures were established and the pressure transducer calibrations checked. Helium was used as the pressurant and the feed tank was vented to NTO vapor pressure following each run sequence to prevent NTO gas saturation. The isolation valves were then opened and a few seconds later the engine valves were opened on a steady state or pulsed basis for the required run duration. During the run, differential pressure recordings were made across each valve and filter, the flow rates from each engine were recorded, propellant temperatures at the inlet and outlet of each component were recorded, and feed tank, system, and catch tank pressures were monitored and recorded.

There was no attempt made to maintain a feed tank to system temperature difference during a flow run. Once the appropriate initial temperature differences had been established, the system was allowed to follow the incoming propellant temperature controlled only by its own thermal inertia. This was felt to more closely simulate the anticipated system thermal environment than would a constant temperature gradient.

Temperature conditioning of the propellant was accomplished by applying electrical power to the heaters or cold nitrogen gas from a liquid nitrogen cylinder to the feed tank as described in Section 2.0. Temperature conditioning of the system was accomplished by applying electrical power to the environmental box heaters or injecting cold nitrogen gas, from a liquid nitrogen cylinder, into the box. The feed tank and box heating/cooling

arrangements were controlled by a pair of automatic recording controller units to allow unattended operation.

Electrical valves were plumbed to the system just downstream of each engine to allow sample taking during a flow run. Samples were routinely taken during the first run at each temperature condition, or if any flow anomalies were observed during the run. The sample bottles were normally purged with filtered gaseous nitrogen to eliminate oxygen which could give a false low NO reading due to oxidation of some NO to NO<sub>2</sub>.

After each run the data was reduced at several points along the continuously recorded data tapes and computer processed to correct for the effects of pressure and temperature.

#### 3.2 FLOW TEST SEQUENCE

The test matrix performed during this study is presented in Table 3-1. The test conditions were revised from those originally planned and presented in Table 1 of Appendix II due to observed occurrences of flow decay during the initial test sequence. A revision in the test plan and sequence following the initial test series was necessary since flow decay was observed during the 150°F propellant to 12°F system test runs. All the temperatures listed are nominal, reading tolerances are listed in Section 3.3.1 and Appendix II, while actual test temperatures for each component are presented in Appendix V. Initially, both isolation valves were opened during a test run and separate runs were made with left engine, right engine and both engines. However, after the initial test series all test runs were made with both engines and after run 15, only one isolation valve was opened since it was indicated by NASA that this more closely reproduced the system's probable use mode. Both steady state and pulsed mode operation was employed during the flow tests. Flow tests at each temperature condition were performed on both a steady state followed by pulse run and pulse run followed by steady state basis. This was done to examine the possible interaction between steady state and pulsed operation. A three to four second steady state flow was employed at the beginning and every 60 seconds throughout most pulse runs to obtain stabilized flow and pressure data.

Table 3-1. Test Matrix

			Run	Nominal	Nominal	
	Engines (1)	Iso Valve(s)	Duration	Hold Tank	System	
Run	Used	Used	(sec)	Temp.°F	Temp. F	Propellant
		_				
1	Right	Both	1 <b>0</b> 70	150	150	Neat NTO
2	Right/Both	*1	1280	150	150	per MSC-
3	Left/Both	tt 	1105	150	75	1 -
4	Left	t1	600	150	75	PPD-2
5	Left	tt	600	150	12	
6	Right	11	600	150	12	
7	Both	**	600	150	12	
8	11	11	100(3)	58	58	
9	11	11	$\begin{array}{c} 100 \\ 620 \\ (2) \end{array}$	70	60	
10	11	11	480(2)	70	60	
11	(4)	-		-	-	_
12	*1	11	400(3)	70	50	
13	*1	11	600(2)	70	50	
14	11	11		90	50	
15	11	11	100(-)	90	50	}
16	''	Right	200 (2)	12	150	
17	*1	Left	700	12	150	
18	11	Right	570(2)	12	12	
19	11	Left	710(3)	12	12	
20	"	Right	ツノヘしーノ	90	90	
21	*1	Left	7/ハ しょり	90	90	
22	11	Right	7/0\~;	70	70	
23	11	Left	7/0(0)	70	70	
24	''	Right	<b>フとハ \ ~</b> ノ	50	50	
25	11	Left	$\frac{360}{360} \frac{(3)}{(3)}$	50	50	
26	11	Right	300(3)	30	30	
27	11	Left	360 <sup>(2)</sup>	30	30	
28	11	Both	81(2)	30	30	
29	11	Left	$\frac{81}{360}(2)$	90	70	
30	11	Right	360 (3)	90	70	
31	11	Left	360 (2) 360 (3)	90	50	
32	" '	Right	362(3) 362(3)	90	50	
33	"	Left	360 (2) 360 (3)	90	90	Artifici-
34	".	Right	360(3)	90	90	ally Aged
35	::	Left	360 (3) 360 (2) 362 (3)	70	70	
36	11	Right	362(3) 360(2)	70	70	NTO
37	::	Left	360 (2) 360 (3)	50	50	11
38	!!	Right	360(3)	50	50	11
39	<u>''</u>	Left	360(2)	90	70	11
40	''	Right	360 (2) 360 (3) 360 (2)	90	70 70	11
41	*1	Left	360 (2) 403 (2)	90	50	11
42	*1	Left	403 (-)	90	50	''

- (1) Nominal flow rate is .05 lb/sec with 1 engine, .10 lb/sec with both engines.
- (2) Run consisted of pulsed flow on a .06 sec on, 1.0 sec off cycle followed by steady state flow.
- (3) Run consisted of steady state flow followed by pulsed flow on a .06 sec on, 1.0 sec off cycle.
- (4) Run 11 consisted of four pulses for instrumentation checkout, and no data was taken.

#### 3.3 FLOW TEST DATA ACQUISITION

Instrumentation locations are shown on the test schematic, Figure 2-2. The parameters monitored include temperatures, flow, pressure, and differential pressures across all critical test system components. The instrumentation techniques included the recording of all critical parameters on the Leeds and Northrup, Type W strip chart recorder (15)\* or the Honeywell Visicorder (11). All temperatures and the feed tank and catch tank pressures were recorded on the strip chart recorder.

The temperature measurements were performed with copper constantan thermocouples with a  $150 \pm 0.2$ °F reference temperature provided by a Pace Reference Junction (16).

The temperature recording system was calibrated periodically with a thermocouple potentiometer to assure proper scale factor. The recorder scale was adjusted to indicate true temperature for operator convenience, but data reduction was performed with the thermoelectric voltage output to provide for the inherent non-linearities of thermocouples.

System component differential pressure measurements were performed with strain-gauge type transducers and signal conditioning units fed to the Visicorder. The engine flow measurements were performed with turbine type meters fed to a pulse rate converter, providing a D.C. voltage proportional to the flow rate. This voltage was also recorded on the Visicorder.

The feed tank and catch tank pressure recording system was calibrated prior to most runs by resistance-pressure ("R-Cal") equivalents to set scale span and zero. "R-Cal" equivalents were determined from transducer calibrations performed by the TRW Systems Group Metrology Laboratory.

Measurement accuracies for each instrument and overall reading are presented in Table 3-2.

<sup>\*</sup>Number in parenthesis indicates instrumentation list item number in Appendix II.

The above pressure and flow systems were calibrated with internal references immediately preceding each run to assure consistent scale factors. They were also periodically checked immediately following selected runs to monitor short term drifts, if any.

#### 3.3.1 Measurement Accuracy

Table 3-2 presents a tabulation of the uncertainties in temperature, pressure, and flow measurements on an absolute basis and the overall accuracy from run to run.

The "R-Cal" accuracy is a function of the calibration resistor tolerance and allows a constant systematic offset in pressure readout for any given resistor transducer pair.

The maximum within run measurement uncertainties are printed in Table 3-3. This measurement uncertainty is reduced considerably during steady state runs since the repeatability error of the instrumentation becomes negligible.

The uncertainties presented in Tables 3-2 and 3-3 were derived from data supplied by the TRW Metrology Department.

Table 3-2. System Measurement Accuracy Run to Run

Temperature	
Thermocouple	<u>+</u> 1.5°F
Recorder (± 3% of span, 220°F span)	+ 0.66°F
Reference Junction	+ 0.2°F
	+ 2.4°F
Pressure	
Transducer (linearity + repeatability)	<u>+</u> 0.5%
Recorder (resolution of $\pm$ 0.2 div, 65 div)	<u>+</u> 0.3%
R-Cal (accuracy of resistors used)	<u>+</u> 1.0%
	<u>+</u> 1.8%
Flow	
Flowmeter	<u>+</u> 0.2%
Rate Converter	<u>+</u> 0.2%
Recorder	± 0.3%
	<u>+</u> 0.7%

Table 3-3. System Measurement Accuracy Within a Single Run

Temperature	
Thermocouple	<u>+</u> 1.5°F
Recorder	<u>+</u> 0.66°F
Reference Junction	+ 0.2°F
	+ 2.4°F
Pressure	
Transducer (repeatability)	± 0.1%
Recorder	+ 0.3%
	+ 0.4%
F1ow	
Flowmeter	<u>+</u> 0.1%
Recorder	+ 0.3%
	+ 0.4%

#### 3.4 FLOW TEST CHEMISTRY SUPPORT

The primary function of the program was to observe flow anomalies in the OWPS within the temperature conditions expected in use. Routine specification propellant analyses as well as certain specific chemical analyses were performed to verify that any abnormal flow behavior would be attributable to the system/propellant interface rather than to propellant compositional anomalies alone.

Propellant samples were taken at each temperature set run and analyzed for nitric oxide assay and water equivalent. Non-routine tests such as particulate content, NTO assay, NO assay, chloride content, particle count, metals analysis, infrared analysis, X-ray fluorescence spectra, non volatile residue (NVR) analysis, and nitrate content were performed on selected samples if the run data indicated a spurious result or when fresh propellant was loaded into the run tank.

# 3.4.1 Analytic Techniques

The analytic techniques for NTO assay, nitric oxide assay, water equivalent, chloride content and particulate content were performed by the procedures outlined in the MSC-PPD-2A specification.

The oxidizer density was measured by weighing the NTO sample in a variable volume pycnometer. The particle size distribution test was adapted from standard particle sizing and counting techniques (References 11 and 12), where the sample is filtered through a cross gridded filter paper and the particles captured are counted under a microscope. The dissolved contaminant test for non-volatile residue (NVR) was conducted by the procedure described in the JPL/NASA Interim Report (Reference 2). This analysis is designed to determine the magnitude of dissolved materials which remain as a residue under conditions of 20 torr, and either 100°C (water solubles) or 60°C (acetone solubles). Although this procedure is not prescribed within any NTO specification, enough data has been accumulated within TRW Systems that it is felt there is a distinct possibility that observed flow anomalies may be attributable to a synergistic effect between the non-volatile contaminant and the postulated colloidal metal content of the propellant (Reference 9).

Dissolved metal content of the oxidizer was determined with a Perkin-Elmer Model 290 atomic absorption spectrometer. Aliquots of each sample (approximately 4 ml) were transferred to glass ampoules. These samples were hydrolyzed in a sulfuric acid-hydrogen peroxide solution which was then concentrated by evaporation and rediluted to a reference volume for analysis. In order to alleviate difficulties associated with transfer of propellant containing insoluble metal-containing species, the transfer was done utilizing a syringe fitted with a Millipore filter holder and a Teflon filter (LCWP-02500,  $10 \pm 2\mu$ ), except for samples Nos. 54, 59, 60 and 64, which were not filtered.

Infrared analyses utilized a Perkin-Elmer Model 521 grating infrared spectrophotometer. The spectra were obtained using either KBr pellet or thin film techniques.

X-ray fluorescence spectra were obtained with a General Electric Model XRD-5 X-ray spectrophotometer.

Nitrate content of aqueous solutions of contaminants were determined by the Brucine alkaloid spectrophotometric procedure.

## 3.4.2 Experimental Accuracies

Table 3-4 outlines the sensitivity and accuracy of the analytical techniques where applicable. Although the accuracy for atomic absorption analysis is normally quite good, no figures can be given for NTO analyses due to the inherent variations in the sampling and transfer techniques. This problem was emphasized by results from a round robin test on iron content determination by atomic absorption techniques where TRW Systems Group and other aerospace companies analyzed the same solutions of iron compounds at various concentration levels (Reference 13).

Table 3-4. Sensitivity and Accuracy of the Analytical Techniques for Nitrogen Tetroxide Analysis

Accuracy	Sensitivity (low detection limit)	Accuracy						
NO Content Water Equivalent Chloride Content Particulate Weight Density Non-Volatile Residue Metals Fe Cu Cr Ni Zn	0.5 mg/1 - 0.5 mg/1 0.1 ppm 0.2 ppm 0.2 ppm 0.2 ppm 0.2 ppm	+ 0.005% 1 + 0.005% 2 + 0.005% 1 + 0.005% 1 + 0.5 mg/1 + 0.0005 g/cc + 0.5 mg/1						
Mn Infrared Spectroscopy X-Ray Fluorescence Nitrate Content	0.1 ppm - - 10 ppm	qualitative analysis qualitative analysis qualitative analysis						

<sup>1</sup> Implied by the MSC-PPD-2A Specification Limits

<sup>2 + .05%</sup> Implied by MSC-PPD-2B Specification Limits.

#### 3.5 NITROGEN TETROXIDE AGING STUDIES PROCEDURE

The OWPS will be subjected to thermal cycling during its operating lifetime, therefore, an NTO aging study was performed in order to assess changes in NTO composition which might contribute to performance degradation. Four gallons of NTO, previously stored for approximately six months, were thermally cycled daily for two months between 150°F and 12°F. Chemical analysis of the NTO before cycling showed that it was in specification, with a nominal dissolved metals content. The container was a series 316 stainless steel tank, previously used for NTO storage. The NTO was analyzed after cycling to provide the basis for artificial aging.

### 3.6 NITROGEN TETROXIDE - BRAZE ALLOY COMPATIBILITY STUDY

A short term compatibility experiment was performed on the braze alloy planned for use in the assembly of the OWPS. Since the test system used in this study was welded and not brazed, it was felt that the test might indicate a potential problem which would not show up on the flow tests. The braze alloy was purchased from Western Gold and Platinum Company as a  $4" \times 1/2" \times 0.010"$  thick sheet, Nioro VPOF Grade Strip per ASTMB-260-62T Class Bau -4, Lot No. 12456. Lot certification analysis is shown in Table 3-5.

The test was carried out under the same conditions as the NTO aging study; samples of the braze alloy were placed in compatibility tubes, NTO added, and the tubes were thermally cycled between 12°F and 150°F on a once a day cycle for two months.

After the test was completed, the samples were removed from the compatibility tubes and the propellant and samples analyzed.

Table 3-5. Lot Certification Analysis of Braze Alloy Used in the Nitrogen Tetroxide Compatibility Study

<u>Metal</u>	Weight Percent
Gold	81.65
Nickel	18.35
Aluminum	<0.001
Copper	0.004
Lead	0.001
Magnesium	<0.001
Silver	0.008
Iron	0.001
Manganese	<0.001
Silicone	0.001
Palladium	<0.001
Calcium	<0.001

#### 4.0 EXPERIMENTAL RESULTS

Results are in four parts describing the flow test results, the chemical analyses, the braze alloy compatibility results, and the propellant aging results. Each of these contribute to an understanding of the overall system flow decay characteristics. The flow tests give a measure of actual system performance under simulated service conditions while the chemical analyses, compatibility and aging tests give an indication of potential problems due to variations in propellant composition, corrosion of system components, buildup of corrosion products, and possible propellant deterioration.

#### 4.1 FLOW TEST RESULTS

The results of flow testing the system over the expected use temperature range as indicated in the Test Matrix, Table 3-1, are summarized in the plots of percent corrected flow vs. time presented in Figures 4-1 through 4-40. More detailed data as to pressure drops, temperatures and actual flow for each component showing significant flow anomalies is presented in the plots of Appendix IV and the tabulations of Appendix V. The corrected flow values presented were obtained by calculating an equivalent flow area for each component based on the pressure drop, flow rate, and temperature at that location and then calculating the equivalent flow based on a standard pressure drop and temperature.

Both the corrected flow and equivalent area calculation were based on the relation:

$$Q = C_{d}^{A} \sqrt{2gh}$$
 (1)

where: Q = volumetric flow

g = acceleration due to gravity

h = head loss

A = area

C<sub>d</sub> = discharge coefficient - dimensionless taken as .6 in all calculations.

The above equation is just a special case of Bernoulli's equation:

$$\frac{1}{2g} \left( V_2^2 - V_1^2 \right) + \frac{P_2 - P_1}{\rho} + (H_2 - H_1) = 0$$
 (2)

where: V = flow velocity

P = pressure

 $\rho$  = weight density

H = head

g = acceleration due to gravity

and the subscripts 1 and 2 refer to the conditions at the inlet and outlet to the component.

Rearranging (1), the calculated flow area is:

$$A = \frac{Q}{C_d \sqrt{2gh}}$$
 (3)

where:

$$h = \frac{(P_1 - P_2)}{\rho} \tag{4}$$

The volumetric flow and propellant temperature were determined from the flow meter and thermocouple located downstream of each engine. This volumetric flow was converted to weight flow at the measured temperature according to the relation

$$w = Q \rho \tag{5}$$

where: w = weight flow.

By continuity the mass or weight flow in the system must be a constant and therefore this weight flow calculated from each flow meter was used in calculating the data for its corresponding engine, and the weight flows from the two flow paths were summed to obtain the total flow through the isolation valves and filters. Local volumetric flows were calculated for each component

from the mass flow using the density indicated by the inlet temperature to the component from equation (5) rearranged to read:

$$Q = \frac{w}{\rho} \tag{6}$$

These actual volumetric flows were used to calculate the equivalent flow areas for each component from equation (3).

Corrected flow data as presented in Appendix III was obtained by calculating volumetric flow from equation (1) and weight flow from equation (5) at a pressure drop of 120 psi for the engines, 8 psi for one isolation valve open, and 2 psi for two isolation valves open. The temperature was taken as 70°F in all corrected flow calculations. The values of pressure drop for the corrected flow calculations were selected from the engine data in Appendix I and the actual pressure drop data generated in system testing as presented in Appendix V.

It should be noted that the percent of "maximum corrected flow" data is numerically equal to percent of "maximum equivalent area" data thus giving an indication of percentage variation in flow and/or equivalent orifice size in the same plots. The actual corrected flows and equivalent areas for each condition may be calculated by multiplying the percent indicated by the maximum flow or the maximum equivalent area. The data used to prepare these plots including corrected flow data is presented in tabular form in Appendix III. The maximum flow and equivalent areas for the components showing significant flow variations during the test program are shown in Table 4-1.

The occurrences in which observed flows through a component or the system did not correspond to expected behavior for a normal liquid flow system have been classed as flow anomalies or flow variations and flow decays or flow degradations. Flow anomalies or variations include any abnormal flow behavior such as abrupt or gradual increases and decreases in flow or a combination of these over a flow run. Flow decays or degradations indicate a continuous flow decrease over a portion of a flow run as opposed to the more general case of the flow anomalie or variation.

Table 4-1

Component	Max. Equiv. Area (in <sup>2</sup> )	Max. Corrected Flow Lb/Sec	Max. Corrected Flow GPM	Run No.
Right Engine	1.310 x 10 <sup>-3</sup>	.0547	.272	19
Left Engine	$1.371 \times 10^{-3}$	.0572	.285	37
Both Isola- tion Valves	$19.75 \times 10^{-3}$	.106	.530	9
Right Isola- tion Valve	$10.59 \times 10^{-3}$	.114	.568	32
Left Isola- tion Valve	10.08 x 10 <sup>-3</sup>	.109	.541	37

It can be seen from examining Figures 4-1 through 4-40 that flow variations of up to 14.6 percent and 15.8 percent were experienced by the right and left engines, respectively. The isolation valves showed a 21.5 percent variation. The most serious case of flow decay occurred during run 7 for the engines and run 5 for the isolation valves (both open). The temperature conditions for runs 7 and 5 were a feed tank temperature of 150°F and a system temperature of 12°F. The right engine flowed slightly less than the left in most runs on an actual flow basis (see Appendices IV and V), however, it stayed above the left engine in a majority of runs on a percentage basis. This indicates an unequal susceptibility to flow degradation or decay for the two engines and a possible slight initial mismatch in equivalent orifice size. The left isolation valve showed a higher flow variation than the right, however, it was normally used during the steadystate followed by pulse runs, while the right isolation valve was used more frequently for the pulse followed by steady-state runs. The left isolation valve showed the greatest percent corrected flow degradation which was 8.6 percent and occurred during run 31. The right isolation valve exhibited maximum corrected flow degradation of 3.3 percent during run 32. Table 4-2 summarizes the occurrences of flow anomalies, and flow decay for each run. Temperature conditions and percent of maximum flows for each component are also included.

	Run Con			Stea	Stat	Flow			-	2	-	2	-	2	Puls	Steady	2,	-	2	-	2	-	2	-	-	2	Stei	2	1	2	~	1	2	-	2	-	2	-	2		2
	Propellant												31	ıeı		do	o I c	1 2	:-a	ldd	) )	SW	. ¥	'S¥	'N									8Å	λ	π	Бİ	ЭĮ	li li Iq	11	
	Lt Iso	ı	,	•	'	1	,	,	,	,	1	,	,	,	,	4.2	'	1.0	,	2.3	,	6.0	,	2.2	,	1.5	,	2.2	,	9.8	,	0.7	'	0.4	,	2.2	,	6.0	,	4.3	
w Decay	Rt Iso	,	'	,	1	,	,	,		•	,	,	,	3.2	2.0	,	1.6	,	0	,	1.8	ı	2.4	ı	1.0	1	'	,	1.4	1	3.3	•	1.5	1	1.4	ı	2.0	ı	0.5	1	1.6
Percent Flow	Both Iso	15.6	6.3	3.2	15.2	7.5	2.8	9.0	4.0	9.0	1,0	1.1	0.5	1	1	,	٠	,	1	,	'	'	,	ı	,	ı	6.7	1	1	1	ı	1	,	,	,	1	,		,	'	•
Max P	Lt Eng	2.6	6.2	5.8	11.3	,	15.8	0.4	0.3	0.1	0.4	0.4	2.0	2.3	2.5	1.2	9.0	9.0	1.9	0.1	0.7	9.0	2.0	0.5	2.1	0.5	0.7	1.9	1.8	9.7	4.0	0.4	0.4	0.2	0.3	4.3	3.2	0.2	0.5	0.3	8.0
	Rt Eng	,	1.2	1	1	3.6	5.9	0.3	1.8	0.1	0.7	1.4	2.7	0	4.6	5.1	2.2	3.4	0.1	1.2	1.0	9.0	1.6	0.7	1.1	4.1	0.3	3.3	0.5	2.0	2.2	0.4	6.0	8.0	1.2	0.2	6.0	9.0	0.5	2.2	6.0
	Lt Iso	,	1	•	ı	,		1	,	,	,	,	,	,	,	4.6	1	1.3	•	2.3	١	6.0	1	2.1	1	1.4	,	4.0	'	8.5		0.7	,	9.0	,	6.2	,	1.8	,	4.3	
iation	Rt Iso	•	,	ı	ı	(	ı	•	ı	1	,	ı	,	3.9	2.0	,	1.9	ı	1.0	,	1.8	,	2.5	,	1.0	,	,	,	9.5	ı	3.7	,	1.5	1	1.4	1	2.0	1	9.0	1	2.3
F10	Both Iso	21.5	7.6	4.0	15.2	7.6	11.0	9.0	4.0	9.0	2.8	1.1	1.5	,	ı	•	ı	,	1	1	1	,	1	ı	•	•	6.7	,	1			,	ı	(	1	,	,	,	•	1	
Max Percent	Lt Eng	10.2	7.0	8.2	1.3	,	15.8	0.3	0.4	0.2	1.1	1.4	1.9	2.3	2.5	11.2	1.2	0.7	2.7	8.0	1.7	9.0	2.7	0.5	2.2	9.0	1.0	7.3	8.2	9.7	7.9	0.4	0.4	0.2	0.2	11.2	3.5	0.4	9.0	9.0	8.0
	Rt Eng	14.6	1.2	'	,	3.6	13.4	0.7	1.8	0.1	1.1	1.4	2.7	1.4	4.6	5.5	2.5	3.4	2.6	2.3	6.0	1.0	2.6	1.0	1.1	4.1	0.3	4.3	2.7	2.2	2.9	0.4	8.0	1.2	1.2	0.5	1.1	6.0	9.0	2.2	1.0
	Lt Iso	'	ı	,	ı	,	'	1	,	1	'	,	,	,		79.5	,	92.0	,	92.7	,	94.0	,	96.4	,	95.0	•	94.6	,	97.4	ı	88.6	,	90.7	1	100.0	,	91.4	,	94.5	,
ed Flow	Rt Iso		,	1	,	,	,	•	1	ı	1	1	,	95.0	66.3	1	91.1	1	88.9	,	93.3	t	94.9	,	93.9	1	1	1	96.3	•	100.0		7.06	,	91.8		8.36	1	91.8	1	95.4
Max Percent Corrected Flow	Both Iso	86.0	78.3	74.2	82.7	6.07	81.3	96.6	100.0	88.9	97.0	92.0	91.2	•	1	•		١	•	1	•	,	•	,	,	,	90.3	١	,	1	•	1	٠		•	•		,	,		ı
Max Perce	Lt Eng	93.0	92.7	90.3	97.6	1	99.3	9.88	7.06	87.6	90.3	6.68	0.06	90.3	95.3	95.4	92.3	6.68	91.3	90.1	6.06	6.68	92.2	90.7	6.06	89.4	90.6	98.0	97.0	8.86	97.4	89.1	89.0	88.7	88.1	100.0	98.6	7.68	89.1	8.68	90.4
	Rt Eng	78.4	8.62	ı	1	90.08	85.4	93.8	95.4	91.9	95.4	94.4	95.7	93.2	94.9	93.4	94.3	100.0	90.1	91.2	92.7	92.0	94.3	95.5	92.7	93.2	93.7	93.8	94.1	92.6	0.96	93.0	93.1	93.8	93.6	92.6	6.56	94.0	93.9	97.6	94.3
p F	System	150	75	75	12	12	12	28	09	09	20.5	20	20	20	150	150	12	12	06	06	70	70	20	20	30	30	30	70	70	20	20	06	06	70	70	20	20	70	70	20	20
Temp	Feed Tank	150	150	150	150	150	150	00	70	70	70	70	06	06	12	12	12	12	06	06	70	70	20	20	30	30	30	06	90	06	06	90	90	70	70	20	20	06	06	06	06
	Run	7	52	4	Ŋ	9	7		6	10	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	59	30	31	32	33	34	35	36	37	38	39	40	4.1	42

(1) Run consisted of steady state flow followed by pulsed flow on a .06 sec on, 1.0 sec off cycle. (2) Run consisted of pulsed flow on a .06 sec on, 1.0 sec off cycle followed by steady state flow.

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# 4.1.1 Experimental Data Reduction Uncertainty

The equivalent area of each component was calculated from the equation, obtained by combining equations (3) through (5).

$$A = \frac{Q\rho_1}{C_d \rho_2 \sqrt{2g \frac{\Delta P}{\rho_2}}}$$
 (7)

where: Q = volumetric flow at flowmeter

 $\rho_1$  = weight density at flowmeter

 $\rho_2$  = weight density at component

 $\Delta P$  = component differential pressure

 $C_{d}$  = discharge coefficient

g = acceleration due to gravity

Rearranging (7)

$$A = KQ \rho_1 \rho_2^{-1/2} \Delta P^{-1/2}$$
 (8)

where:  $K = \frac{1}{C_d \sqrt{2g}}$ 

The density was determined from the formula:

$$\rho = 95.4 - 0.0737T - 2.65 \times 10^{-9} \times T^4$$
 (9)

where: T = temperature °F

This equation was selected for a precise fit to the density curve provided in Reference 15. The total uncertainty in density is

$$\Delta \rho = \frac{\partial \rho}{\partial T} \Delta T \tag{10}$$

The worst case density error is at  $150^{\circ}F$  where  $\Delta \rho = 0.29\%$ .

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The error in equivalent area is given by:

$$\Delta A = \frac{\partial A}{\partial Q} \Delta Q + \frac{\partial A}{\partial \rho_1} \Delta \rho_1 + \frac{\partial A}{\partial \rho_2} \Delta \rho_2 + \frac{\partial A}{\partial \Delta P} \Delta (\Delta P)$$
 (11)

The individual errors are:

$$\frac{\partial A}{\partial Q} \Delta Q = K \rho_1 \rho_2^{-1/2} \Delta P^{-1/2} \Delta Q \qquad (12)$$

$$\frac{\partial A}{\partial \rho_1} \Delta \rho_1 = KQ \rho_2^{-1/2} \Delta P^{-1/2} \Delta \rho_1$$
 (13)

$$\frac{\partial A}{\partial \rho_2} \Delta \rho_2 = \frac{1}{2} KQ \rho_1 \rho_2^{-3/2} \Delta P^{-1/2} \Delta \rho_2$$
 (14)

$$\frac{\partial A}{\partial \Delta P} = \frac{1}{2} KQ \rho_1 \rho_2^{-1/2} \Delta P^{-3/2} \Delta(\Delta P)$$
 (15)

Substituting equations (12) through (15) in equation (11), and dividing by equation (8), the percent error in equivalent area is given by:

$$\frac{\Delta A}{A} 100 = \left(\frac{\Delta Q}{Q} + \frac{\Delta \rho_1}{\rho_1} + \frac{\Delta \rho_2}{2\rho_2} + \frac{\Delta(\Delta P)}{2\Delta P}\right) 100$$
 (16)

Substituting the values from Table 3-2 in equations (10) and (16), the absolute and run to run accuracy is given by:

$$(100) \frac{\Delta Q}{Q} = \pm 0.7\%$$

$$(100) \frac{\Delta \rho_1}{\rho_1} = 0.29\%$$

$$100 \left(\frac{1}{2}\right) \left(\frac{\triangle \rho_2}{\rho_2}\right) = .14\%$$

$$100 \left(\frac{1}{2}\right) \left(\frac{\triangle(\triangle P)}{\triangle P}\right) = .9\%$$

The total uncertainty in equivalent area on a run to run basis from equation (16) is + 2.0 percent.

The within-run uncertainty is obtained in similar fashion by substituting the values from Table 3-3 in equations (10) and (16). The within-run uncertainty in equivalent area is  $\pm$  1.0 percent. Since corrected flow data was calculated at an arbitrary pressure and density condition, no further error is introduced compared to the equivalent area.

## 4.1.2 Result Summary

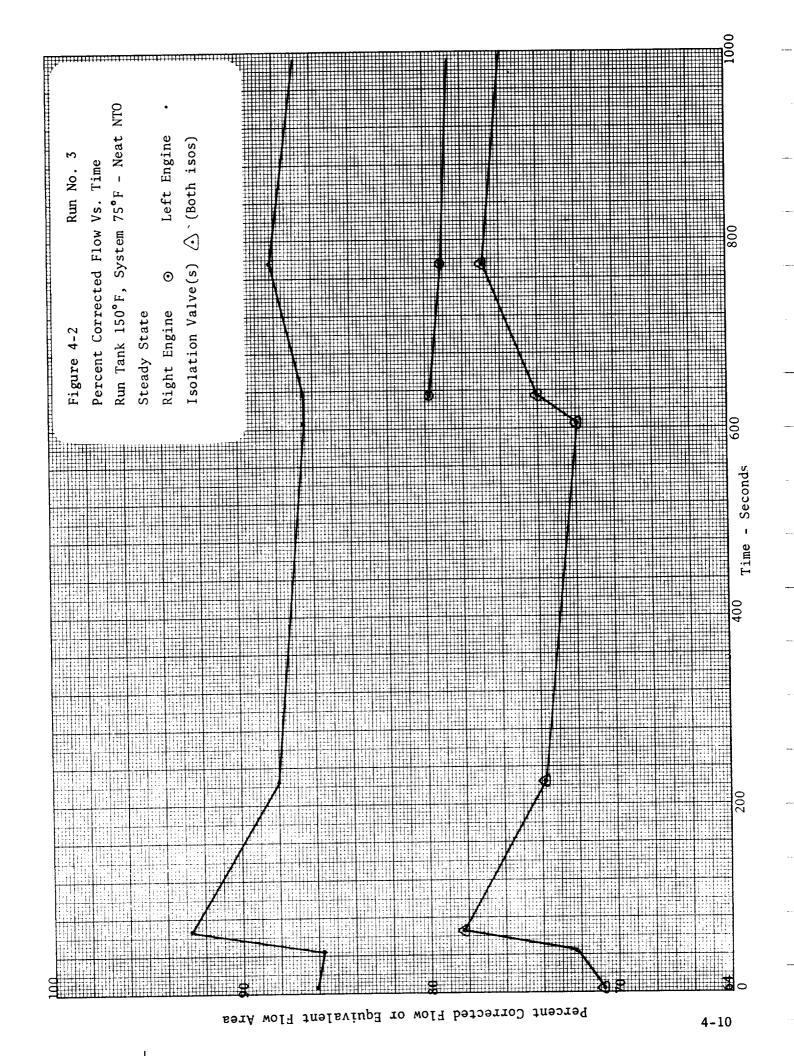
The within-run accuracy in the corrected flow from Section 3.3 and 4.4.1 is  $\pm$  1.0 percent, resulting in a two percent flow uncertainty band. Therefore, a flow decay of two percent was chosen as the minimum significant value. In twenty-four out of forty runs, flow decays equal to or greater than two percent were experienced in the engines and/or the isolation valves. Figures 4-41 through 4-45 illustrate the percent maximum flow variation as a function of feed tank and OWPS temperature, and Figures 4-46 through 4-50 illustrate the percent maximum flow decay as a function of feed tank and OWPS temperature.

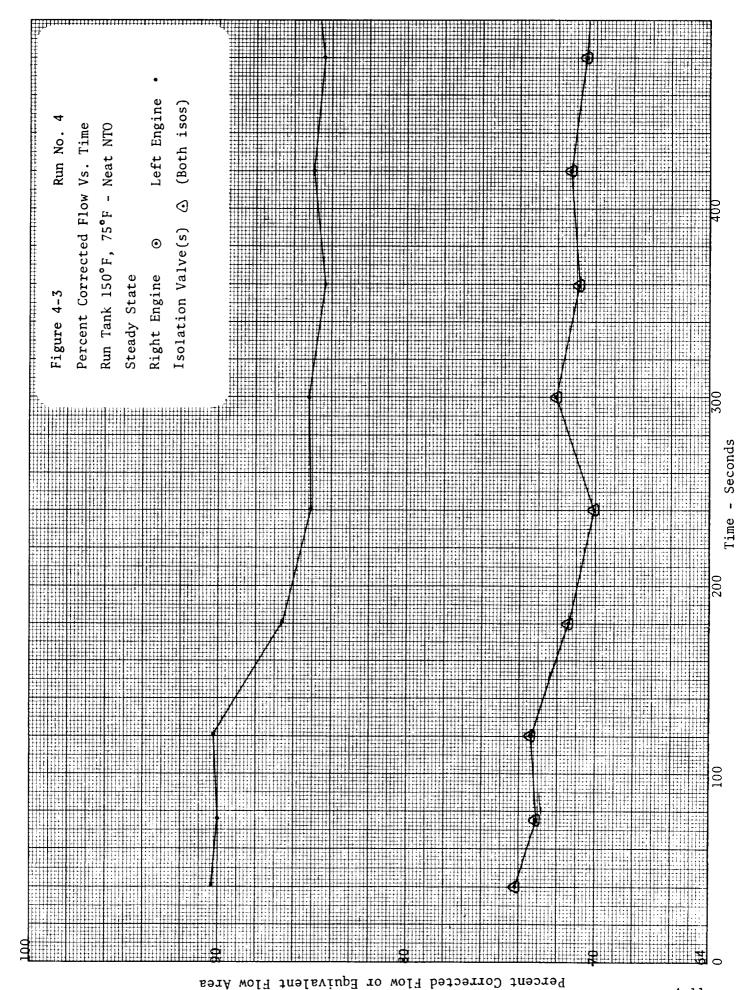
In order to assess the possible effects of the operational mode on flow degradation, plots of maximum percent flow decay versus feed tank and OWPS temperature were made for the right and left engines. Separate curves are shown for steady-state-pulse operation and pulse-steady-state operation. These plots are presented in Figures 4-51 through 4-54.

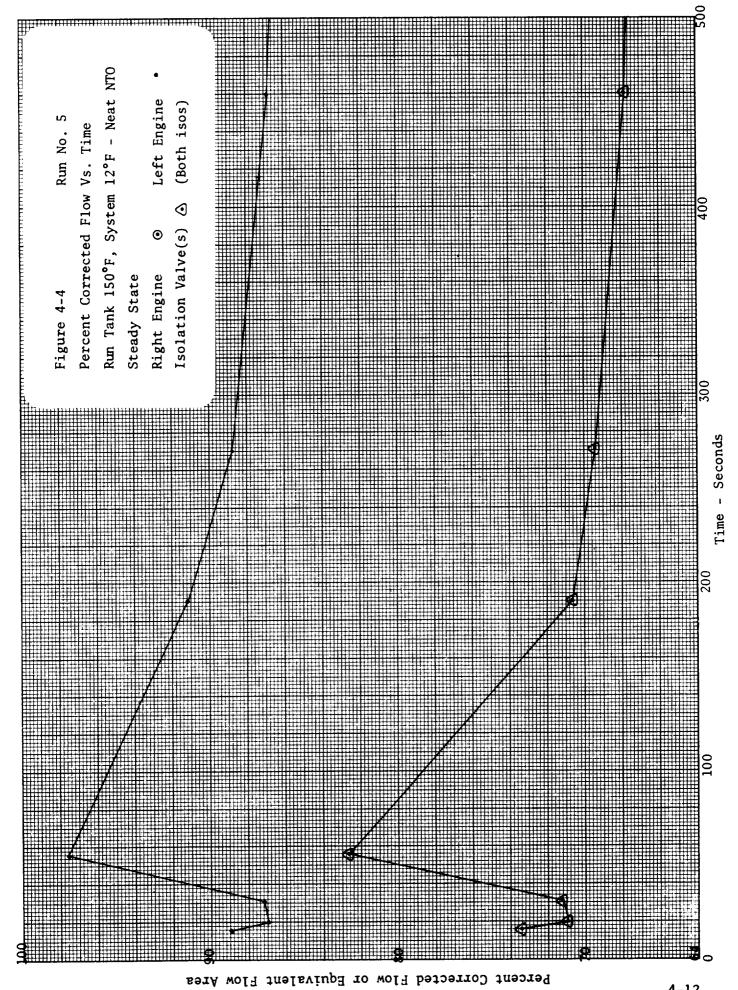
In general, the largest flow anomalies and decays occurred at the temperature extremes, 150°F and 12°F. The flow variations were greatest for the left engine and isolation valves. Most variations occurred during the initial portion of the run, or when the run mode was switched, e.g., from pulse to steady-state or vice versa.

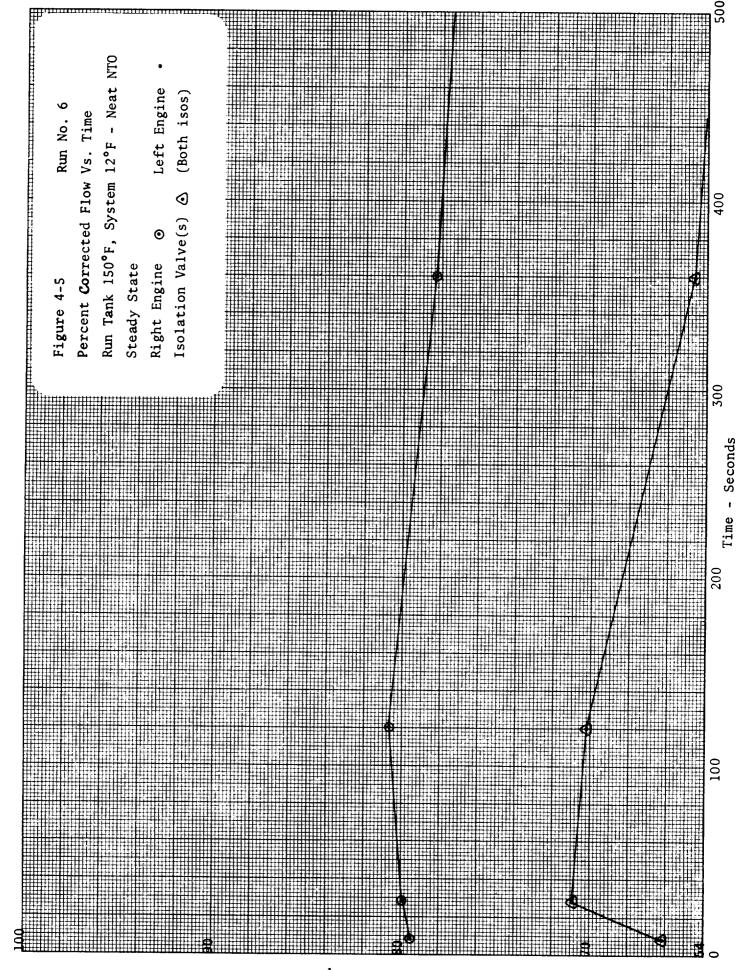
In most cases where there was an initial feed tank to OWPS temperature gradient, the flow decay was greater when the system was operated in the pulse-steady-state mode. This operating mode allowed the initial temperature gradient to exist for a longer period than the steady-state-pulse mode since the system tended to be heated or cooled by the incoming propellant.

Percent Corrected Flow or Equivalent Flow Area

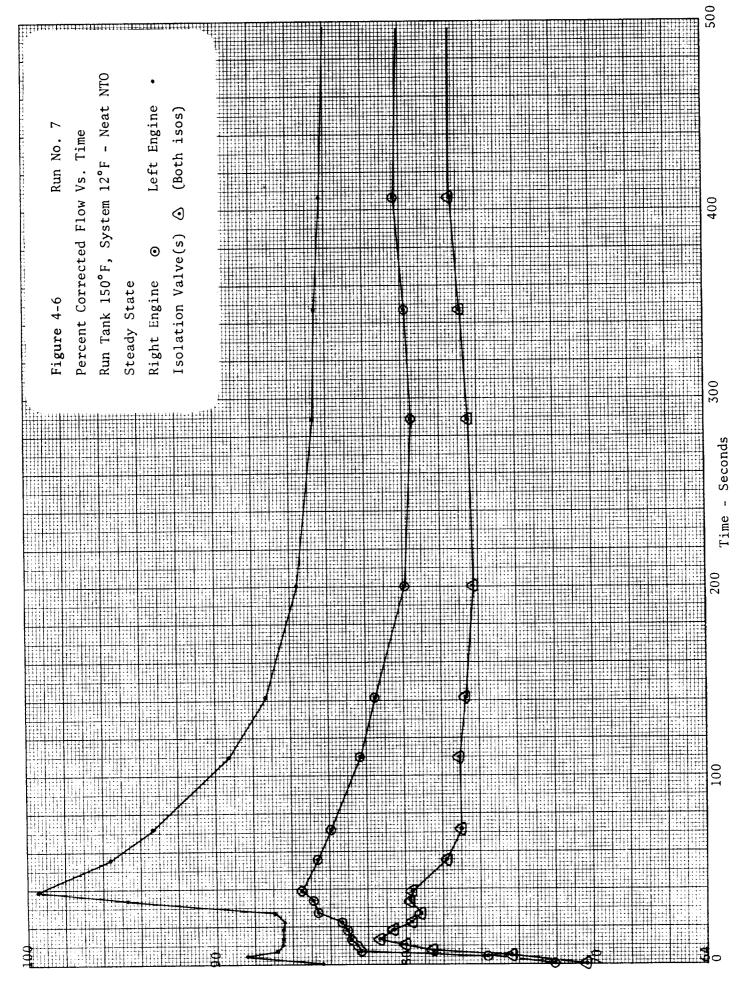


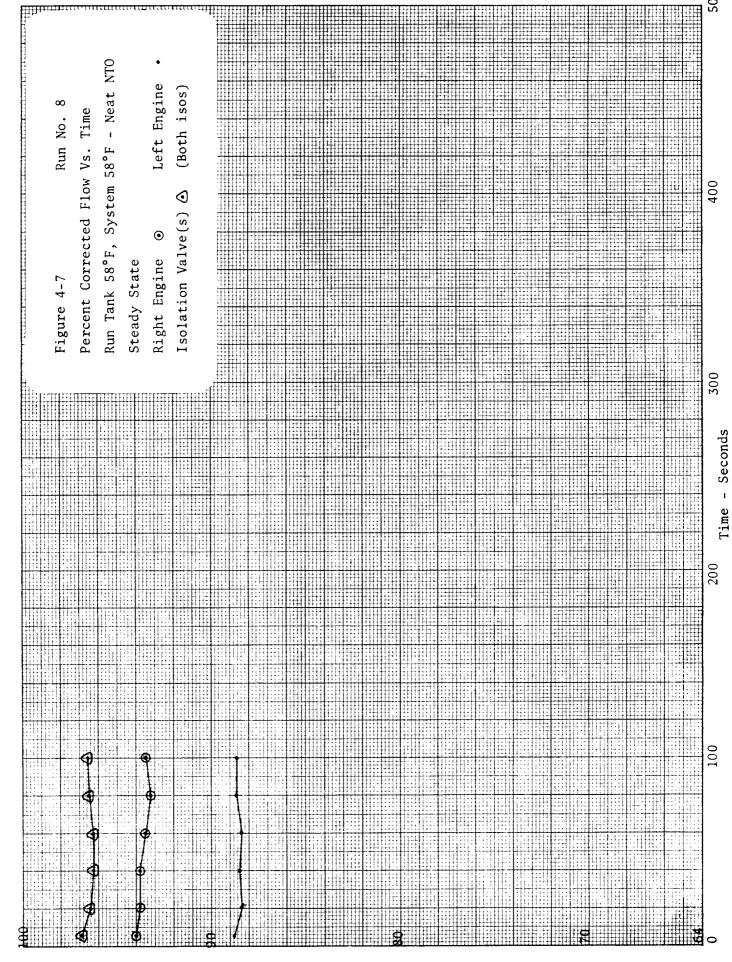




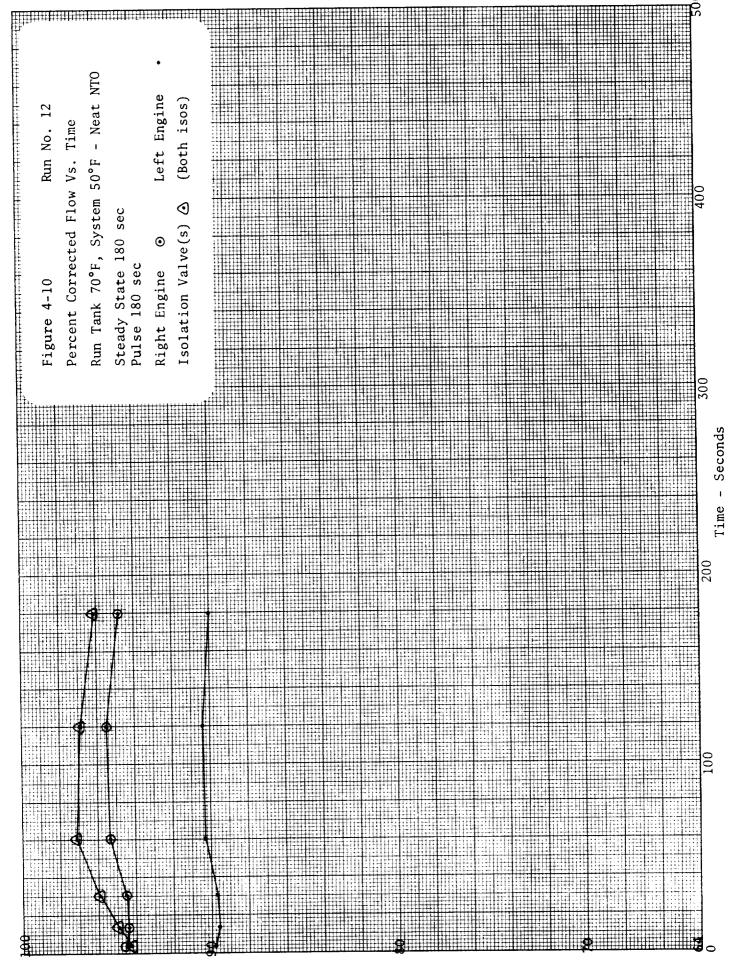


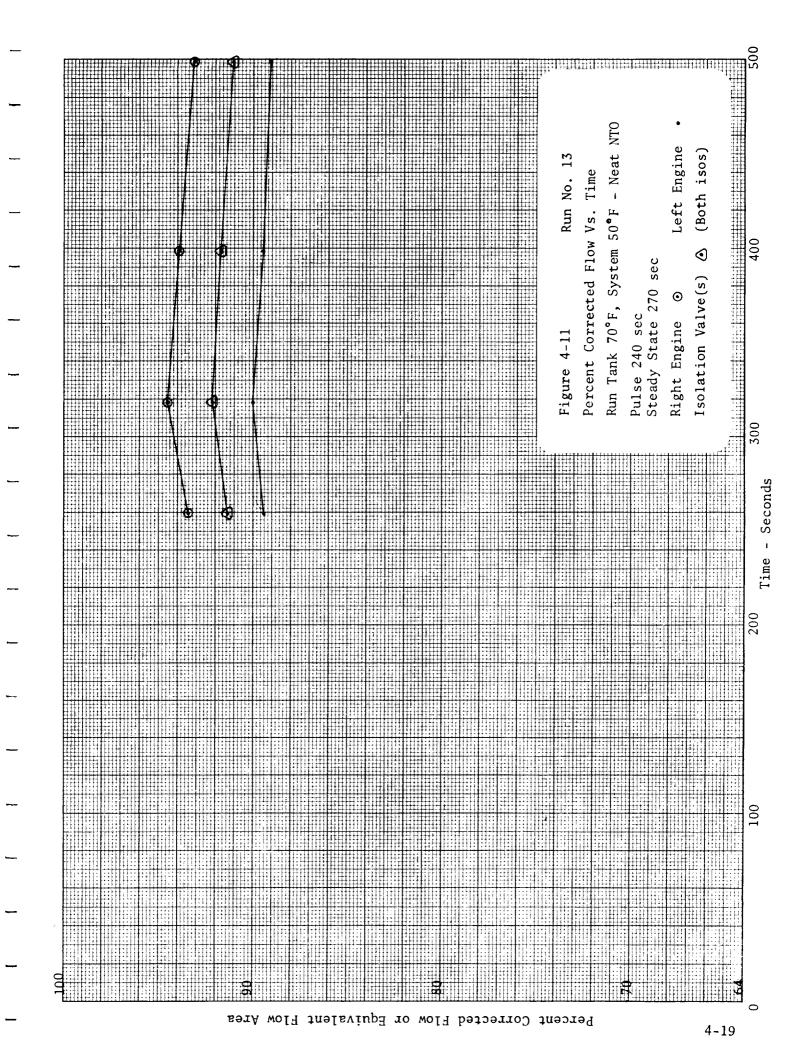
Percent Corrected Flow or Equivalent Flow Area

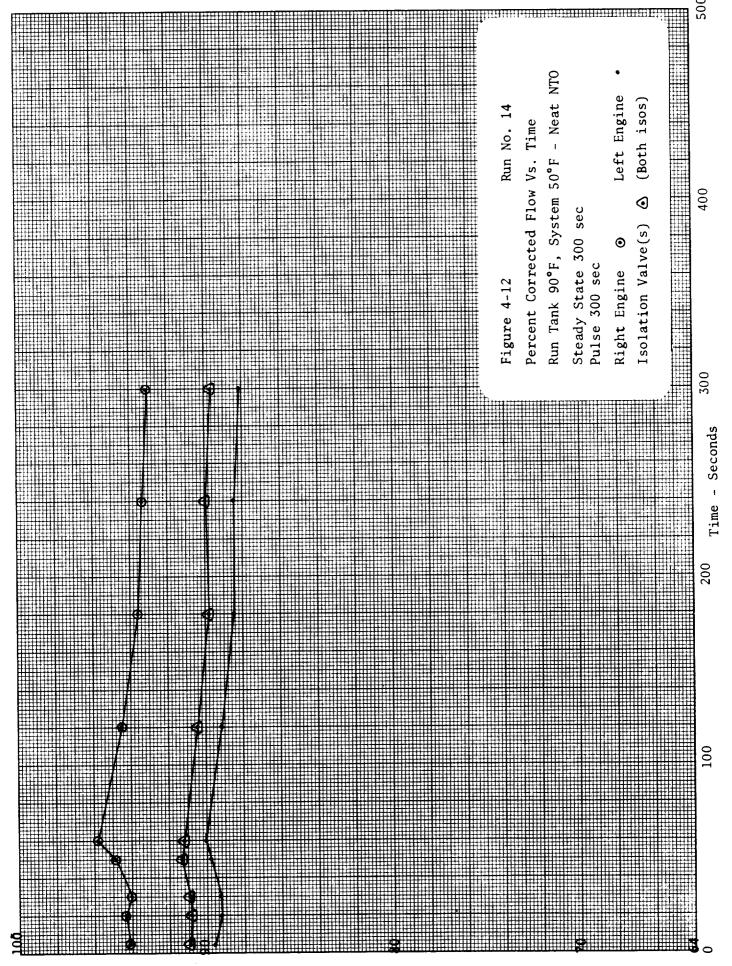




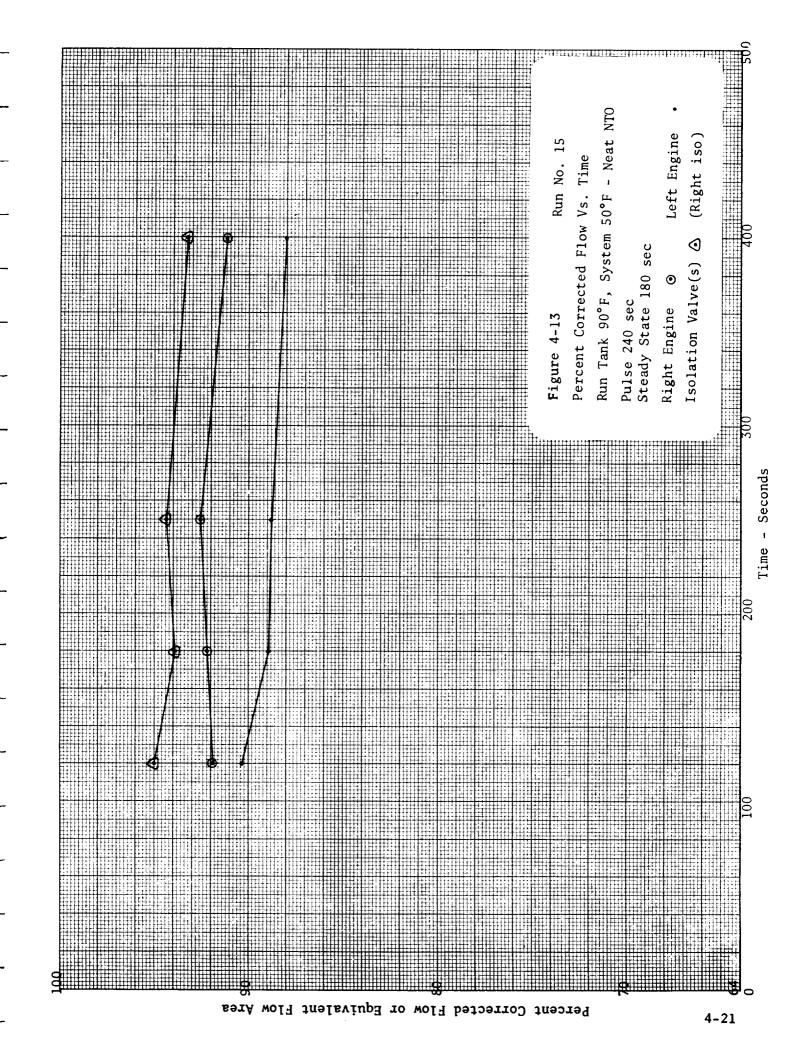
Percent Corrected Flow or Equivalent Flow Area

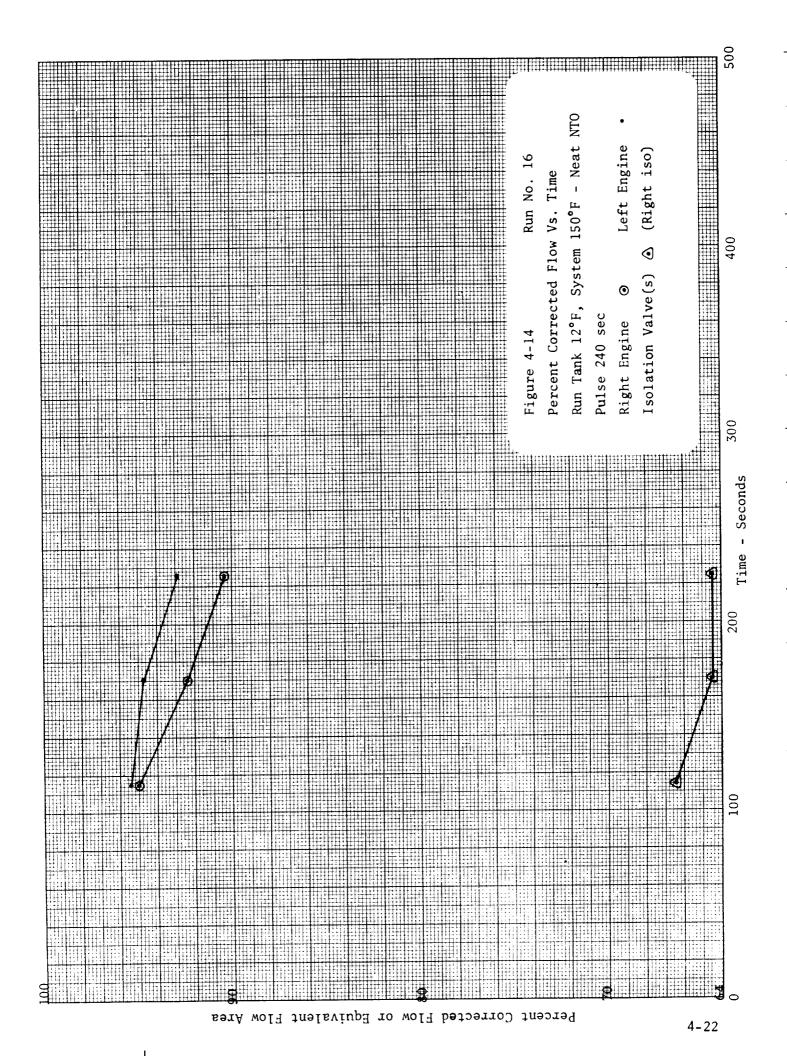


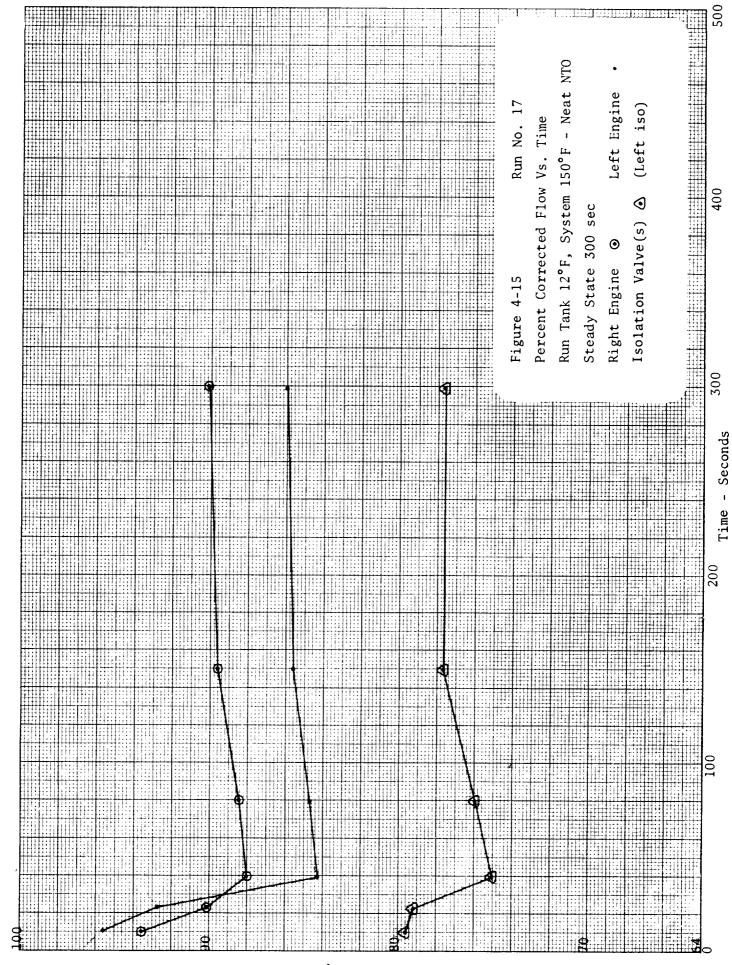




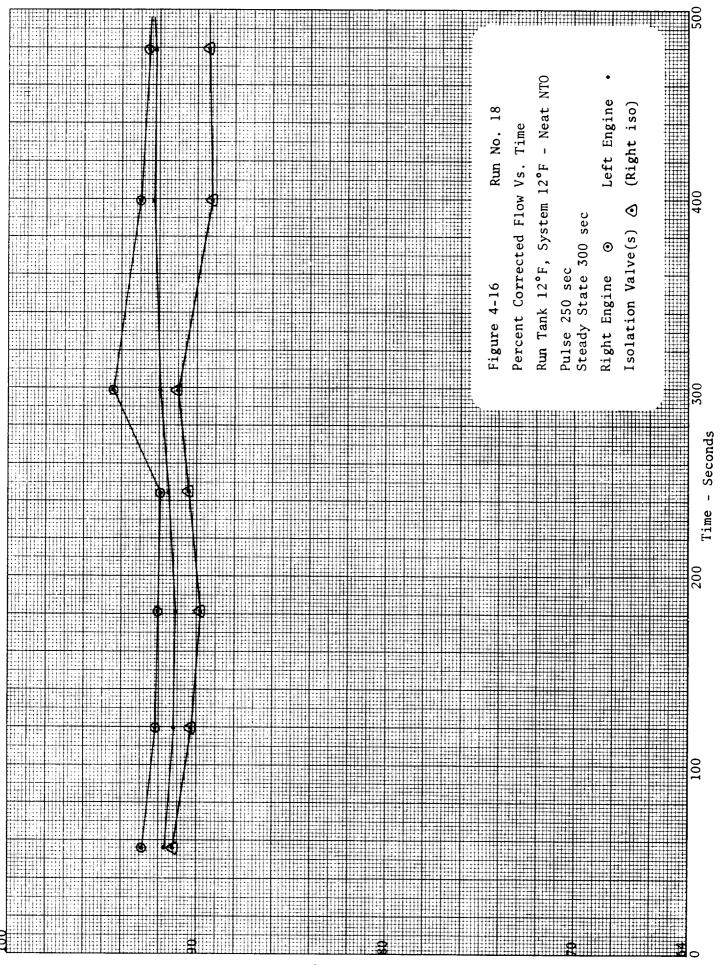
Percent Corrected Flow or Equivalent Flow Area



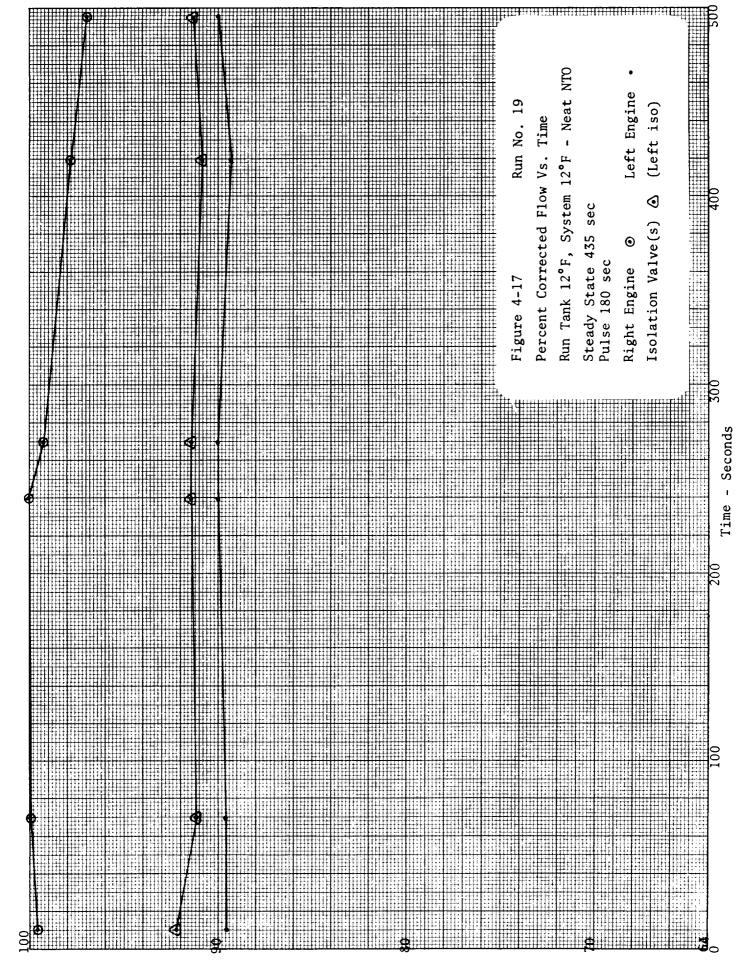




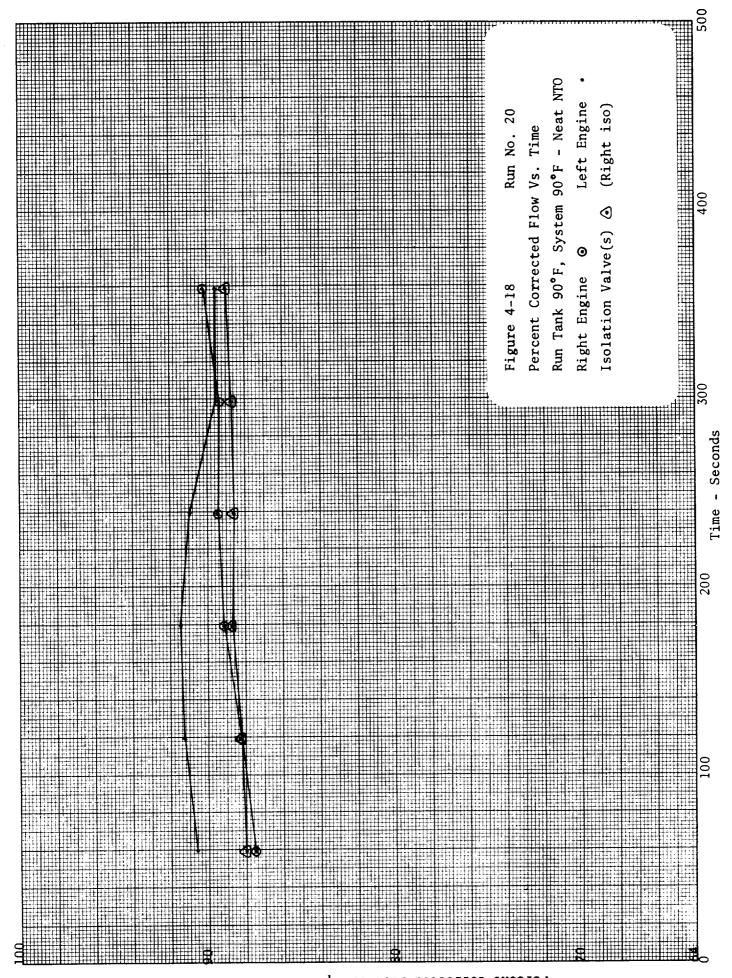
Percent Corrected Flow or Equivalent Flow Area

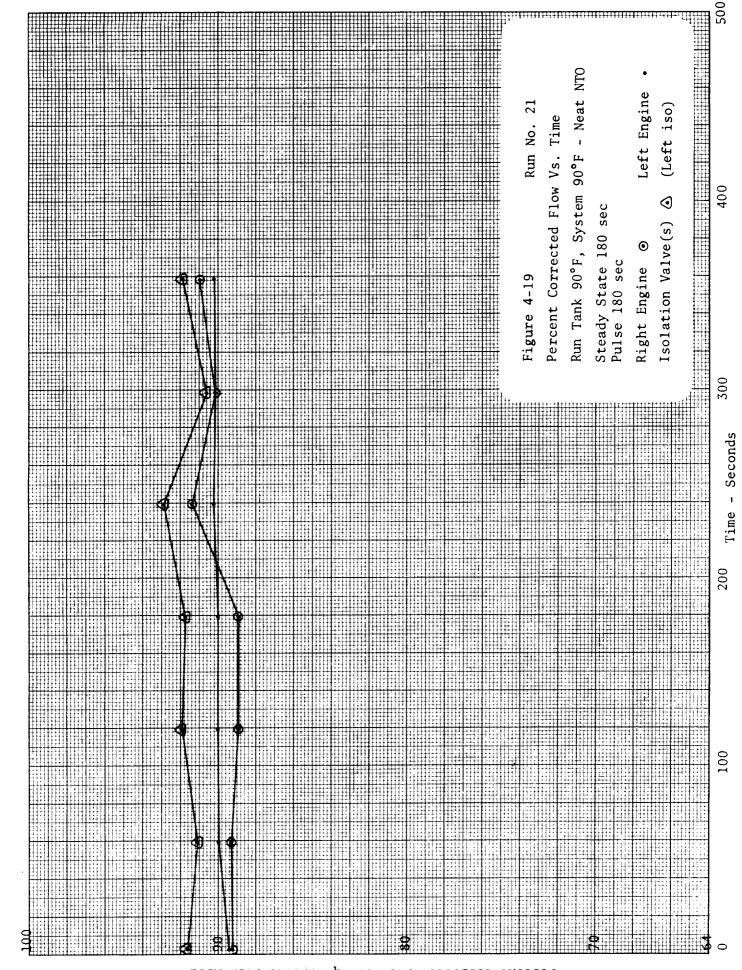


Percent Corrected Flow or Equivalent Flow Area

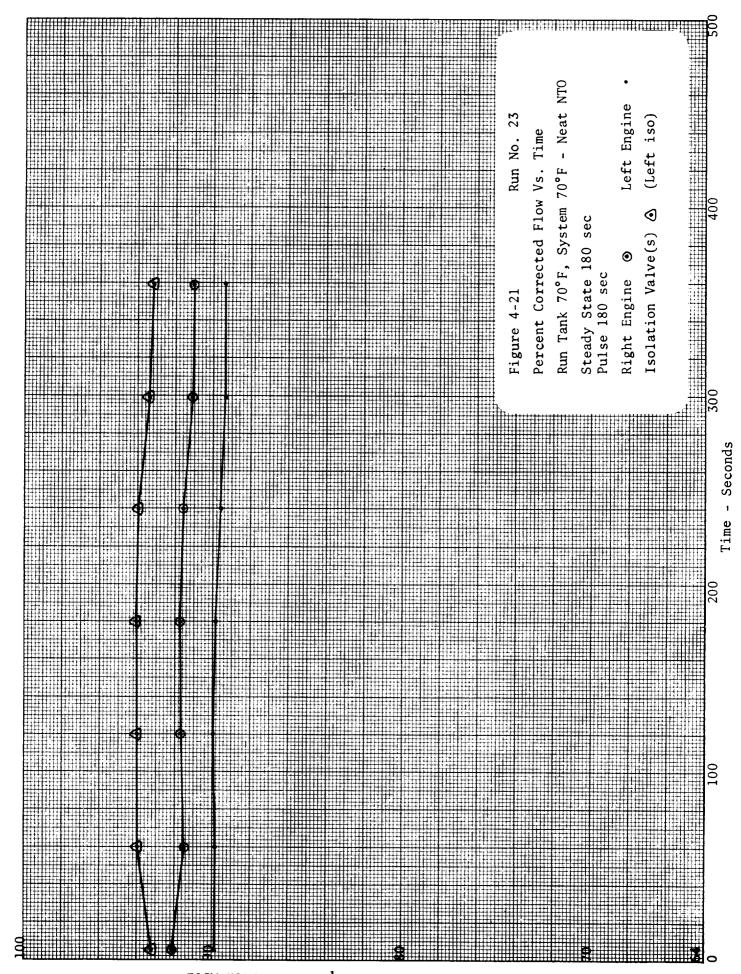


Percent Corrected Flow or Equivalent Flow Area

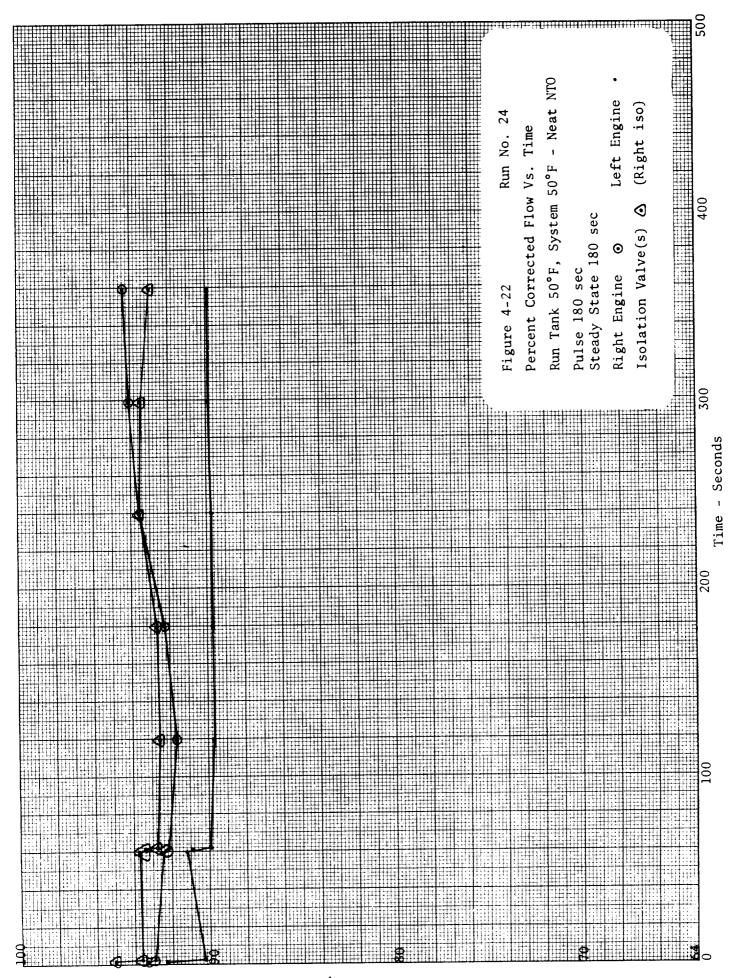




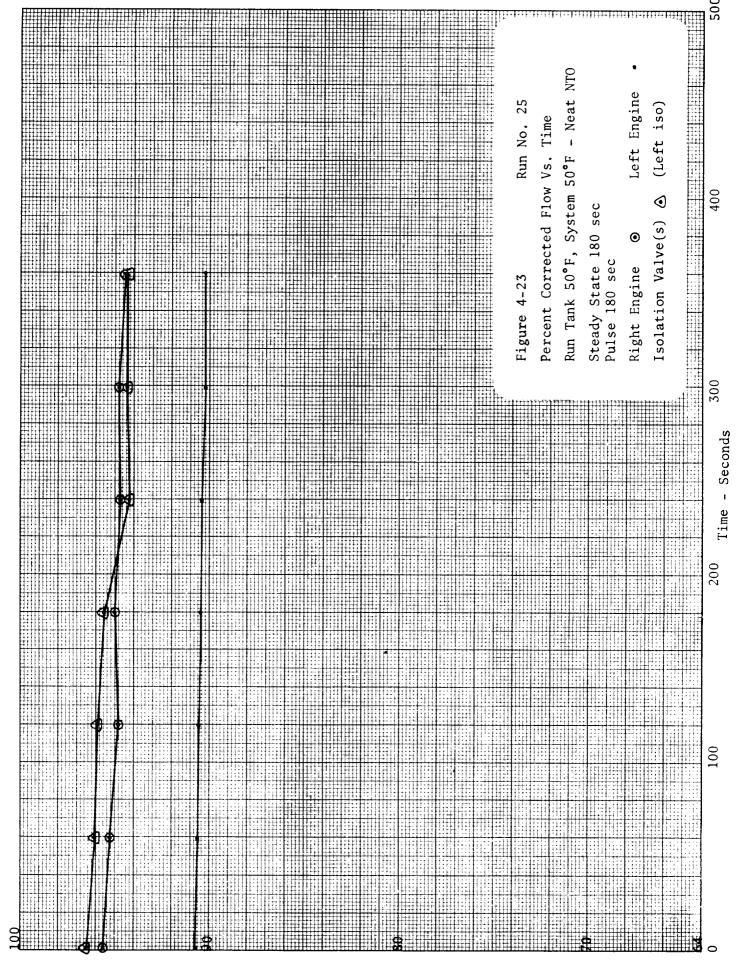
Percent Corrected Flow or Equivalent Flow Area



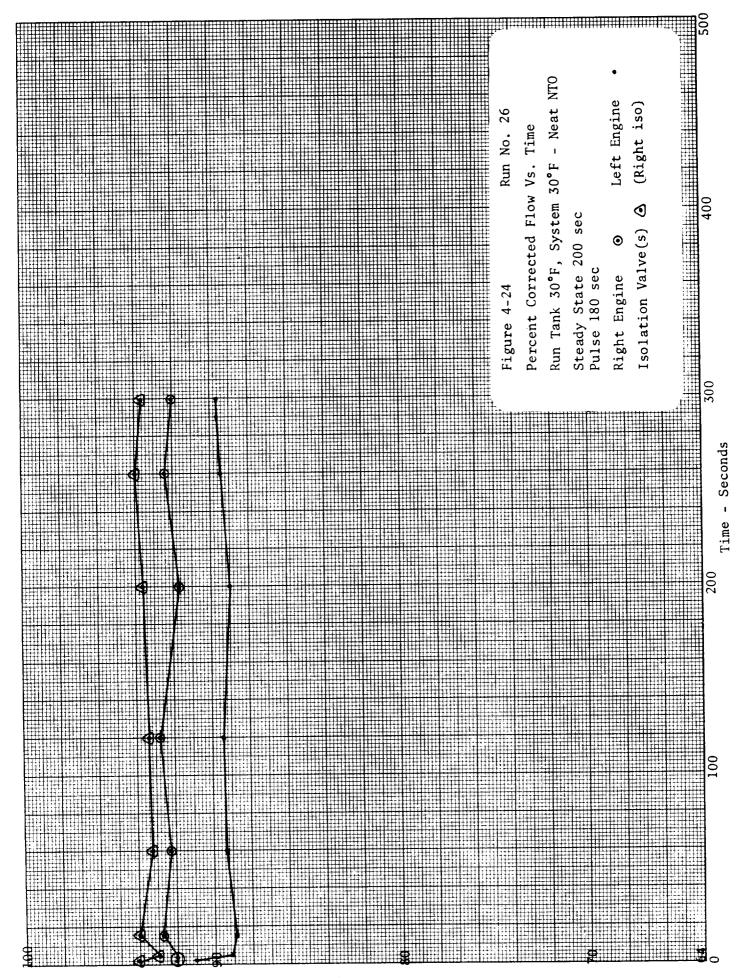
Percent Corrected Flow or Equivalent Flow Area

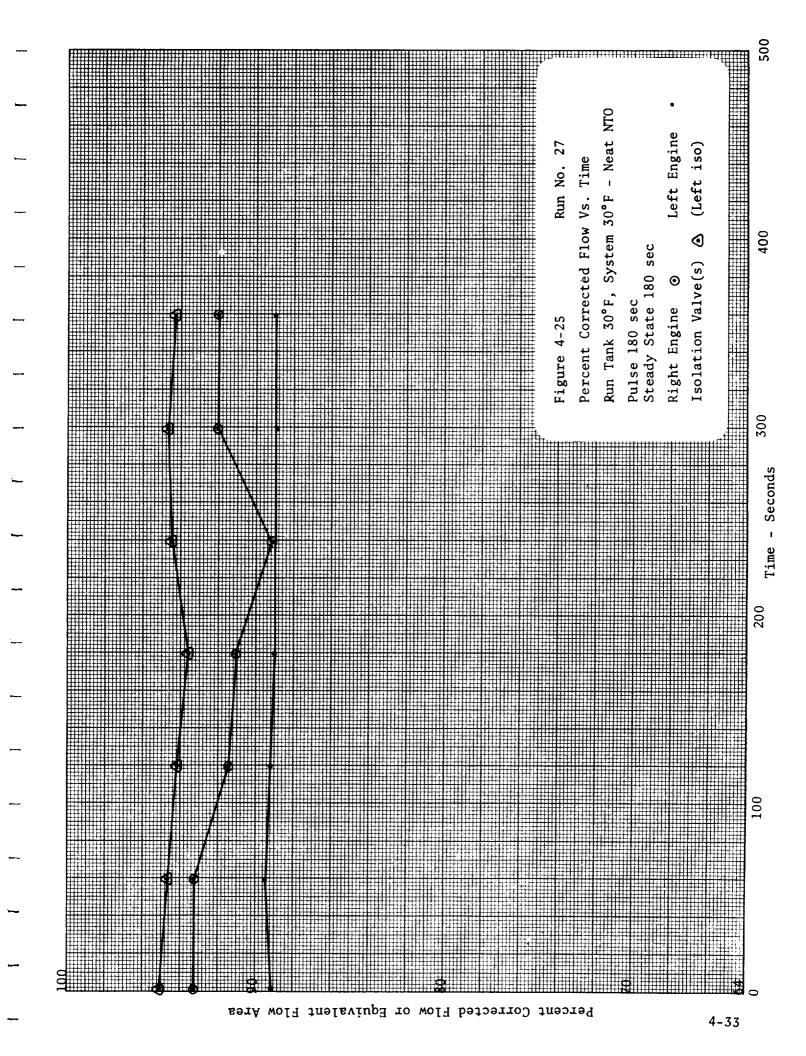


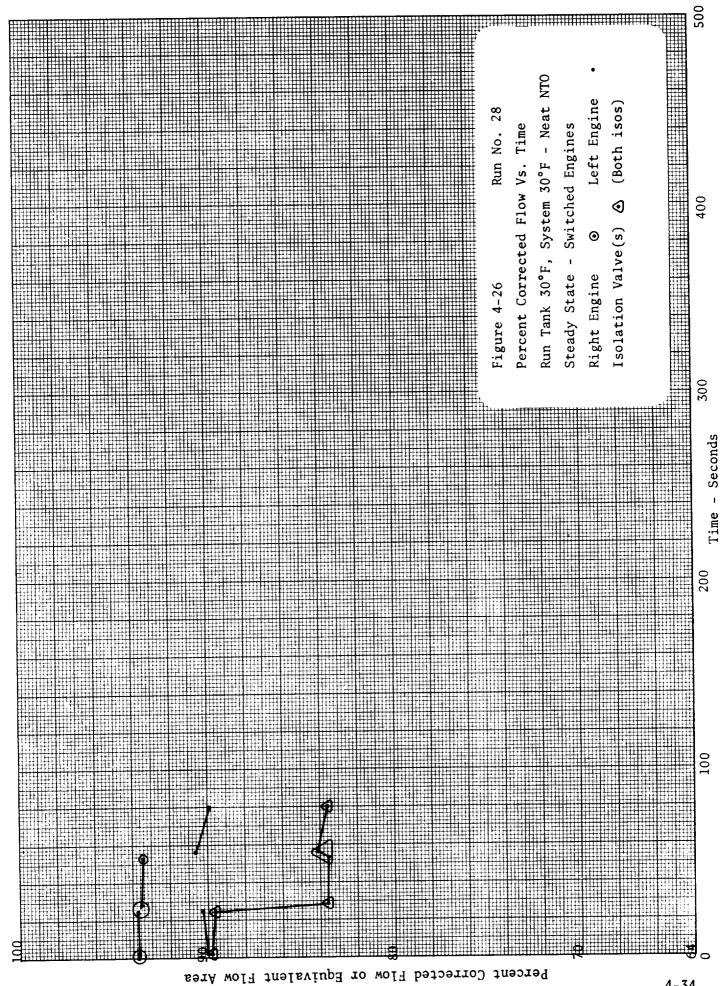
Percent Corrected Flow or Equivalent Flow Area

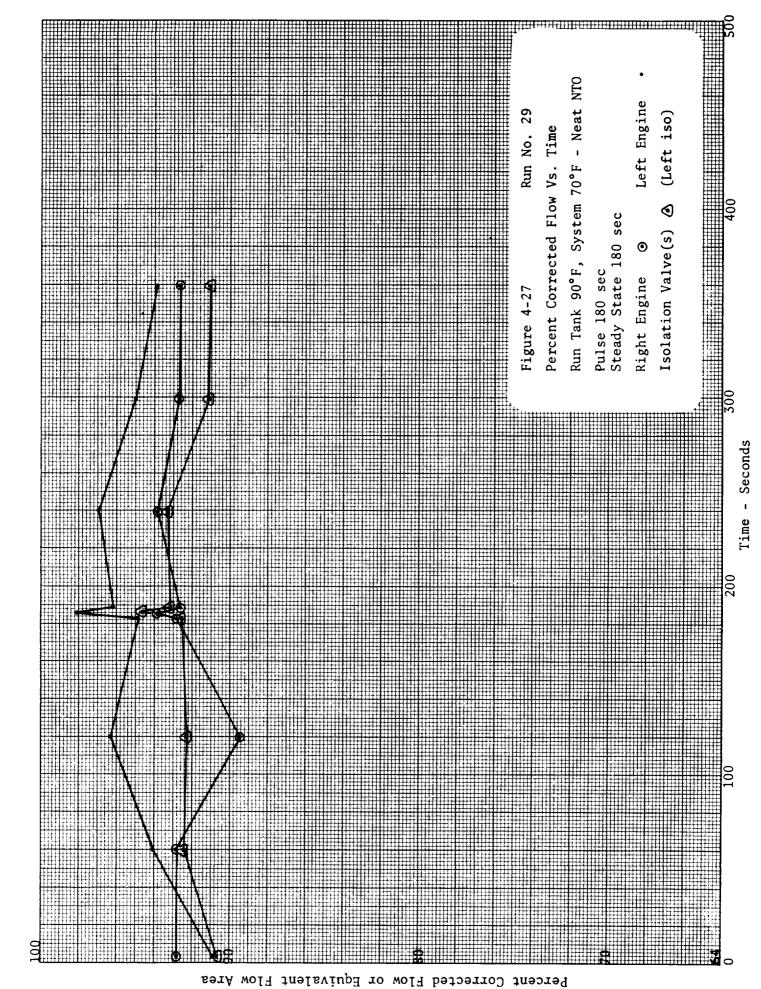


Percent Corrected Flow or Equivalent Flow Area

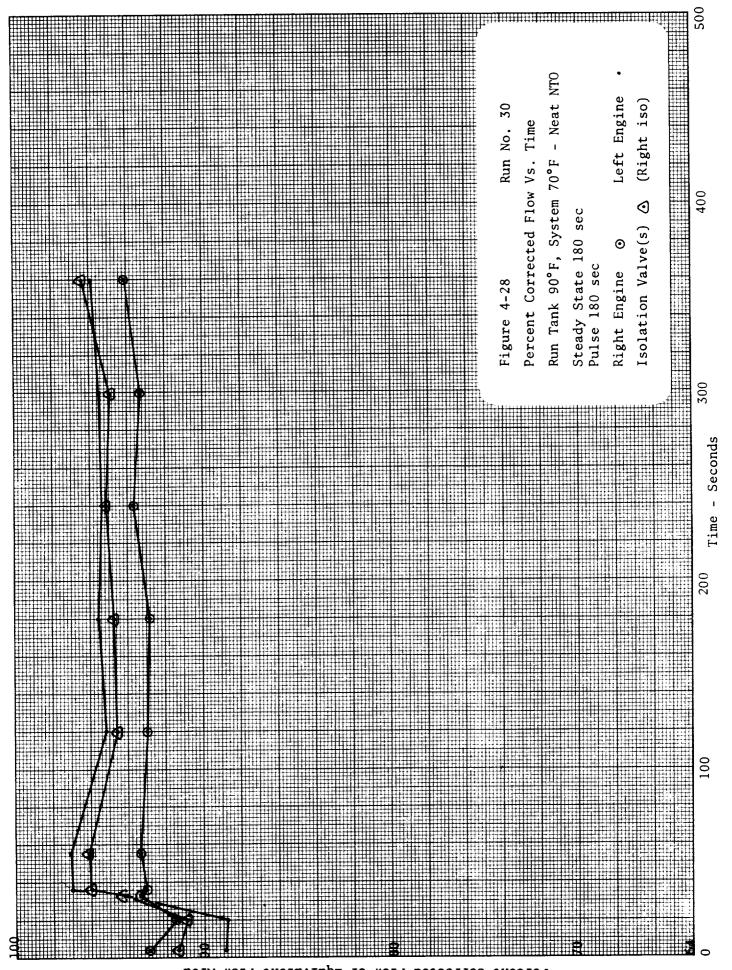




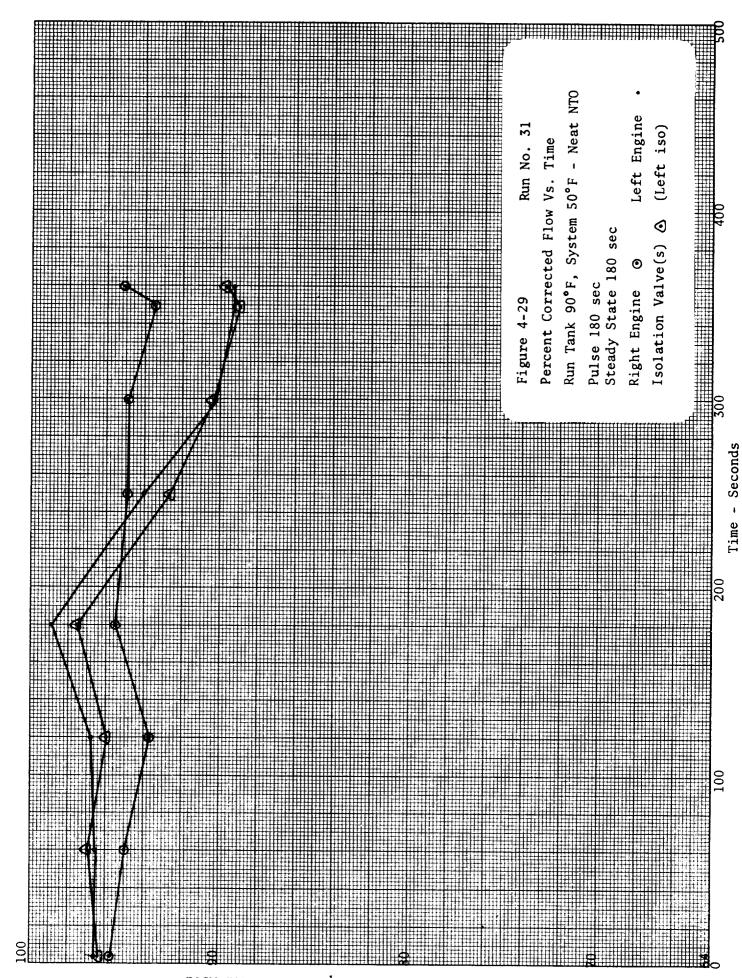


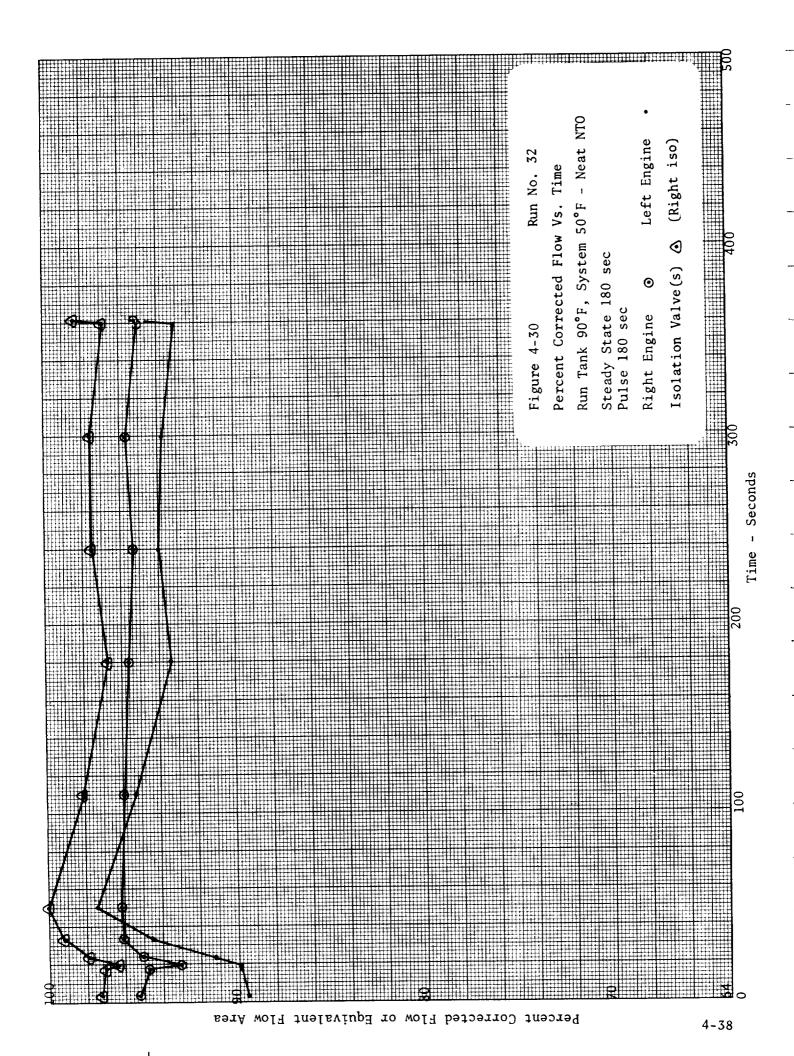


4-35



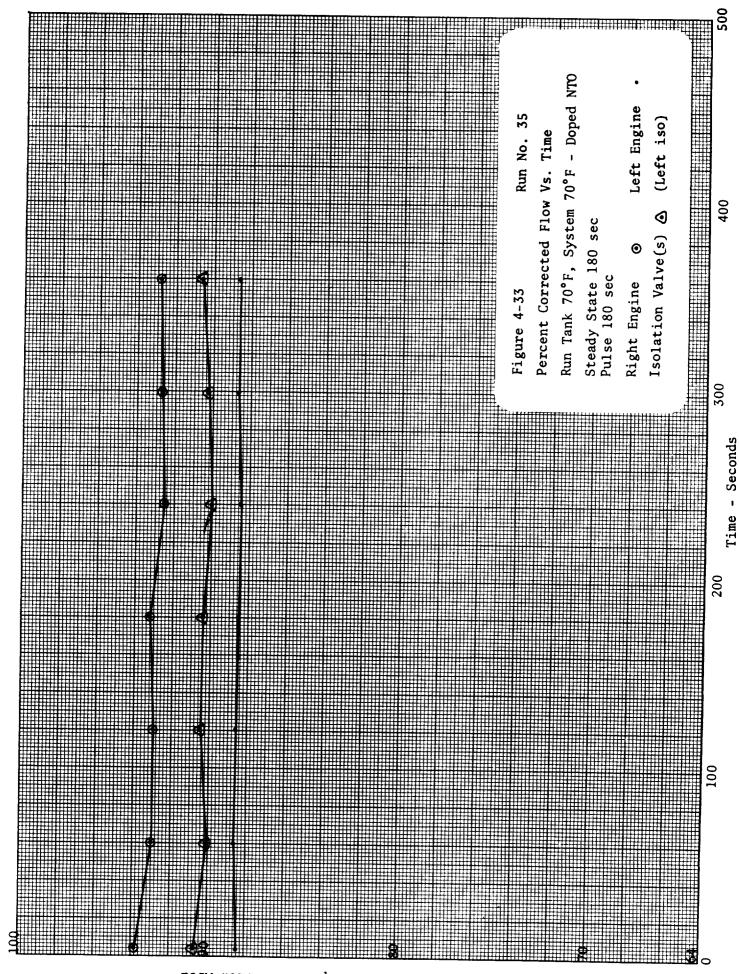
Percent Corrected Flow or Equivalent Flow Area

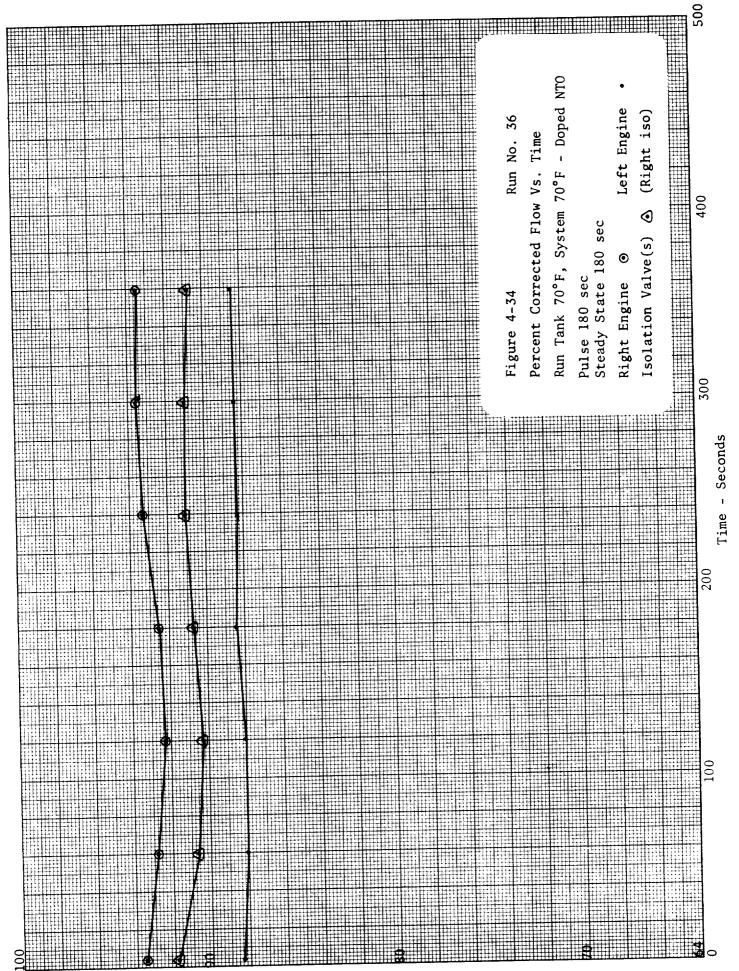




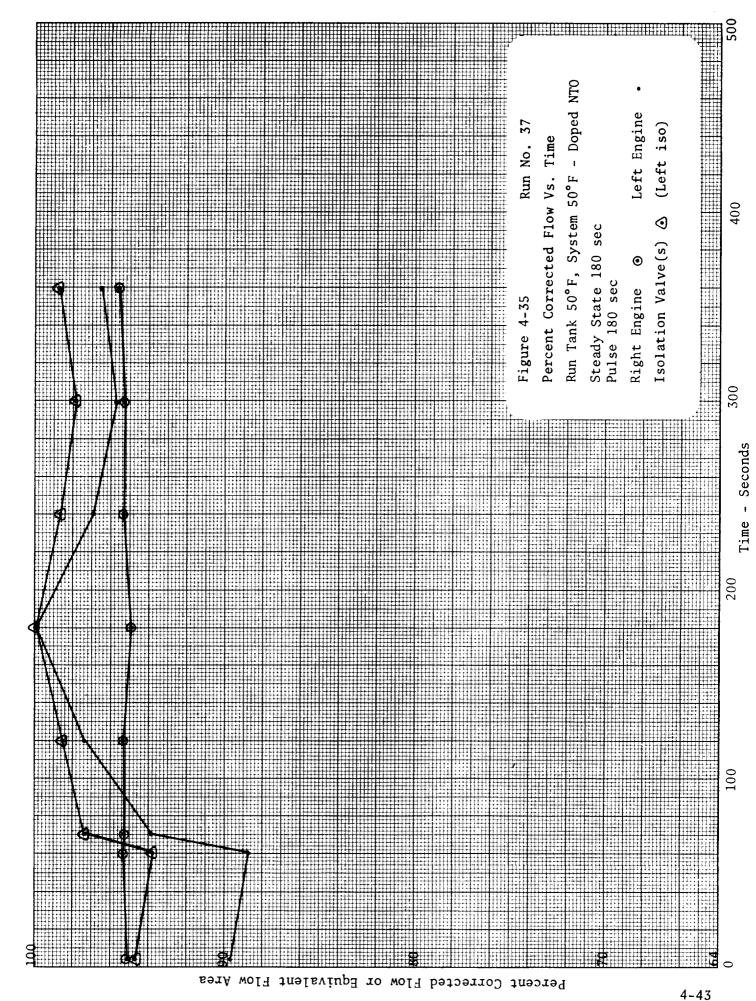
Percent Corrected Flow or Equivalent Flow Area

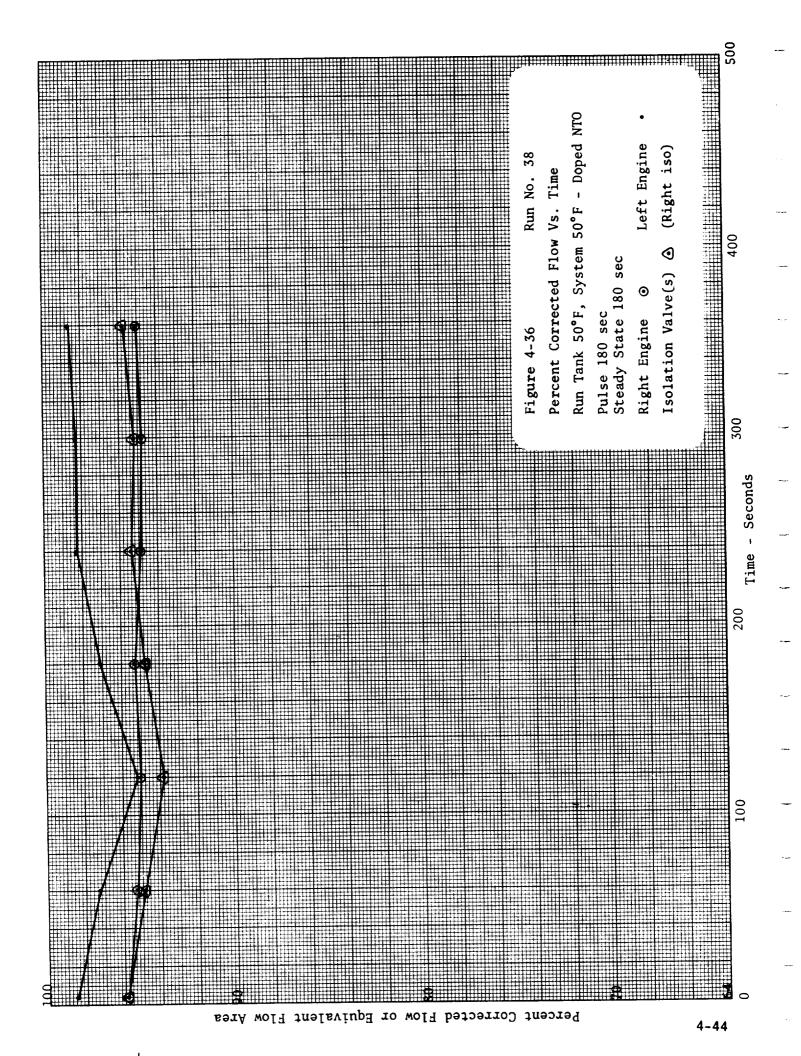
Percent Corrected Flow or Equivalent Flow Area

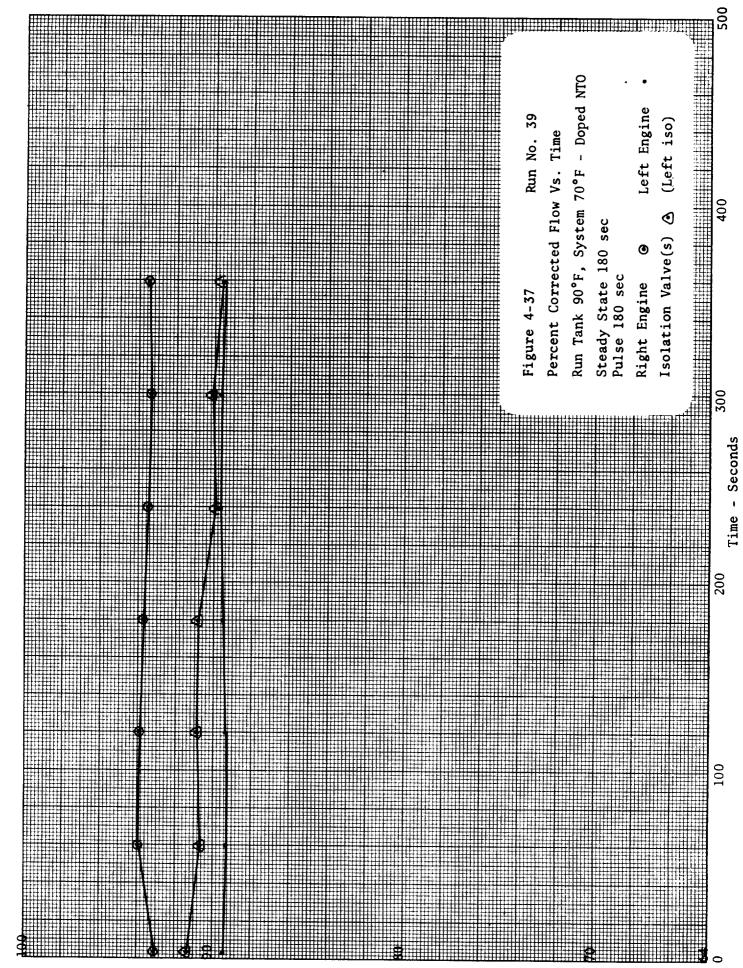




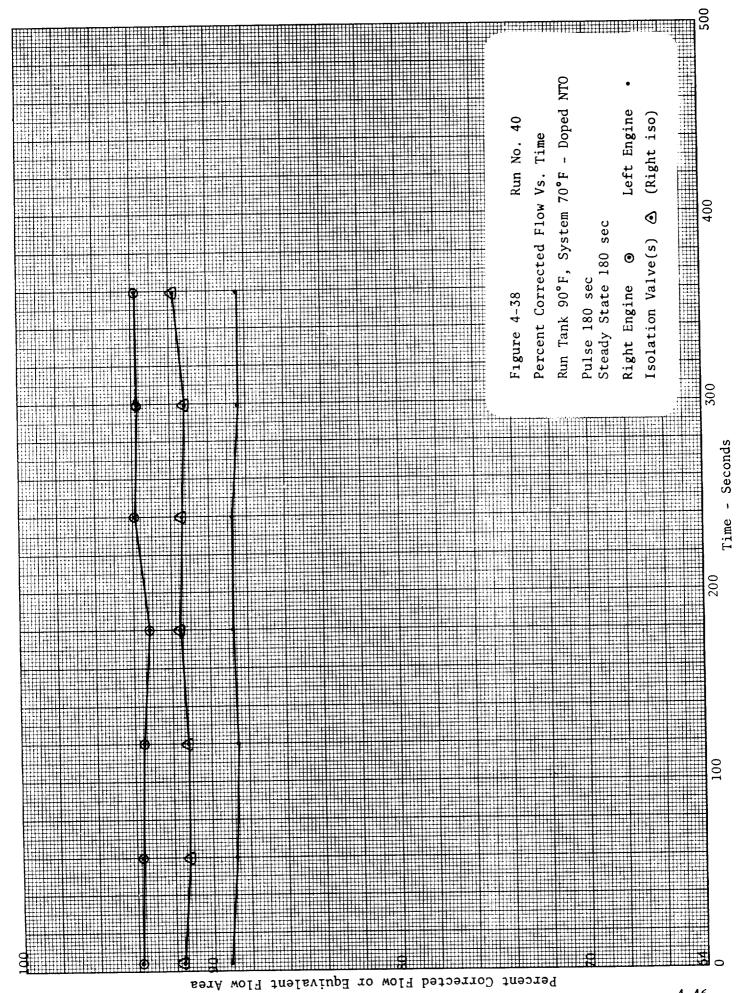
Percent Corrected Flow or Equivalent Flow Area

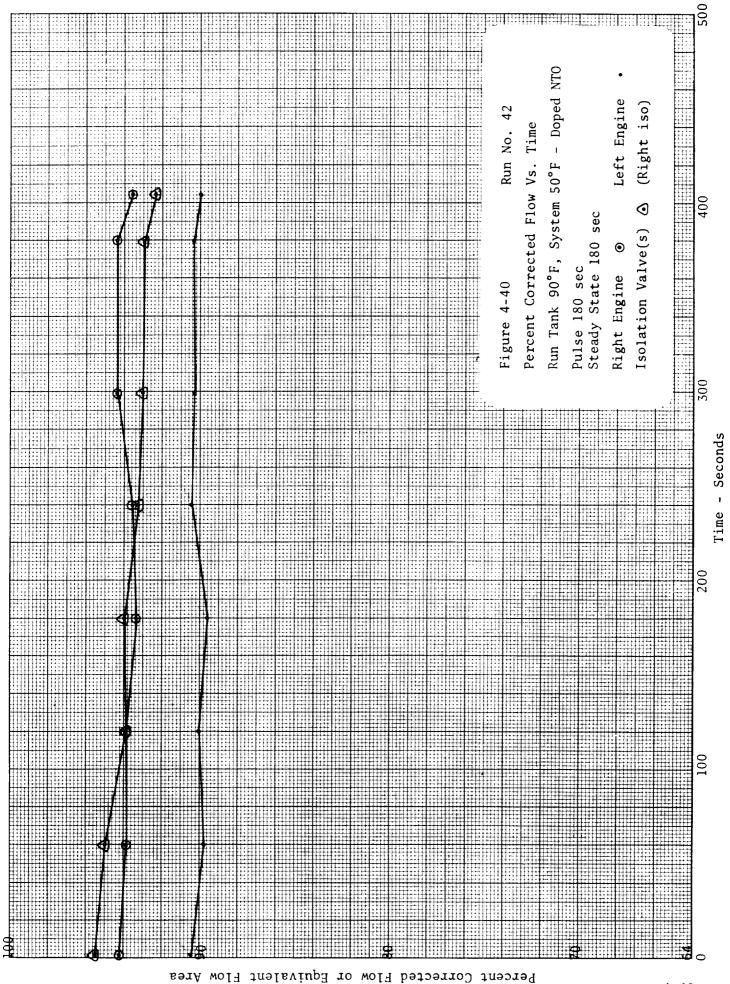




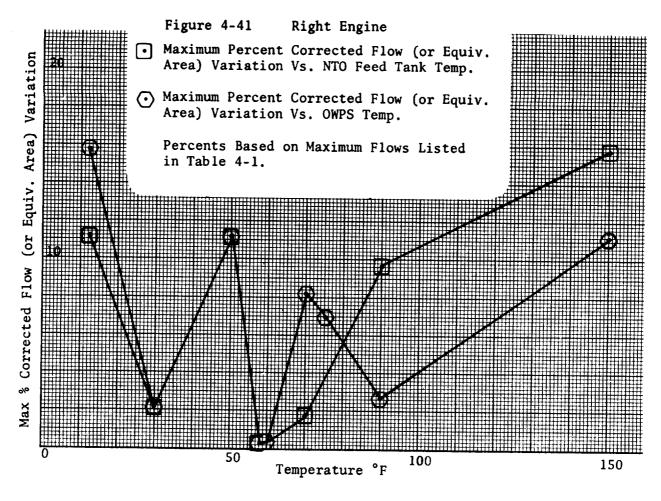


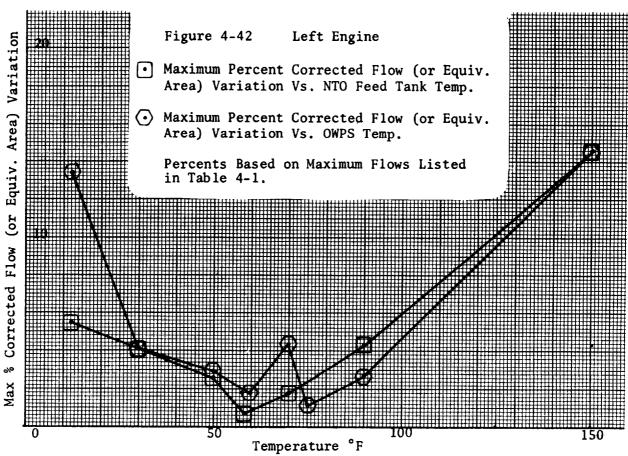
Percent Corrected Flow or Equivalent Flow Area

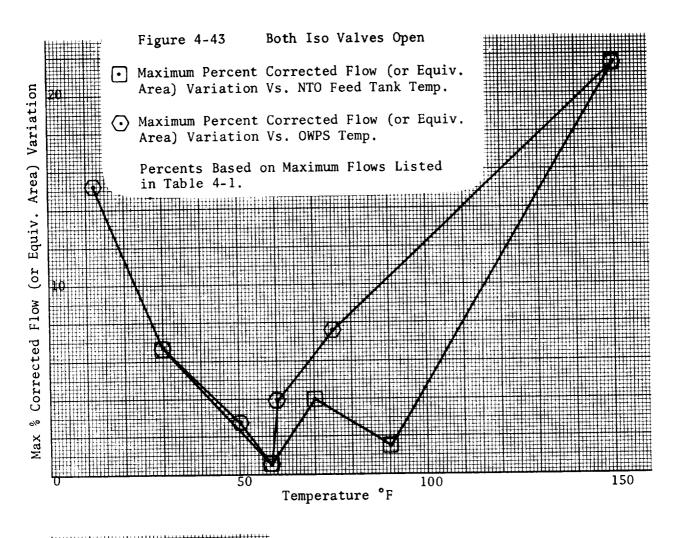


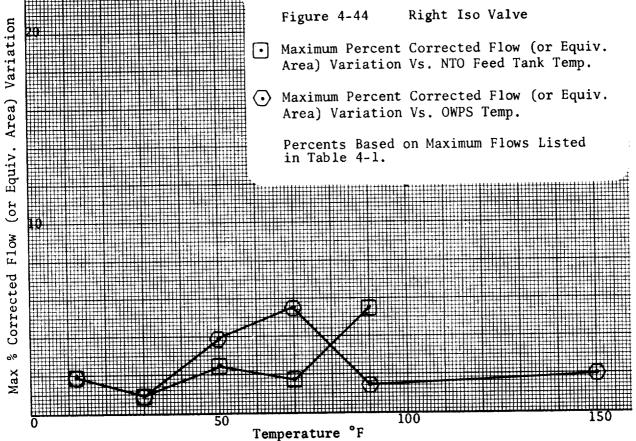


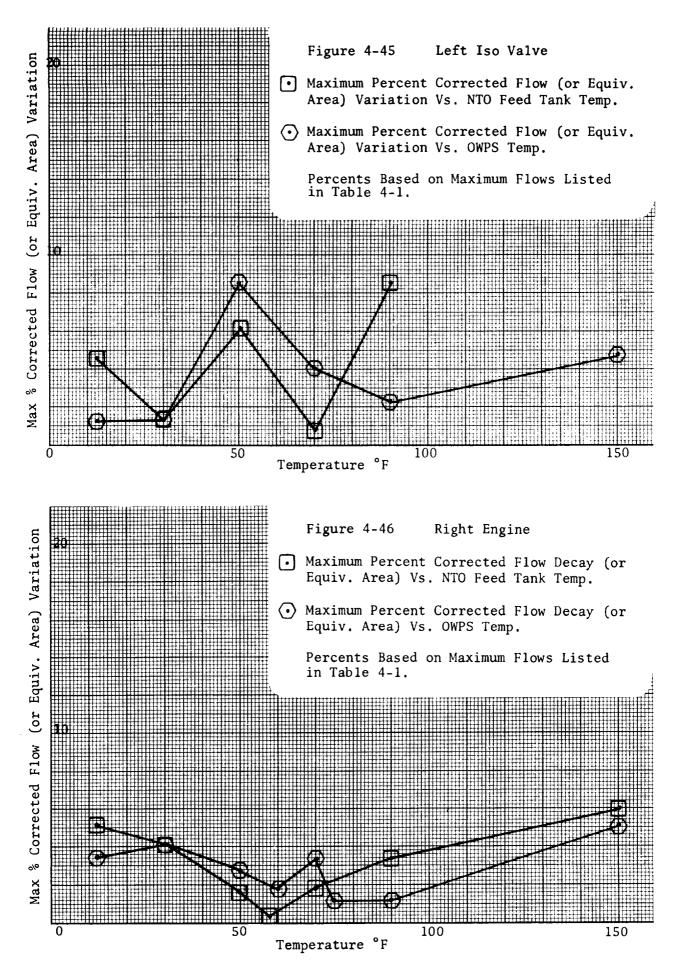
4-48

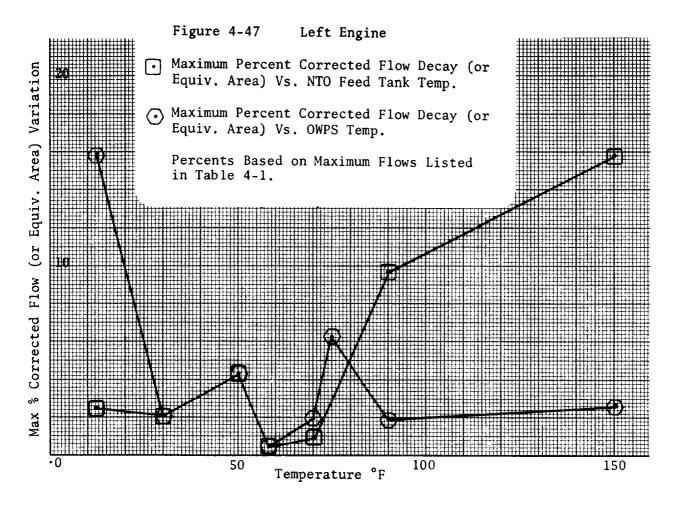


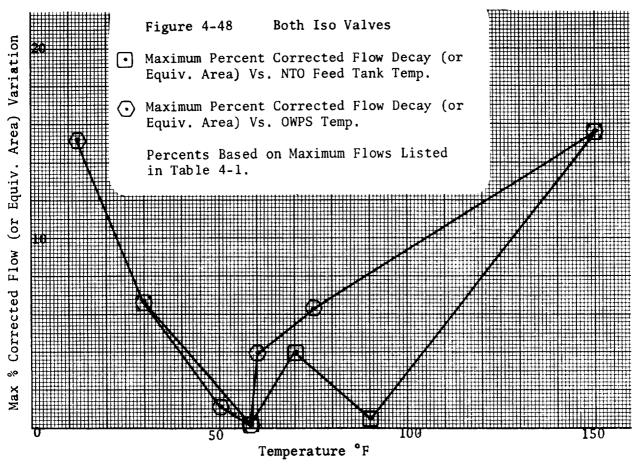


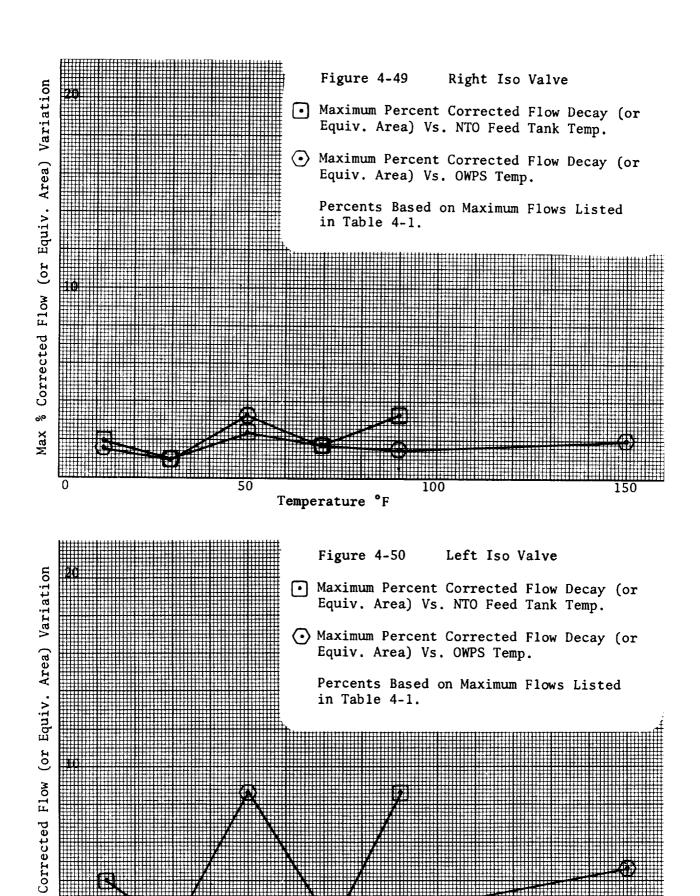












Temperature °F

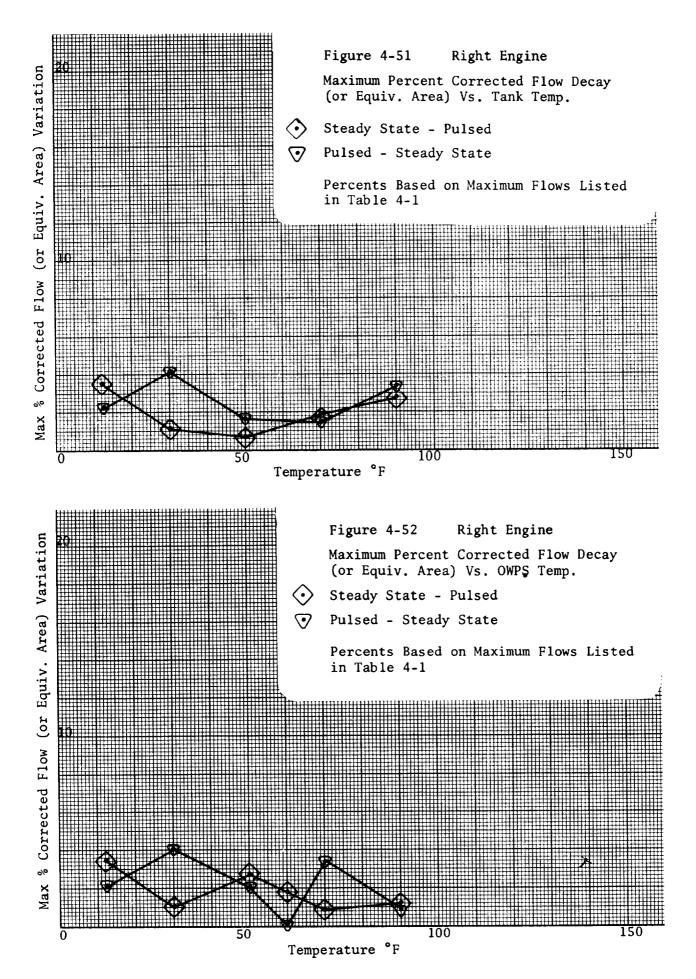
100

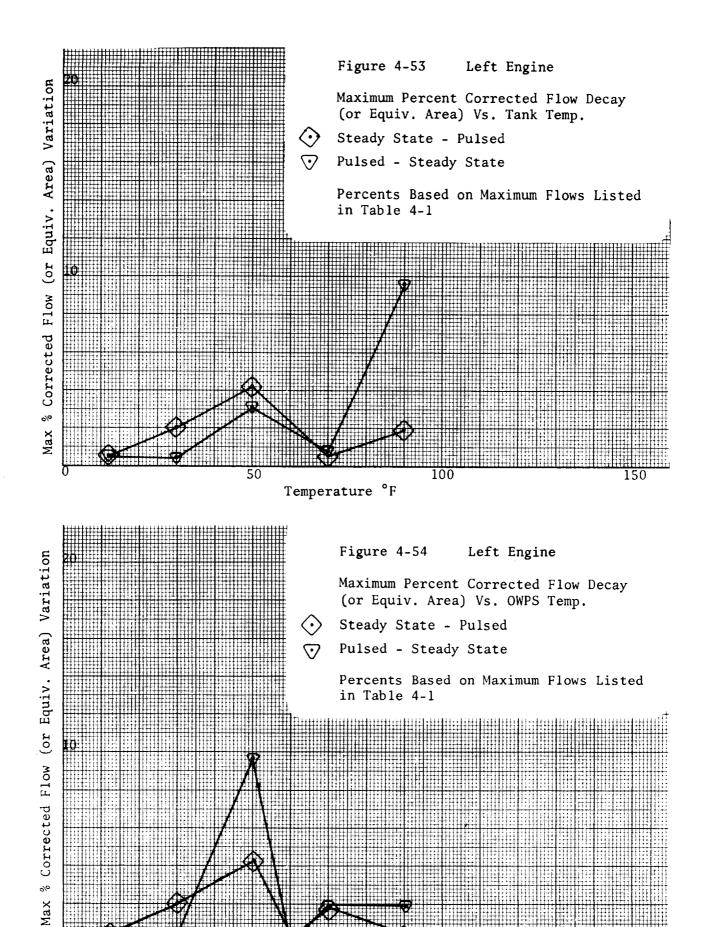
150

50

%

0





Temperature °F

100

50

## 4.2 FLOW TEST RESULTS - CHEMICAL ANALYSES

## 4.2.1 Nitrogen Tetroxide Analysis

The results of the chemical analyses of nitrogen tetroxide used in the flow tests are presented in Table 4-3. All propellant loaded into the feed tank was double filtered, first through a nominal  $10\mu$  filter, and then through a nominal  $5\mu$  filter. After each filling, the filter assembly was examined for material captured by the filters during transfer. In each case, the  $10\mu$  filter had red to black-brown particulate material on the filter screen. Microscopic examination of the  $5\mu$  filter showed little or no contamination. Figures 4-55 through 4-60 are photographs of the contaminants on the  $10\mu$  filter and loose material found in the filter housing from the first two loadings. The filters were cleaned to TRW Specification PR 2-2 level 2 prior to use.

After each filling, a sample was drawn and analyzed for base point reference. Samples were taken at each temperature operating point and during selected runs where anomalous flow behavior was suspected. The sampling location was just downstream of the engine as shown in Figure 2-2.

The routine analyses of the propellant indicated that the propellant stayed within use specification over entire test sequence. Some variation in NO content was noted from the flow test specimens, but it is felt that the variation was due to an insufficient purge of some of the sample cylinders, resulting in oxidation of some of the NO to NO<sub>2</sub>. This was corroborated by the periodic analyses of the feed tank, which indicated that little variation in NO content had occurred at the source.

The variation in particle count in both the run tank and test system indicated that the cycling temperatures and/or NTO dwell times have caused a certain amount of feed tank contamination to be built up. Of particular interest was the large build up in particle count from the first filling (sample log 54), before the feed tank had been conditioned, and the second filling (sample log 60) after the conclusion of the 150°F feed tank runs.

Table 4-3. Results of Chemical Analyses of Nitrogen Tetroxide From Run Tank and Flow Tests

	>250µ/ 50u Fibers	-						in the second			32/2 96				12 0/2F								5 1/3F	5 1/3F					
Count	10-25µ  25-50µ  50-75µ  75-100µ  100-250µ	2									12	_			15								24			4	4	4	4
Particle Count	75-10	ļ																											
-	1 50-75	20	0 1 ,040	2 109							150				108								15						
	r. =	18	3,0								886				260								48						
ļ 	10-25	09	4,000	1,050	2,500	700					1.832	1,425			1,195								190	190	190	190	190	190	190
tals	5	2.3	8.0		_	1.2					13.2		_			9.0		ni1			_		1.3						
Dissolved Metals Content, ppm	J 5	N. A.									l nil					4 0.2		3 0.4					3 <0.1						
Dissol Conte		4.4 1.1	1.6 1.0	1.6 0.3		0.3 nil				_	7 0.1				_	5 0.4	_	9 0.3					6 0.3			<u>v</u>			
	le Fe	-									2.7					3.5		6.0					3.6						
Non-Volatile Residue mg/l	Acetone	N.A.	258.5	27.5	31.5	19.5						22.5				38.4		1.0	_			_	17.5	17.5	17.5	17.5	9.0	9.0	9.6
Non-Volati	Kater Soluble	29.0	13.5	16.5	1.5	30.5						7.0				28.8		0.5				0	10	01	4.0	10 4.0	4.0	4 . 0	4.0
	Particulate Weight mg/l	0.5	1.0	< 0.5	.5.	6.0	N.A.	N.A.	N.A.	N.A.	1.0	1.5	2.5	0.5	1.5	1.0	N.A.	< 0.5	10.5	0.5	3.5	5.5		3.5	3.5	3.0	3.5 3.0 6.0 4.0	3.5 3.0 0.5 0.5 0.5	3.5 0.6 0.9 0.5 0.5
Chloride or NOC1	E/W	0.02	0.015	0.000	0.011	0.005												600.0				0.007							
Water	Equival.	0.05	0.08	0.11	0.11	0.11	0.10	0.09	0.09	N.A.	60.0	0.10	0.10	60.0	0.11	0.11	0.11	0.11	0.11	0.11	0.11	0.12		0.11	0.11	0.11	0.11 0.11 0.11	0.11 0.11 0.11 0.11	0.11 0.11 0.11 0.11 0.11
Assay	N/N %	0.62	0.70	0.58	0.56	0.59	0.45	0.35	0.51	0.46	0.30	0.67	99.0	0.64	0.61	0.61	0.41	0.62	0.53	0.53	0.61	0.54		0.42	0.42	0.42	0.42 0.42 0.47 0.39	0.42 0.42 0.47 0.39	0.42 0.42 0.39 0.38
Assay (		99.25	98.76	99.13	99.21	99.29			_		-						_					99.43	-	-					
Density A		1.420 9	N.A. 9	1.423 9	1.420 9	1.420 9									_	<u>-</u>						1.420 99	_						
	Run No.	Tank fill	Tank fill	Tank fill		Fank fill Art. Aged NTO	-	2	'n	2	9	7	6	12	15	17	18	19	20	22			29		31	3.3 b	33 35 35	31 35 <sup>b</sup> 37 <sup>b</sup>	3.1 3.5 3.5 4.7 3.9 9.
e e							53	55	56	57	28	59ª	61	62	63	64 <u>a</u>	9	99	75	76	77	78	80		81	81	81 86 87	81 86 87 88	81 87 88 89
Sample	Log	54 <del>a</del>	60 <sup>a</sup>	7.4	83	87	S	L/)	.,																				

 $\underline{a}$  Samples for dissolved metals content were not filtered before analysis.  $\underline{\underline{b}}$  Artificially aged NTO test runs.

1		

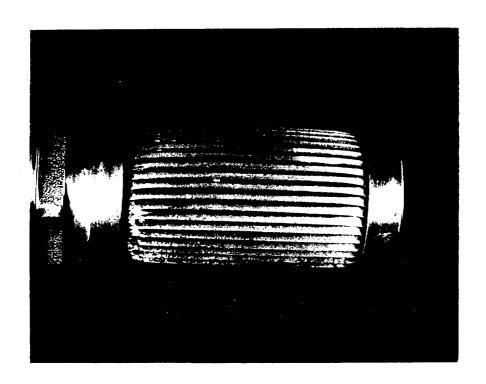


Figure 4-55. Photograph of Nominal  $10\mu$  Filter After First Propellant Loading (Approx. Magnification: 1X)

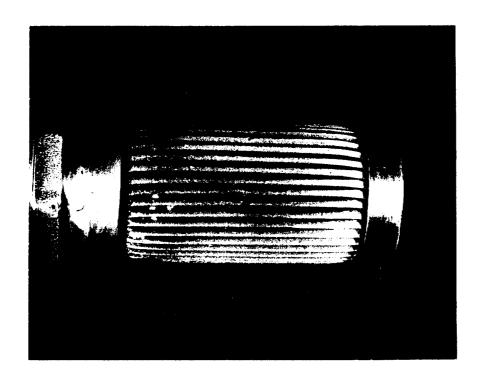


Figure 4-56. Photograph of Nominal  $10\mu$  Filter After First Propellant Loading (Approx. Magnification: 1X)

I		

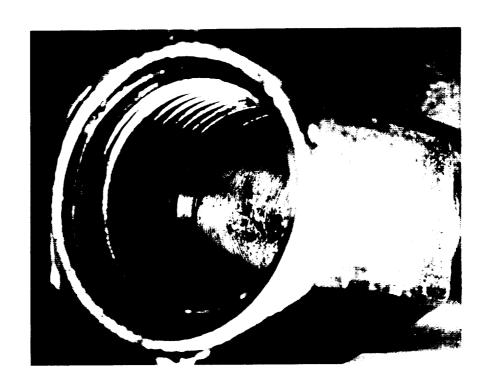


Figure 4-57. Photograph of Filter Housing After First Propellant Loading (Approx. Magnification: 2X)

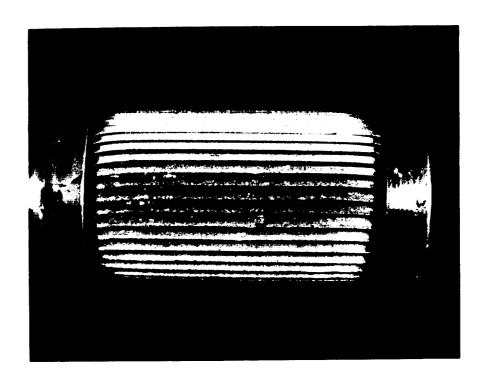


Figure 4-58. Photograph of Filter After Second Propellant Loading (Approx. Magnification: 1.5X)

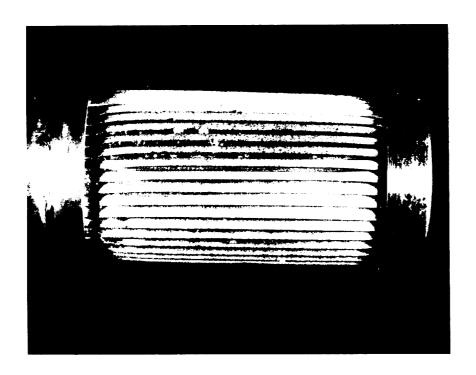


Figure 4-59. Photograph of Filter After Second Propellant Loading (Approx. Magnification: 1.5X)

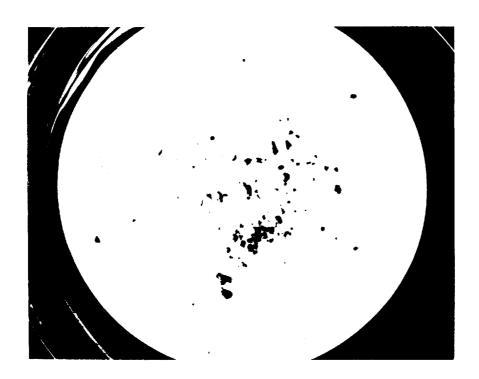


Figure 4-60. Photograph of Material From Filter Housing After Second Propellant Loading (Approx. Magnification: 1.5X)

The particle count became lower on successive fills, since the feed tank was nominally conditioned only between 30°F and 90°F. It is felt that this behavior simulates the contamination mechanism which might exist in the actual OWPS nitrogen tetroxide storage tank.

## 4.2.2 NTO Contamination Analysis

Because of the large flow variations experienced in the 150°F and the 12°F feed tank runs, the test system was dismantled after each series of runs, the trapped NTO drained and filtered, and each component backflushed with Freon TF. The residue was caught on Millipore filter paper. Table 4-4 illustrates the particulate weights found in the test system after each run series. Figure 4-61 shows the filter pad from sample point 7(b).

The filter from sample point 7(a) was scraped and the residue analyzed by a micro KBr infrared technique. The spectra obtained gave an indication of OH and NO<sub>3</sub> anions and indicated that the residue consisted mainly of hydrated metal nitrate salts. Sample points 1, 3, 6 and 7(b) were analyzed by X-ray fluorescence and infrared techniques. The infrared analyses again indicated metal nitrate salts. X-ray analyses identified iron in all samples, plus chromium in sample point 3(b) and chromium, nickel, and zinc in sample point 7(b).

The second phase liquid found at sample points 6 and 7(a) was dissolved in water and analyzed for metal content by atomic absorption spectroscopy. The results are presented in Table 4-5. The numbers are indicative of relative amounts only since the initial sample sizes were not known. Analysis of the samples by the Brucine method gave a positive nitrate test, thus, the materials were probably metal nitrates.

In addition to the contaminants found in the OWPS test system, special analyses were performed on the acetone soluble NVR samples from sample log numbers 60 and 64 and on the particulate weight filter paper from sample log 75.

Table 4-4. Particulate Weights from Disassembled Test
System Components and Trapped Nitrogen Tetroxide

	Sample Point	Particulate Weight, mg <sup>a</sup>	Particulate Weight, mg <sup>b</sup>
1.	Backflush from first filter	0.1	0.7
2.	Backflush from isolation valves	1.9	1.1
3.	Backflush from second filter	0.2	1.1
4.	Backflush from right engine	0.4	0.2
5.	Backflush from left engine	0.5	0.1
6.	N <sub>2</sub> O <sub>4</sub> from first filter inlet part	3.4 <sup>c</sup>	2.5
7.	Combined N <sub>2</sub> O <sub>4</sub> from engine inlets	2.4 <sup>c</sup>	2.3 <sup>d</sup>
8.	N <sub>2</sub> O <sub>4</sub> from downstream of both engines		0.4 <sup>c</sup>

a From runs culminating in 150°F feed tank to 12°F test system

 $<sup>^{\</sup>rm b}$  From runs culminating in 12°F feed tank to 12°F test system

 $<sup>^{\</sup>rm c}$  Transparent globules of a second phase liquid found in the N $_2$ O $_4$  . The second phase was insoluble in N $_2$ O $_4$  or Freon but was soluble in water.

 $<sup>^{\</sup>mbox{\scriptsize d}}$  As c, except additional tan colored residue on filter.

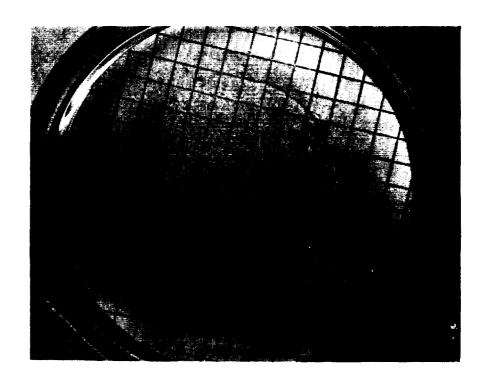


Figure 4-61. Filtered Residue from Sample 7(b) (Approx. Magnification: 2X)

Table 4-5. Analysis of Nitrogen Tetroxide Insoluble Liquid Found in OWPS Test System

	<u>Metals, μg</u>						
Sample	<u>Fe</u>	Ni	Cr	<u>Cu</u>	Zn		
6(a), N <sub>2</sub> O <sub>4</sub> insolubles from first filter inlet part	125	165	45	10	44		
7(a), N <sub>2</sub> O <sub>4</sub> insoluble from right engine (a)	162	37.5	33	7.5	31		
7(a), N <sub>2</sub> O <sub>4</sub> insolubles from left engine (a)	5.0	17.5	12.5	5.0	42.5		

<sup>(</sup>a)  $N_2^00_4$  portion combined for total sample point 7(a) in Table 4-3.

The acetone soluble NVR samples were analyzed by infrared spectroscopy.

The resultant spectra consisted of organic constituents and nitrates which may or may not be organic in nature. The organic portion gave indications of alkyl, aryl, hydroxyl, and carboxylic acid groups.

The filter pad from sample log 75, which had the highest particulate weight found, was first analyzed by X-ray fluorescence, and showed an indication of iron. The pad was then cut in half and the two sections rinsed with water and isopropanol, respectively.

The alcohol rinse gave an infrared spectrum which correlated to the spectra obtained from the NVR residues. The water rinse produced a red-brown residue which yielded an infrared spectrum indicative of a nitrated metal salt.

Since the results from the NVR and particulate weight analyses from various samples of NTO were similar, it is indicated that the NVR material, in particular the organic components, may saturate (under certain conditions) to such an extent that some of the material may be suspended in the NTO, as well as being in solution, and aggregate into particles larger than  $10\mu$  under operating conditions and temperatures. Since NVR contaminants have been found in fresh specification grade propellant in concentrations varying from 50~mg/1 to 350~mg/1 (Reference 2), the origin of the material is uncertain.

## 4.2.3 Analysis of the Crystalline Material

In an attempt to determine the nature and formation of the crystalline material found in the compatibility tests as described in Section 4.4, and to elucidate the flow anomalies found in the 12°F feed tank to 12°F or 150°F system runs, a series of experiments were performed on both specification nitrogen tetroxide and the one sample (sample log 58) that had the highest indicated copper content. There were two types of crystals formed upon cooling the NTO, these were white and blue-green in color.

The blue-green crystals were formed at 1°C above the freezing point of NTO, and would not redissolve upon rewarming the solution to 55°C. The crystals were collected by filtration and analyzed by atomic absorption and infrared spectroscopy. These crystals were extremely deliquescent and were analyzed as an aqueous solution. Atomic absorption analysis gave  $47.6\mu$  g of copper, correlatible to the estimated amount of original sample collected. Infrared spectra indicated only the presence of nitrates. From the analyses, and the original color of the crystals, it is concluded that the contaminant was anhydrous cupric nitrate. It has been noted, however, that Cu  $(NO_3)_2 \cdot N_2O_4$  has been prepared (Reference 14), thus the material may have had NTO coordinated to the parent compound. Other than the small amount noted in the compatibility tubes, all other attempts to obtain similar material from samples other than sample log 58 were unsuccessful.

The white crystalline material was obtained at -11.7°C (the total solution freezing point was -12.7°C). These crystals redissolved upon warming, and were collected by decanting the supernatent NTO at -12.0°C. The crystals, upon melting, turned into a dark brown liquid and were analyzed for comparison with the starting material. The comparative analysis is given in Table 4-6. Infrared spectrophotometric scans of the material and specification grade NTO gave essentially identical spectra.

The analyses performed on the white crystalline material tend to disprove the theory that the material is either a ternary phase of  $HNO_3$ ,  $H_2O$ , and NO, or a binary phase of  $HNO_3$  and  $HNO_2$ , but rather indicate a phase of nitrogen tetroxide. The presence of active nucleation sites in NTO could cause the nitrogen tetroxide to freeze at a temperature higher than the normal freezing point, however, the source or composition of the nucleating material is unknown at this time, and while the precipitation of a white crystalline material has been observed before at TRW Systems Group, this phenomena presently seems random in occurrence.

Table 4-6. Comparison of MSC-PPD-2 Nitrogen Tetroxide and the Higher Freezing Point White Crystals

Analysis	Starting NTO	Higher Freezing Crystals
$N_2O_4$ assay, % w/w	99.21	99.28
Chloride as NOC1, % w/w	0.011	0.007
NO content, % w/w	0.56	0.47
Metals, ppm		
Fe	1.5	0.8
Ni	0.4	ni1
Cr	nil	0.2
Cu	4.6	3.0

#### 4.3 NITROGEN TETROXIDE AGING STUDY RESULTS

Analysis of the NTO before cycling showed that the propellant was in specification, with a nominal dissolved metal content. After aging, the iron, nickel, and chromium content had increased, while the copper content had decreased slightly. Table 4-7 shows a comparison of the metals content before and after thermal cycling. The reduction in dissolved copper content is probably due to precipitation during thermal cycling, as was observed in the compatibility and freezing point tests.

A materials balance calculation was made, based on the aged NTO, in order to determine the additional amount of iron necessary to dope the NTO in the run tank to approximately the same level as the aged propellant. Doping with nickel and chromium were not considered, based on the results from the previous study performed for JPL on possible NTO contaminants (Reference 2). The iron was added as the Addison adduct,  $NO \cdot Fe(NO_3)_4 \cdot n N_2O_4$  which was prepared by reacting a solution of anhydrous ferric chloride in ethyl acetate with NTO, stripping off the ethyl acetate, and resuspending the reaction product in NTO.

Table 4-7. Metal Content of Nitrogen Tetroxide Used in Aging Study

Concentration, ppm

Metal	Original NTO	NTO After Thermal Cycling
Iron	1.5	3,4
Copper	4.6	0.8
Nickel	0.4	1.6
Chromium	nil	0.8

Both the aged propellant and the iron dopant were added to the run tank, with filtration as done previously. Figures 4-62 and 4-63 show the material caught on the filter. Considerably more material was removed in the filter than in previous tests, as shown by a comparison of Figures 4-55 through 4-60. Additional specification grade NTO was added to the run tank to completely load the system, and the NTO was allowed to equilibrate for forty-eight hours while being heated from approximately 70°F to 90°F.

Laser scattering tests on the doped and undoped NTO are shown in Figures 4-64 and 4-65 and indicate a slightly larger Tyndall effect in the doped NTO. It could not be determined if the scattering material was suspended particulate material or colloidal in nature. Analysis of the NTO in the run tank showed a smaller iron content than calculated. Since the samples for metals analysis are filtered, as explained in Section 3.4, it is inferred that the majority of the iron in the NTO was in the form of suspended particulate matter.

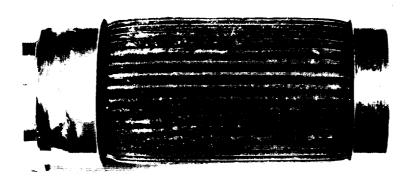


Figure 4-62. Photograph of  $10\mu$  Nominal Filter from Loading of Artificially Aged Nitrogen Tetroxide (Approximate Magnification: 2X)



Figure 4-63. Photograph of Material in Filter Housing From Loading of Artificially Aged Nitrogen Tetroxide (Approximate Magnification: 2X)

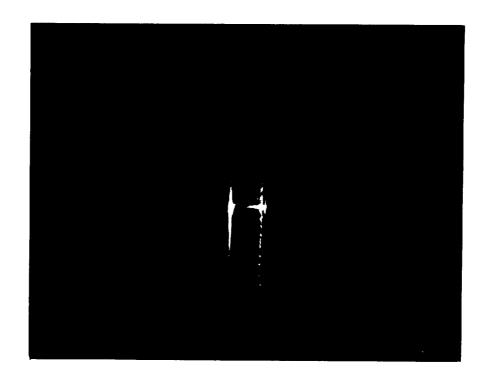


Figure 4-64. Tyndall Light Scattering Effect in Specification Grade Nitrogen Tetroxide Using He-Ne Laser

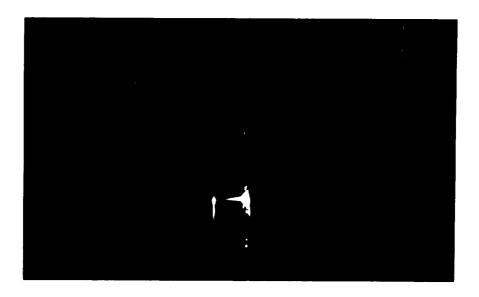


Figure 4-65. Tyndall Light Scattering Effect in Artificially Aged Nitrogen Tetroxide Using He-Ne Laser

### 4.4 NITROGEN TETROXIDE - BRAZE ALLOY COMPATIBILITY STUDY RESULTS

## 4.4.1 Nitrogen Tetroxide Analysis

The compatibility tubes were examined after termination of the thermal cycling test, and again, both white and blue-green crystalline material was noted in the bottom of the tubes. Figures 4-66 and 4-67 show the compatibility tubes, samples, and crystals. Some distortion is due to the lighting, moisture condensation, and imperfections in the glass, but the crystals are apparent in the bottom of the tubes. Because of the crystalline material, two types of analyses were performed on the NTO: analysis of the NTO fluid proper, and analysis of the crystalline material formed during the thermal cycling test. There was an insufficient amount of the blue-green crystals to be analyzed separately.

Two methods were used in an attempt to obtain the crystals for analysis: filtration through a Millipore filter, and aspiration of the NTO, leaving the crystals in the tube.

In each case, the crystals quickly deliquesced and were analyzed as a liquid. X-ray fluorescence indicated the presence of copper and iron in both samples, and in addition, nickel, manganese and chromium were found in compatibility tube No. 1. Table 4-8 gives the results of atomic absorption analyses of the material from compatibility tube No. 1.

Table 4-8. Metal Content of Crystalline Material from Compatibility Tube No. 1

Metal	Weight, μg
Copper	3.5
Nickel	5.0
Manganese	0.5
Chromium	4.0
Iron	4.0

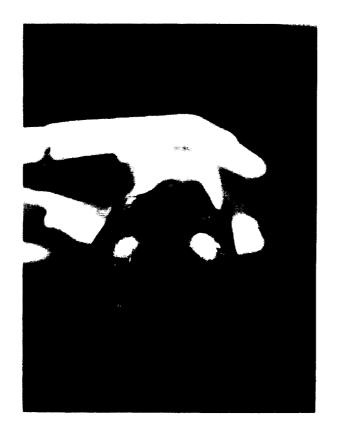




Figure 4-66. Compatibility Tubes, Samples, and Crystals





Figure 4-67. Compatibility Tubes, Samples, and Crystals

These values are relative, since the original weight of the crystals could not be determined due to the liquification. The infrared spectrum of the liquid suggested that the metals were present as nitrates, but the results are inconclusive since considerable change had occurred in the crystals upon removal from the compatibility tubes.

The NTO freed from the crystals was analyzed for dissolved metal content. The results are presented in Table 4-9 and are compared to the original NTO used in the tests.

Table 4-9. Metals Analyses of Nitrogen Tetroxide Used in NTO-Braze Alloy Compatibility Tests

Concentration,	ppm

Metal	Original Unaged Nitrogen Tetroxide	NTO from Tube No. 1	NTO from Tube No. 2
Iron	1.4	2.9	3.5
Copper	4.7	0.7	0.9
Nickel	0.1	0.7	0.2
Manganese	nil	0.2	0.2
Chromium	nil	nil	ni1

# 4.4.2 Braze Alloy Analysis

The original strip of braze alloy was cut into two, 1-1/2" x 1/2" test sections, with the center section reserved for metallurgical examination. The samples were degreased, ultrasonically cleaned, and then weighed, measured for thickness, and their surfaces photographed. Figures 4-68 through 4-71 show the original surface and the transverse and longitudinal cross-sections.

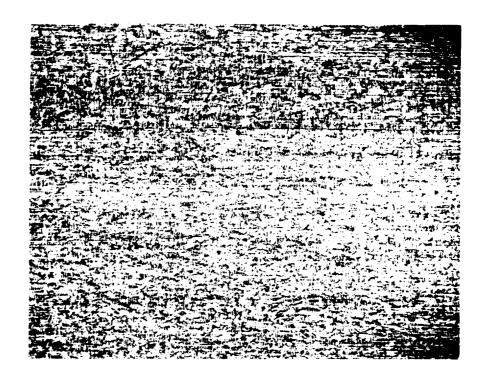


Figure 4-68. Photograph of Typical Surface of Braze Alloy Before Test (Approx. Magnification: 50X)

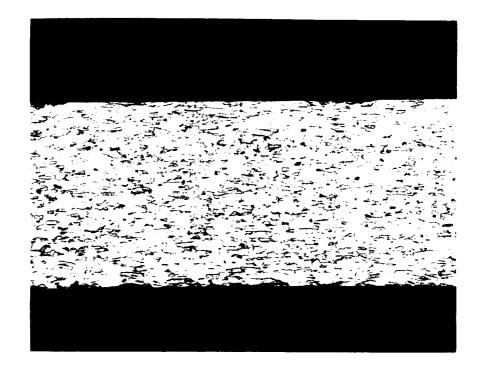


Figure 4-69. Photomicrograph of Transverse Cross-Section of Braze Alloy Before Test (Approx. Magnification: 200X)

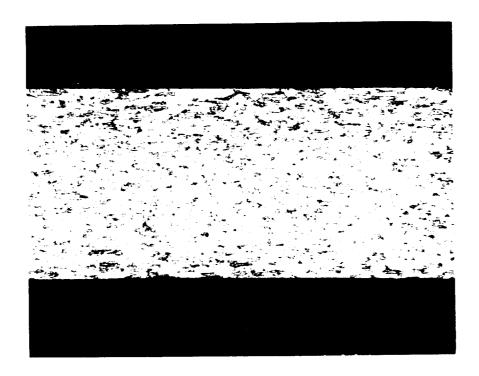


Figure 4-70. Photomicrograph of Transverse Cross-Section of Braze Alloy Before Test (Approx. Magnification: 200X)

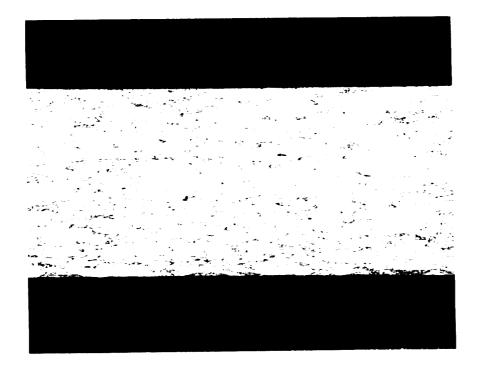


Figure 4-71. Photomicrograph of Longitudinal Cross-Section of Braze Alloy Before Test (Approx. Magnification: 200X)

The specimens were rinsed with distilled water after removal from the compatibility tubes, and the surfaces rephotographed. Figures 4-72 through 4-74 show that the surface had picked up a deposit, but the deposit was too thin to analyze. After photographing the surfaces, the samples were cleaned as before, and weighed and measured. There was no measurable change in weight or thickness, and the cleaning had removed the previously described deposit. Microscopic examination of the surfaces showed no signs of pitting, cracking, or other corrosive attack by the NTO. The samples were then sectioned and the transverse and longitudinal cross-sections were metallurgically examined. Figures 4-75 and 4-76 show the transverse and longitudinal cross-sections after thermal cycling in NTO. No evidence of intergrannular cracking or surface attack was apparent.

The results indicate that minimal interaction had occurred between the NTO and the braze alloy over the test duration, although the presence of a surface deposit and the increase in the metals content in the NTO suggests that some reaction had taken place. This finding is corroborated by the test results from the Martin Marietta propulsion sterilization program sponsored by JPL/NASA (Reference 10), in which it was found that high nickel content alloys such as stainless steels exhibited considerable reaction with NTO at 275°F within 600 hours. This reaction generated substantial quantities of an undesirable viscous product, with the composition varying depending on the alloy tested. Such viscous products could cause clogging of filters and fine orifices.



Figure 4-72. Photograph of Braze Alloy Surface Deposits After Test in "As-Received" Condition (Approx. Magnification: 50X)

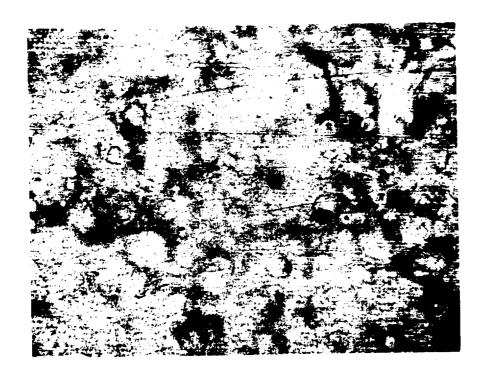


Figure 4-73. Photograph of Braze Alloy Surface Deposit After Test in "As-Received" Condition (Approx. Magnification: 50X)

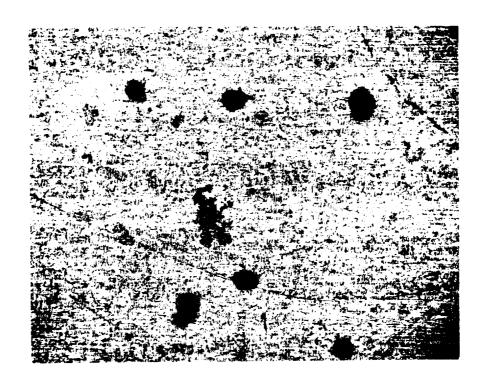


Figure 4-74. Photograph of Braze Alloy Surface Deposit After Test in "As-Received" Condition (Approx. Magnification: 50X)

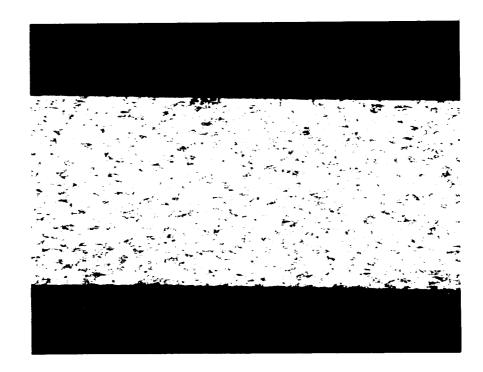


Figure 4-75. Photomicrograph of Transverse Cross-Section of Braze Alloy After Test (Approx. Magnification: 200X)

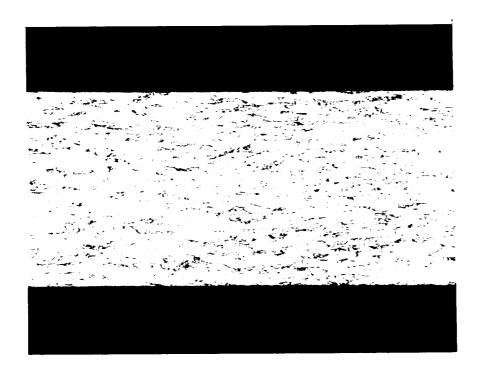


Figure 4-76. Photomicrograph of Longitudinal Cross-Section of Braze Alloy After Test (Approx. Magnification: 200X)

#### 5.0 CONCLUSIONS

The conclusions presented are based on the testing described in Sections 3 and 4 and cannot be indiscriminately applied to other environmental conditions or other systems. These conclusions are:

- 1. Flow decay and other flow anomalies of up to 10 percent may be expected during flow of specification grade nitrogen tetroxide when system and propellant temperatures are between 90 and 50°F.
- 2. Flow anomalies and flow decays are more prevalent and more serious when operating from a hot feed tank to cold OWPS than during isothermal runs, if only flow decays exceeding two percent are considered to be significant, and the temperature range of interest is limited to between 90 to 50°F.
- 3. Flow anomalies and flow decays between 90 and 50°F are greater and more frequent when operating in a pulsed flow followed by steady state flow mode than when flowing in the steady state-pulsed mode.
- 4. Three clogging mechanisms have caused the flow anomalies and flow decays observed in this test program. These are:
  - a) Formation of gels from solvated colloidal particles under flow as suggested in References 2 and 9.
  - b) Generation of flow degradation products due to propellant saturation at high temperature followed by precipitation or coagulation of these products at lower temperatures.
  - c) Formation of flow degradation products by crystallization or freezing at temperatures above the normal NTO freezing point.
- 5. The greatest flow variations encountered are in the extreme temperature test cases, namely 150°F feed tank to 150°F and 12°F OWPS and 12°F feed tank to 150°F OWPS.

- 6. Flow variations at the 150°F 150°F run conditions were probably caused by generation and accumulation of contamination during feed tank warmup to 150°F. This is supported by the large initial flow fluctuations observed after flow which then slowly stabilized as the material was washed through the system.
- 7. Flow variations during the 150°F 12°F run conditions are attributable to both particulate accumulation and gel formation, since both types of material were found upon system teardown and inspection.
- 8. Flow variations during the 12°F 150°F run conditions are probably attributable to formation of precipitates in the feed tank at the low temperature operating condition, which reliquified as the NTO flowed through the warm OWPS. The shape of the flow curves indicate an initial decay with a gradual leveling off of flowrate and chemical tests indicate that the main precipitate liquifies below room temperature, confirming that this precipitate is the main cause of these flow anomalies. It is assumed that the 12°F 12°F test runs did not exhibit the same magnitude of flow anomalies that the 12°F 150°F runs did because of depletion of the precipitate from the feed tank due to the previous runs. Insufficient NTO was present in the OWPS itself to generate significant quantities of the precipitates and cause a large variation in the flowrate through the isolation valves and engines.
- 9. The flow tests utilizing artificially aged propellant generally behaved similarly to those using specification grade nitrogen tetroxide, except for one isothermal run at 50°F. It is assumed that particulate contamination was responsible for this flow variation.

#### 6.0 RECOMMENDED PROBLEM SOLUTIONS

The mechanisms involved in flow decay within a system include buildup of clogging material when the NTO is subjected to high shearing velocities and/or differential temperatures, and static buildup of potential clogging material in the system from interaction between the NTO and the system. The former mechanism requires flow to occur while the latter forms statically and then physically causes flow variations or decay when the NTO is subsequently displaced by flow. A total solution should consider both of these mechanisms, therefore, a combination of "solutions" must be applied be eliminate overall system flow problems.

Several potential solutions are outlined below:

- a. Cold filtration to reduce contaminant level.
- b. Use of materials of construction which do not cause a buildup of flow decay products.
- c. Elimination of small orifices, clearances, and filters,
- d. Tight temperature control of system and propellant.
- e. Dissolution or breakup of contamination products so they will pass through orifices, clearances, and filters.

Dissolved or finely suspended contaminants can be removed to a lower contaminant level by chilling the propellant and then cold filtering with a finer mesh size filter than those used in the system. This technique should reduce the contaminant level and allow more severe operating conditions such as shearing velocities or temperature gradients than would normally cause flow variations and decay. This solution is susceptible to the resaturation reactions which occur at higher temperatures with most materials presently used in the OWPS. This saturation time varies with the material used, and the propellant.

Certain materials cause more flow degradation product buildup than others. Nickel bearing alloys such as 18-8 stainless steels produce gel-like materials when exposed to NTO at elevated temperatures. Certain aluminum and titanium alloys are the least susceptible to NTO attack (Reference 10).

The use of stainless steel alloys, particularly in the regions of high service temperatures, should be avoided.

In-system filtration should be limited to protection against the largest tolerable particle. Injector and valve orifices should be kept as large as possible, and where filters are necessary upstream of such components, the filtration area should be made as large as is possible. In the OWPS unit tested, it is recommended that the internal filters in the isolation and engine valves either be eliminated or else increased in both filter area and pore size. The two large system filters in the OWPS showed no significant signs of degrading system flow, even though their micron rating (15 $\mu$  absolute) was finer than the filter strainers in the isolation and engine valves (10 $\mu$  nominal - 25 $\mu$  absolute).

The percent corrected flow curves presented in Section 4 show minimal flow variation during isothermal flow runs. Thus, generation and/or precipitation of flow degradation products should be minimized by tight temperature controls on the NTO supply tank and the rest of the OWPS, since flow degradation products from a saturated solution are precipitated at low temperatures and the system may resaturate itself from NTO/system materials interaction at high temperatures. It is recommended that the system be maintained at as constant a temperature as possible throughout its operating life. The use of passive thermal control techniques and coatings to accomplish this should be investigated.

Some chemical and physical techniques (References 2 and 4) have been attempted to either keep flow degradation products in solution during flow, or to remove them after formation. This work has resulted in possible short term solutions to the flow decay problem. Mechanical excitation of the flow system components is a potential method of breaking up the flow decay products and thus minimizing flow degradation. It is recommended that the use of ultrasonic excitation of the filters and/or orifices be investigated as a method of preventing the formation or accumulation of flow degradation products.

#### 7.0 RECOMMENDED INVESTIGATIONS

The test program performed indicates that a 9 percent variation in MSC-PPD-2 NTO flow, and an 11 percent variation in artificially aged NTO flow can occur over the 90 - 50°F temperature range which encloses the expected system operational temperature spectrum. These variations were found during "cold flow" tests as described in Sections 3 and 4. It is felt that hot or simulated hot firing tests could cause a much more serious clogging problem. This is confirmed by the findings of JPL Contract 951709, Reference 10, which indicated a buildup of gel-like material on nickel bearing metal surfaces at temperatures of 275°F. Therefore, flow testing with hot firings or simulated hot firings, where actual firing temperature gradients are reproduced, is recommended for this system.

It is felt that further aging studies including the presence of all materials of system construction are warranted. This is particularly true in terms of the results of the experiments described in Reference 10. Investigations of flow with propellant artificially saturated with nickel-NTO compounds is recommended.

The blue-green crystals observed during the flow runs and temperature cycling tests of this program could cause a problem in systems exposed to temperature cycling as they form at the low temperature end of the cycle and do not redissolve at the high temperature end. This could possibly cause a gradual buildup of crystalline matter which could clog fine orifices or filters. The formation mechanics, composition, and possible elimination of these crystals require further study.

The observed white crystalline matter, which forms at approximately 1°C above the freezing point, could cause problems in systems exposed to temperatures near the freezing point of NTO. The composition and formation mechanics of these crystals should be studied further, particularly the influence of such variables as water content, NO content, dissolved metals content, and dissolved polymers and organics. It is possible that some of these could

raise the freezing point further, requiring systematically higher operating temperatures.

The braze alloy corrosion studies were limited to samples of the braze alloy only. While these showed minimal braze alloy attack, the corrosion experienced in an actual brazed assembly could be significant due to the corrosion couples formed. These effects should be examined further, particularly at elevated temperatures, before brazing is used in a flight system.

The areas of recommended further investigation are:

- Hot (or simulated hot) firing flow tests
- Artificial propellant aging study with all system construction materials
- Study composition and formation mechanics of bluegreen crystals
- Study composition and formation mechanics of white crystals
- Study actual braze point corrosion, and long term corrosion of other system materials in combination.

#### 8.0 REFERENCES

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# APPENDIX I SUMMARY OF MARQUARDT MIR 272

#### ENGINE DESCRIPTION

The Marquardt Corporation Model R-1E-002 Rocket Engine is a hypergolic, bipropellant, pressure-fed engine nominally rated as delivering 22 pounds vacuum thrust at steady state operation. The thrustor components include solenoid valves which control the propellant flow to the single doublet injection element, injector head assembly, and a radiation cooled molybdenum thrust chamber. The solenoid valves are protected from possible contaminants by a 10 micron nominal - 25 micron absolute sediment strainer located upstream of the valve armature. ON-OFF propellant flow is controlled by actuating either the primary coils (Coil No. 1) or the coaxial redundant coils (Coil No. 2) of the solenoid valves. The engine is orifices by restrictors in the inlet fittings to operate at a steady state mixture ratio of 1.65 using monomethylhydrazine (MMH) fuel and nitrogen tetroxide ( $N_2O_4$ ) oxidizer at  $70^{\circ}F$ . It operates at a nominal chamber pressure of 95 psia.

#### ENGINE ENVELOPE

The critical dimensions of the Model R-1E engine are as follows:

Minimum clearance envelope diameter = 7.040 inches

Minimum envelope length = 10.405 inches

Nominal combustion chamber throat area = 0.1327 inches

Nominal thrust chamber exit area = 5.363 inches

#### ENGINE OPERATING REQUIREMENTS

The engine is orificed to operate at a thrust level of 22 pounds at the following propellant pressure and temperature conditions:

Nominal inlet pressure = 213 psia Nominal inlet temperature = +70 + 10°F  $\underline{\text{Maximum operating range}}$  - The engine may be operated at any combination of the following:

Maximum inlet pressure = 240 psia Minimum inlet pressure = 180 psia Maximum inlet temperature = +120°F Minimum inlet temperature = +20°F

The propellants may be pressurized with either helium or nitrogen gas, and may be 100% saturated with helium.

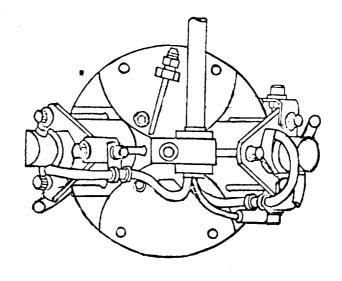
#### ENGINE VALVES

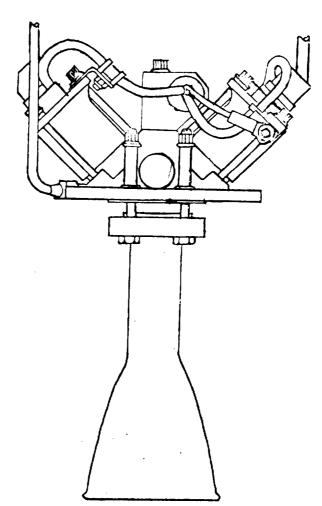
The valves may be actuated with a regulated d.c. voltage between 21 and 28 volts (nominal = 25 vdc). Either coil may be actuated, however, it is recommended that like coils always be used (both No. 1's or both No. 2's). The solenoid valves may be opened for any pulse width greater than 15 ms.

The propellant valves have the following nominal performance characteristics:

Opening response at 25 vdc and 203 psia inlet pressure	8 ms
Closing response at 25 mdc and rated flow	5.0 ms
Current draw at 28 vdc and 70°F	0.63 amp
Pull-in voltage at 70°F and 203 psia inlet pressure	10 vdc
Dropout current at operating conditions	0.2-0.14 amp
Dropout voltage at operating conditions	1.0-7.0 vdc
Resistance of Coil No. 1 at 75°F	43.6 ohms
Resistance of Coil No. 2 at 75°F	47.5 ohms
Maximum operating time at 28 vdc and rated flow	Unlimited

The engines as supplied for this program did not include the thrust chamber.





R-1E THRUSTOR

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# APPENDIX II

TEST PLAN AND PROCEDURE
NTO FLOW DECAY STUDY
CONTRACT NAS 8-21489

J. L. Reger, Principal Investigator

M, J. Makowski, Project Manager

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#### 1.0 OBJECTIVES

The objective of this test program is to determine if a flow decay problem exists in the Orbital Workshop Propulsion System.

#### 2.0 BACKGROUND

Flow decay and flow stoppage have occurred in nitrogen tetroxide (NTO) flow systems containing fine filters and small clearances. This flow degradation has been investigated by TRW Systems under NASA Contracts NAS 7-107 and NAS 7-549. The clogging mechanism has been postulated to be the solvation, coagulation and final precipitation of complex iron colloids from the solution with eventual drying of the gel resulting in a crystalline powder-like residue. The phenomenon appears as an increase in NTO viscosity in high velocity flow and seems to occur in areas of turbulence and constriction such as entrances to valves, filters, orifices and capillaries. Flow blockage was observed in both capillary and filter flow tests using MSC-PPD-2A NTO as well as propellant doped with metal ions likely to be found in an aged system. blockage was caused by a gel-like material found at the entrance to the capillary and filter which dried to a powdery crystalline residue. Changes in propellant temperature appear to be an important factor in inducing the flow decay process. The clogging material has been analyzed and found to contain iron complexes resulting from reactions between NTO, soluble impurities, and ferrous alloys used in constructing the system. Organic material has also been detected, which may synergistically contribute to the flow decay phenomenon. These analyses were performed utilizing infrared spectrometric, X-ray fluorescence and atomic absorption techniques.

#### 3.0 SCOPE

This procedure outlines in detail, a parametric study designed to determine if a flow decay problem exists in the Orbital Workshop Propulsion Systems components supplied to TRW by the George C. Marshall Space Flight Center. Test sequence, required instrumentation, test schematics, test procedures and propellant sampling techniques are described.

#### 4.0 COMPONENT CLEANLINESS

The NTO feed tank and any NTO wetted components in the NTO flow system upstream of the flowmeters (see Figure 1) will be cleaned to PR2-2 level 2. Gas pressurization or purge lines entering the test system or NTO feed tank upstream of the flowmeter will be cleaned to PR2-2 level 2 and a  $2\mu$  nominal  $10\mu$  absolute filter will be used at the point of attachment to the system.

#### 5.0 PROPELLANT USED (NTO)

The NTO propellant used in the initial series of tests will meet MSC-PPD-2B when loaded into the feed tank. NTO which has been naturally or artificially aged will be used for certain critical "Doped Propellant" tests as defined in the test matrix.

#### 6.0 OPERATING INSTRUCTIONS

These instructions are intended to describe each operating step in making the test flow runs, and include the system checkout and loading procedures to be utilized initially, or at such times that component replacement or system reclean is required.

#### 6.1 System Checkout

Pressure check the system upstream of the engine valves with helium at 300 psi. Pressure check the catch tank and lines downstream of the engine valves with nitrogen at 200 psi. Check for leaks using "Snoop" and repair any that are found. Note: This is to be repeated whenever a component is removed or replaced.

## 6.2 Nitrogen Tetroxide Loading Procedure

Attach the line from the NTO cylinder to the fill and drain port on the NTO feed tank. Open the sight gauge valves and ventline on the feedback. Slowly pressurize the NTO cylinder and observe the load level on the sight gauge. A one inch differential in the sight gauge level line corresponds approximately to one gallon of NTO. Load approximately fifty (50) gallons of NTO into the feed tank, which allows for ullage and thermal expansion of

the NTO during heating. Close the fill, vent, and sight gauge valves and drain sight gauge. Remove NTO cylinder and load line and attach a 500 milliliter sample bomb to the fill and drain lines. Pull a vacuum on the sample bomb and refill with dry GN<sub>2</sub>. Open the fill and drain valve on the feed tank and open the first sample bomb valve, then the second bomb valve, and fill the bomb with NTO, allowing a small (100 ml approximately) amount of NTO to exit the bomb. Close all valves, and send sample to the Analytical Chemistry Section for analysis. If the NTO is in specification, proceed to wet the complete test section as described in Section 5.3.

## 6.3 Test Section Loading Procedure

Leave the hand valve and remotely actuated valve isolating the feed and catch tanks closed and evacuate the test system. Open the hand valve and remotely actuated valve isolating the feed tank from the system. Apply approximately 25 psi helium pressure to the feed tank. Open system isolation valves and engine valves and allow the NTO to flow through the system. Open the catch tank isolation valve until approximately one inch of NTO shows in the catch tank sight gauge. Close the sight gauge and isolation valves on the catch tank. The system is now ready for pressurization and temperature conditioning.

# 6.4 Temperature Conditioning of NTO Feed Tank and Test System

Stabilize the feed tank and test system at their required temperatures. Utilize the proportional heating or cooling rate adjustment on the controllers to avoid overheating or cold shocking the strip heaters or test components. Monitor by use of thermocouples on tank, strip heaters, and test box. This will require activating the heating and/or cooling controllers on the day before testing in order to allow stabilization of the NTO feed tank and test system. Adjust the step function heat/cool cycle with respect to the NTO tank temperature probe and test system temperature probe such that the three operating temperatures are controlled as follows:

Hot test temperature: 150°F + 4°F

Ambient test temperature: 75°F + 4°F

Cold test temperature:  $12 + 6 \circ F$ 

Do <u>not</u> allow NTO or test system to cycle below 12°F. Once the required test temperatures are stabilized, the system is ready for the test flow runs.

# 6.5 Test Flow Runs

# 6.5.1 Long Duration (600 Second) Flow Runs

After proper temperature conditioning as indicated on the Test Matrix Table 1: Open the hand operated safety valves on both the NTO feed and catch tanks. Vacate the test cell and energize the warning lights. Energize the electrically actuated feed tank valve. Pressurize the NTO feed tank to 235 + 5 psig with gaseous helium. Use the pressure gauge for reference during pressurization, then utilize the pressure transducer for final adjustment. Pressurize the catch tank to 95 + 5 psig with gaseous nitrogen, using the same procedure as for the feed tank. All of the differential transducers have mechanical stops allowing some temporary overpressure during this phase. Activate instrumentation, actuate dual redundant valves, and then actuate the required number of NTO engine valves (e.g., activate engine 1, or engine 2, or use special switch to activate engines 1 and 2 simultaneously) per Test Matrix and engineering direction. Allow the run to go to completion. Continuously monitor the oscillograph channels for pressures, differential pressures and flow rates. If flow or differential pressure anomalies occur, mark the strip. At the end of the run, activate snap sample bomb valve(s) while maintaining flow rate. The sample bombs are to be evacuated and back filled with clean dry nitrogen just prior to each run per 5.6.

After completion of test run series, close the helium and nitrogen pressurant lines, close the electrically activated valve at the feed tank, and vent the feed tank to the NTO vapor pressure at the holding temperature. Vent the catch tank to its ambient pressure. Turn off warning lights, enter test cell,

TABLE 1. TEST MATRIX

Run	Components	Run Duration Sec	Hold Tank Temp. °F	Component Temp. °F	Flow Rate Lb/Sec	Propellan
1	System	600	150	150	.05	
2	System	600	150	150	.10	Neat NTO
3	System	600	150	75	.05	per
4	System	600	150	75	.10	MSC-PPD-2A
5	System	600	150	12	.05	
6	System	600	150	12	.10	
7	System	600	75	150	.05	
8	System	600	75	150	.10	Neat NTO
9	System	600	75 ·	75	.05	per
10	System	600	75	75	.10	MSC-PPD-2A
11	System	600	75	12	.05	
12	System	600	75	12	.10	<u> </u>
13	System	600	12	150	. 05	
14	System	600	12	150	.10	Neat NTO
15	System	600	12	75 75	.05	per
16	System	600	12	75	.10	MSC-PPD-2A
17	System	600	12	12	.05	
18	System	600	12	12	. 10	
			Worst Case	(1) 		
19	System	600	150	12	.10	
20	System	600	150	12	.15	
21	System	.050(2)	150	12	.10	Neat NTO
<b>2</b> 2	Worst Valve	600	150	12	.10	per
23	Worst Valve	600	150	12	.15	MSC-PPD-2A
24	Worst Valve	.050 (2)	150	12 12	.10	
25	Worst Filter	600 600	1 <b>5</b> 0 150	12	.15	
26 27	Worst Filter Worst Filter	.050(2)	150	12	.10	
20	Curtor	600	150	75	05	
28 29	System System	600 600	150 150	75 75	.05	Doped NTO
30	System	600	150	75 75	.15	boped wis
			Worst Case	(1)		
31	System	600	150	12	.05	
32	System	600	150	12	.10	
33	System	600	150	12	.15	1
34	System	.050(2)	150	12	.10	İ
35	Worst Valve	600	150	12	.10	Doped NTO
36	Worst Valve	600	150	12	. 15	
37	Worst Valve	.050 (2)	150	12	.10	
38	Worst Filter	600	150	12	.10	ł
39	Worst Filter	600 .050 (2)	150	12 12	.15	
40	Worst Filter	.030 (2)	150	1 14	.10	

<sup>(1)</sup> These test conditions appeared to be worst case in the NAS 7-549 filter flow assembly study. The actual worst case conditions for this system will be determined from the test results of Runs 1 - 18.

<sup>(2)</sup> Pulsing runs will be made on a duty cycle of .060 sec on and .060 to .100 sec off for a total test duration of 60 seconds. Runs consisting of .060 sec pulses with longer hold times in between will be considered.

and close the test system/catch tank valve. Attach drain tank to catch tank and offload used NTO. Discard the NTO, and send the sample bomb(s) to the Analytical Chemistry Section for analysis.

# 6.5.2 Short Duration Pulse Runs

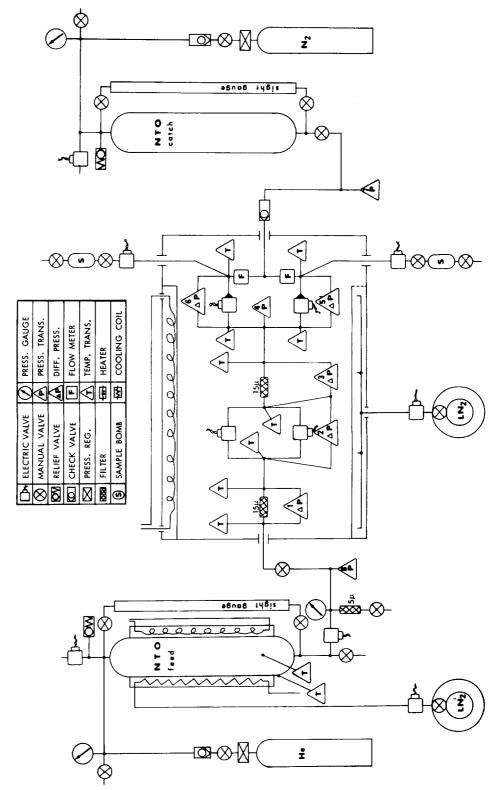
The procedure for the short duration pulse runs is identical with Section 5.5.1 with the following exception. Adjust the pulse period sequences and pulse counter to the required on/off pulse times and firing duration. Activate the sequencing switch on the firing panel. After opening the dual redundant valves, press the sequencing fire switch and allow the run to proceed. After the run is completed, activate the continuous duty engine valve switches and take NTO sample(s) as described previously.

## 6.6 Sample Bomb Preparation

Place the sample bombs in their respective holding clamps with the electrically actuated snap sample valve closed, open both hand valves and evacuate. Back fill with gaseous nitrogen and close the end valve, leaving the hand valve closest to the snap sample valve open. When the NTO sample is taken, the system pressure will ensure filling the bomb with the requisite amount of oxidizer.

#### 7.0 INSTRUMENTATION

Instrumentation locations are shown on the Test Schematic, Figure 1. The data being taken includes temperatures, flows, pressures and pressure differences across all critical test system components. The transducers and recording devices used are listed in Table 2 while an estimate of overall recorded data accuracy is shown in Table 3.



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Table 2. Instrumentation List

ITEM	TRANSDUCERS
1	Data Sensors - 25 psid S/N 101851
2	Data Sensors - 25 psid S/N 95
3	Data Sensors - 25 psid S/N 1140
4	Taber - 300 psig S/N 681139
5	Data Sensors - 150 psid S/N 459
6	Data Sensors - 150 psid S/N 479
7	CEC - 200 psig S/N 17025
8	Taber - 300 psig S/N 651748
9	Right Flowmeter - Foxboro S/N 18964
10	Left Flowmeter - Foxboro S/N 18969
	READOUT DEVICES
11	Visicorder - Honeywell 1508
12	Amplifier - Honeywell 104-7
13	Signal Conditioning Unit - Endenco 4470
14	Pulse Rate Converter - Waugh FR-45
15	Strip Chart Recorder - L/N W
16	Thermocouple Reference Junction - Pace 150
17	EPUT and Timer - Beckman 6146
18	Preset Unit - Beckman 622
19	Function Generator - Exact 503
20	Power Supply - Harrison 802B
21	Valve Driver - TRW
22	Multimeter - Fairchild 7050
23	Temperature Controller - Honeywell S152R15

Table 3. Estimated System Measurement Accuracy

## Temperature

TC 
$$\pm 1.5^{\circ}F$$

Recorder  $\pm 0.6^{\circ}F$ 

Ref. Junction  $\pm 0.2^{\circ}F$ 
 $\pm 2.3^{\circ}F$ 

## Pressure

# Flow

### APPENDIX III

This Appendix contains a tabular presentation of corrected flow data, in both weight and volumetric units, equivalent flow area, percent of maximum corrected flow and percent difference from maximum corrected flow. This data was used to prepare the plots of percent corrected flow and percent flow decay, presented in Section 4 of this report. It should be understood that all percentages given are based on the maximum flow experienced by that component during this test program. These maxima are identified in the tabulation and are summarized in Table 4-1.

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N N	◄ ليا	_ W		4 • 4	1:0	1:0	91.40	1.7	2.1	2.5	2.2	1.7		4.6	9,5	9.8	89.87	9.2	9.8	6,6	9.3		0.5	1.0	1.3	80	80	89.41	
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	7 3	Sad		05069	05030	5025	.050186	5157	05079	05051	5036	05049		05435	05462	05467		05342	05292	05278	02304		04781	04817	04864	04882	04877	•049267	
	CORRECTED	ω Σ		52	250	50	•2498	256	252	251	50	251		0	271	272	.2697	265	253	262	264		238	239	242	243	242	• 2452	
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PAGE 7	CORRECTED	Ædg	ก 55	2556	• 2559	2559	2565	2565	2564		2588	2571	2559		2539	2554	2555		2557	557	2558	2556	2547	2541	25
ш <i>Z</i>		MAXIMUM PERCENT	9.5	7.6	89.90	6.6	0.1	0	0.0		0.9	0.3	00	89.92	9.2	7.6	7.6		9.8	9.8	<b>6</b>	9.7	9.5	89.29	9.2
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#### APPENDIX IV

### EQUIVALENT AREA AND FLOW VS. TIME PLOTS - NTO FLOW DECAY STUDY

This Appendix contains a graphical presentation of the equivalent area and system flow data vs. time collected during the flow test phase of Contract NAS 8-21489. A more complete presentation of this data including component inlet and outlet temperatures and pressure drops, in addition to the data presented in this Appendix, is presented in Appendix V. The flow variations in the flow data plotted in this Appendix may be partially due to variations in overall system pressure drop, however, this effect is relatively small. The effects of system pressure differential variation have been eliminated in calculating the equivalent area. The data plotted here should be used only to examine trends. If an actual value is desired for any data point, the tabular data in Appendix V must be used.

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ы Z	ERCE OF			2.2	0.2	91.10	0.8	7.6	9.5	9.6	7.6	9.7	7.6		9.0	90.60	0.5	0.3	0.3	•	0.1		6.0	9.0	8.7	9,3	9.4	9.0	89.42	9.5
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	FLOW	G G		05092	5075	•050452	05041	05037	5010	05039	05113	5138	05154		5219	.052077	5184	05190	5170	5177	5159		5028	05031	5069	05042	05069	5009	.050510	5032
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PAGE 10	CORRECTED	Md	00	いいしん	2675	2757	2760	2708	2717	2713	2714	272		2744	6470	753	2813	2676	2568	2539	.2538		2547	2557	2558	2595	2689	2771	2714	. 2658
Ш Z H		MAXIMUM PERCENT	OI OI	0 0	93,99	8	6.9	5.1	5.4	5,3	5,3	5.00		6.3	6.3	6.7	00	4	0.0	9.1			4.6	9.8	9.8	1.1	4.4	7.3	5.3	93•36
υ 2 ω	₩ 8	MAXIMUM PERCENT	•	• (	6.01	-	0	90	i	9	9	-		9	4			9	00	0.8	00		0.5	0	7	00	្ស	9	•	49.9
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	FLOW	Sed	05073	4006	•051032	5082	5098	05079	05072	05117	5100	5146		05229	05189	•051145	05216	05180	05182	05107	05191		5207	05178	5087	05192	05246	05255	.052423	5224
	CORRECTED	Æ d S	() LE	1 00	• 25 C	252	53	52	52	20.0	വ	256		260	258	• 2546	259	257	257	54	258		59	57	253	ις 00	261	261	• 2609	260
ພ ຂ ພ	ပေစ	MAXIMUM PERCENT	ος •	103	93 • 34	2.9	3.2	9.9	2.7	3.6	3,2	4 • 1		5.6	6.4	93.55	5.4	4.7	4.7	3.4	6.4		5.2	4.7	3.0	4.9	5.0	6.1	95 • 89	ល ស
Z W		E G	٨.	9	9919	0		<b>~</b>	Ş	+	Ç	œ		<b>ب</b>	0	6 • 45	ភ	ů	ů	ហ៊	Q		.7	ů	Ď	ô	ô	$\infty$	4 - 11	4
υ ⊶ α	ACTUAL AREA	00	216	.197	1.2231	.218	• 255	.217	•215	• 226	-222	• 233	31	253	•243	1.2258	•250	.241	• 245	•224	• 224	32	1.24	.241	•219	• 544	•257	• 259	-256	•252
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PAGE 11	CORRECTED	₩ d g	267	• 2651	271	(	253	253	252	252	253	• 2535	253	252	ה ה	ה ה	253	252	252	252	• 2552	252
ш Z	ERCE 0F		9.0	93.12	5.3		9.1	9.0	00	80	9,0	89.06	9.1	8•7	c o		8,9	8.7	8.6	8.7	88•60	8.7
о <i>2</i> ш	OIFF FR9M	C II	0	6. N 8. N 8. N 8. N	• 6		° 0	1:0	1.1	1:1	0.0	10.94	0.8	1.2	•	<b>5</b>	0.1	1,2	1.3	1.2	11.40	1.2
⊩ W 1	ACTUAL AREA	100	.287	1.2764	•306		• 221	•219	.217	-218	.220	S	.221	.216	<del>,</del>		.219	.217	.214	.216	1.2144	.217
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PAGE 1	CORRECTED	Ø B		252	252	252	252	252	252	.2521		251	250	250	251	251	251	.2520		40	252	267	277	284	275	• 2723	274
W Z		MAXIMUM		8.7	8.6	8.6	8.6	8.6	8.6			4 • 4	8 1	8	8 . 4	8.2	88.43	8.5		9.5	88	3.8	7.3	0.0	96.8	95.67	<b>5.</b> 4
о 2 ш	μ α	MAXIMUM		1.2	1.3	1.3	1.3	1.4	1.3	11.43		1.5	1.0	1.00	1.5	1.7	11.57	1.4		4.	1	6.1	9	0	1	4.33	io.
<b>.</b>	F A	x1000 ×1000		.216	•214	.214	.214	.214	.215	N		.212	.207	• 20g	.212	•21°	1.2121	.213		.227	.217	.286	.333	•370	.327	1.3113	• 322
	F 0 3	S		05125	5095	05092	05096	5055	05068	50		05112	05072	05047	05063	05102	•051174	05110		05203	5210	05211	05208	05198	05208	•052118	05226
	CORRECTED	0 0 7		55	253	253	<b>•2537</b>	251	252	252		ĮŲ	52	5	50	10	.2547	254		59	59	3	59	50	259	•259♦	260
W Z ⊎		MAXIMUM		3.7	3.2	3.1	93 • 23	₽. \$	2.7	2.7		3.5	2.7	2.3	5.6	3,3	93•60	3.4		5 1	5.3	5,3	5.5	50	S. 5	95•33	5.6
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I ∪ ~	D H	SQ.IN. X1000	35	1.2285	.221	•250	.221	.211	•214	.215	36	S.	•215	•209	•213	• 223	• 256	•254	37	1.54	•248	• n 4 0	• 248	•246	• 248	.249	• 252 2
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_	FLOW	<b>ଟ</b> ଅ	05626	05561	.054416	05555	05623	05623	05639	:	05117	05105	05114	.051164	05128	05159	05118		05095	05077	05066	05080	05076	.050574	05055
PAGE 13	CORRECTED	E G	280	276	•2708	276	279	279	280		254	254	254	.2547	255	255	254		253	252	252	252	252	.2517	251
N E	ERCEN OF		8.3	7.2	95.15	7.1	8.3	<b>8</b>	8 • 6		9.4	9.2	9.4	89.46	9.6	9.6	9,5		9.0	8.7	8.6	8.8	8.7	88.43	<b>%</b>
ប 2 ម	DIFF	→ C E W	9		4.85	00	9	•	<b>ب</b>		0.0	0.7	0.5	10.54	0.3	0.3	*		0.9	1.2	1.4	1:1	1.2	11.57	1.6
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	¥ 0 ] L	S d d	05243	05203	•051911	05204	05187	05182	05195		05087	05138	05132	5122	05110	5106	0511		05126	05123	05112	05097	05132	•051240	05125
	CORRECTED	Σ. Δ. Ό	261	259		259	258	257	258		253	255	255	40	254	254	25		255	255	254	253	255	S	252
ω Ζ ⊶	ERCE OPE		5. 9.	5,1	9	5.1	**	4.7	95 • 02		3.0	3.9	3.8	3.6	3.4	3.4	93,51		3.7	3.7	3.5	3,2	3.8	3.7	•
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I © ⊶ α	CTUAL	•00	256	.247	* 5 C •	.247	.243	• 242	e.	99	1.219	.231	.230	.227	.224	•224	1.5254	0	1.228	.228	• 225	•221	.230	-22	228
	T I ME	SEC.	2 ⊃ Z		) (V	00	4	0	360	Z 2	, m		C	00	4	0	360	Z ⊃ α	m		N	00	4	0	360

Ι υ α	Z Ш	ы 2  5				<u>г</u> ш	ี่ 2 ⊶	PAGE 1	
CTU ARE	7.00		CORRECTED	FLOW	CTU	₩ Q	() (1)	CORRECTED	FLOW
\$0.1N.	MAXIMUM	MAXIMUM	A G	<b>g</b> S	X1000 X1000	MAXIMUM PERCENT	MAXIMUM	₩ d <sup>©</sup>	S d d
267	•	6.7	63	5289	•	0.7	ס	ເດ	05104
.278	2 • 41	7.5	200	05335	•	0.1	D)	ഥ	05136
.275	•	7.3	264	05322	•	4	g	ശ	05119
•271	•	7.0	264	05305	•	0.7	Q	ம	05104
.254	•	5.7	260	05232	•	4.0	σ	ഥ	05118
• 250	•	5.4	259	05218	•	0.7	Ð	ഗ	05106
ر 2	4 • 66	95 • 34	•2594		1.2225	10.81	89.19	• 2539	•051004
23		*	256	051	•	σ	90.42	257	O
1229	•	3.8	5	5128	•	m	9.6	55	05129
•230	•	3.9	255	05134	•	0	9,9	256	05145
• 223	•	3,3	254	05102	•	4.	9.6	255	05124
• 225	•	3.4	254	05110	•	9.5	4.0	257	05170
•236	2.67	94•33	.2567		1.2381		0.3	,2571	5165
232	•	<b>#</b> • 3	256	5155	•	<b>.</b>	0.2	256	05161
224		3.4	54	5110	•	-	9.00	255	05138

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CORRECTED	E d U	9	• 38 87 • 38 88 7 • 58 85	377	371	382	ν <b>γ</b>	373	371	75		C	ית ומכו	9	11	37	7.4	67	• 3585	57			20	75	71	.3413	35
	MAXIMUM PERCENT	4 • 1	73.10	• • • • • • • • • • • • • • • • • • •	0.1	เก	0 • V	9•0	200	8			φ. Ω.	0	113	2.6	0.7	9,3	67.70	7 . 4			6.1	0	0.1	94 • 49	3.2
₩ Œ	MAXIMUM PERCENT	VAL 25	6.9	8	φ. 8	7.8	ω ė O π	0 Q	8	9.1		VES.	9 0 4	<b>80</b>	8.6	7.3	9,3	9.0	32,30	លុំភ		VALVES	3,8	9.1	9.8	ហំ	6.1
<b>→</b> 0	× 1000 × × 0000 ×	*		4.09	3.85	4.24	4.01	96.6	3.86	3,99		20 i	4.52	4.02	4.09	6.32	3.96	3.69	13.372	3,32		6 B0TH	3.06	3.99	3.86	B	2.50
T I ME	SEC.	Z	75	180	4	0	9 (	Uα	3	O	:	Z					g	1	460	0		z ⊃ α	œ		Ū	9	009
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	MAXIMUM PERCENT	4 • 4	80 19	0 4	*	4.6	4.2	3. 0.0	1.7	5 5 6	5.7	<b>† • †</b>	8.0	0.3	4 • 1			0.7	מי	78.32	3.8	0	4 . 1	6.9	4 . 0	ı	
•→ C	MAXIMUM PERCENT	VALVES 35•57	9 0	ω ας ας	8 6	5.4	5.7	9	0 0 0 0	10	4	8.5	9.1	9.6	50	)	7	29.2	7.7	21,68	6.1	7.9	5.8	3.0	5	<b>)</b>	
010	SQ. IN. X1000	N	t	0.18 0.08 0.08	6.08	4.73	4.67	4 • 55 6 • 55 7 • 6	40.0	6.97	46.9	4.11	3.99	3.88	4.64	)	•	13,975	4.27	15.470	4.58	4.23	49.4	5.20	06.4	•	
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16	FLOW	g 8		0639	05362	105392	0506	0238	0210	0211	<b>)</b> 		09458	•094166	09398	)		10012	0087	10189	10315	10287	•102169		9706	•097919	14400	1670	1 /0 / 0		
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1 8 S I	⊢ α ⊐ ⊞	SG 1N X 1000	0	19.752	9.56	19.567	9.50	9.00	8 • 95	8 • 95		861	17.560	7.48	7.44		B61	8.58	8.72	18.918	9.15	9.09	8.96	B8T	18.021	18.179	80.08	7.95	)		
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	FLOW	Sdd		0000	•07474	7901	8351	8503	8645	8567	8465	8416	8476	8467	8265	3183	•081939	8147	3107	3129	3174	3211	3236		0272	0236	0208	0220	0244	•102383	
ر. >	CORRECTED	Q A		8	.372	393	ប្រ	S	8	92	d	8	ä	2	11	5	* 4078	5	80	404	406	80	<b>4</b> 09		511	509	508	80	509	•5396	
- <b>∀</b> > z		MAXIMUM PERCENT		9	0.0	4 • 2	00 R1	6.0	1.2	0.5	9.5	9.1	9.6	9.5	7•6	6.9	77.02	6.5	6.2	5 • 4	9.9	7 • 1	4 • 4		6.5	96 • 25	0 9	9	6.2	6 • 2	
Ð I ► ∀	H 82	MAXIMUM PERCENT	Š	0.00	9.7	5.7	1,5	0.0	8.7	4.0	*	6.0	6.0	4.0	<b>ب</b> ع	3.0	22.98	3.4	3.7	3,5	3.1	00	ດີ	VALVE	*	3,78	0	6	.,	.7	
	CTU		86	0.00	3.87	<b>*•66</b>	5.50	5.78	6 • 05	90 10	5.71	29•5	5.73	5.72	5.34	5.19	15.212	5.12	5.05	9.09	5.17	9.04	5.29	1	9.07		8 95	8.97	9.01	9.00	
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17	FLOW	<b>8</b>		0393	0283	0224	103010	0370	0245	0184	0179	0192		9991	9883	9914	099144	9853	6066	9871	9915			0021	100575	7600	0093	0101	0136	
PAGE	RECTED	2		73 •	18	• 68	127	. 29	• 86	• 69	67 .	73		73 .	19	35	935	• 40	32	13 •	35			. 88		. 92	24·	27 .	45	
ר > ח	COR	g G					ស្ត										*								• 57					
→ → >	PERCENT OF	MAXIMUM PERCENT		1:1	0.1	9.6	90 • 33	6.0	9.00	9,3	9.2	9•3		1.9	9.0	1.2	91.27	0.7	1.0	00	1.2			7 . 8	88 • 20	8	8.5	8 5	& •	
A T I 9	0 1 1 1 1 1 1 1 1	E E	4	8.86	œ	<b>ن</b>	9.6	9.0	0.1	9.0	7.0	•	<b>&gt;</b>	0	0		8.73	'n		∵			7	2.1	11.80	1.4	1.4	1.4	-	
ISBL	CTU	X1000 X1000	8	9.648	* 30	• 49	9.562	• 62	• 50	• 45	• 45	• 46	لما	9.275	.17	• 20	9.203	• 1 4	• 19	• 16	.20		-	• 30	9.336	.37	• 36	•37	9	
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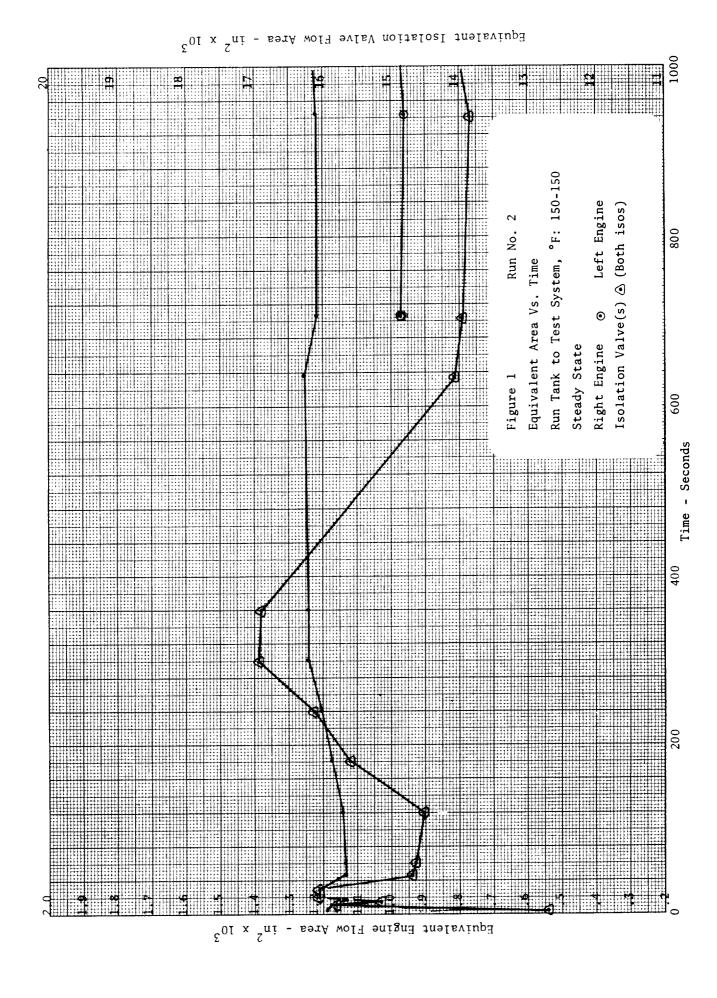
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### APPENDIX IV

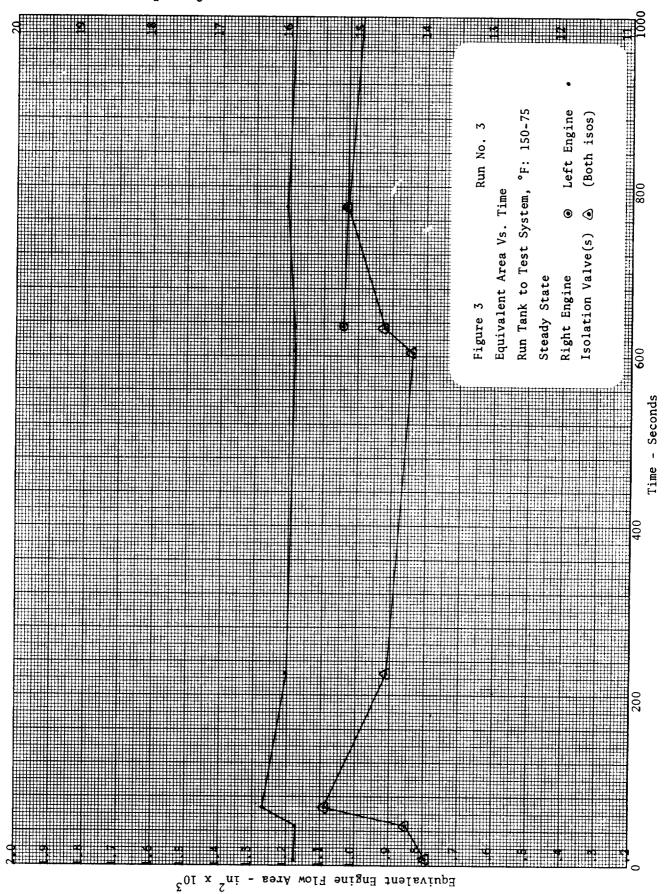
## EQUIVALENT AREA AND FLOW VS. TIME PLOTS - NTO FLOW DECAY STUDY

This Appendix contains a graphical presentation of the equivalent area and system flow data vs. time collected during the flow test phase of Contract NAS 8-21489. A more complete presentation of this data including component inlet and outlet temperatures and pressure drops, in addition to the data presented in this Appendix, is presented in Appendix V. The flow variations in the flow data plotted in this Appendix may be partially due to variations in overall system pressure drop, however, this effect is relatively small. The effects of system pressure differential variation have been eliminated in calculating the equivalent area. The data plotted here should be used only to examine trends. If an actual value is desired for any data point, the tabular data in Appendix V must be used.

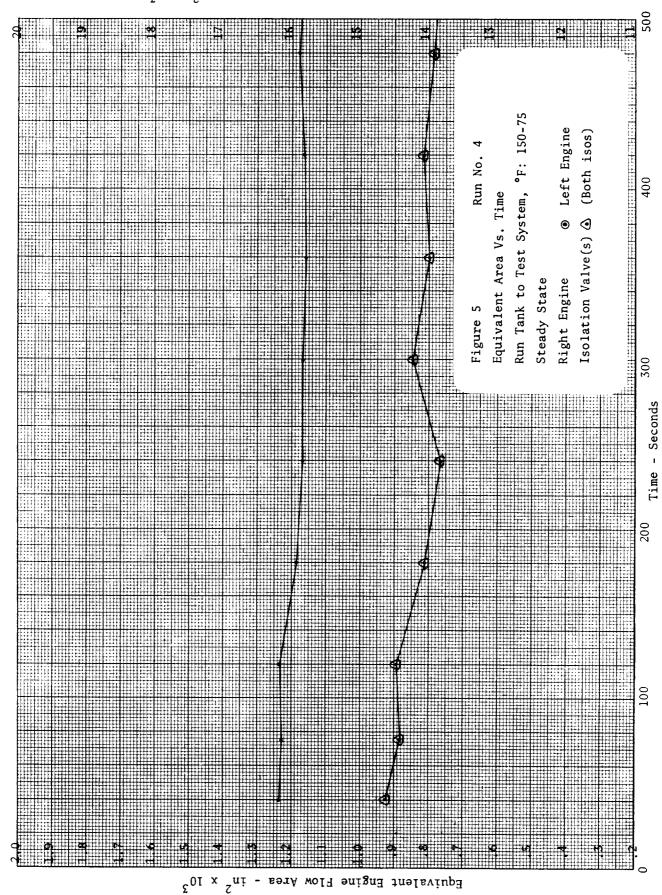
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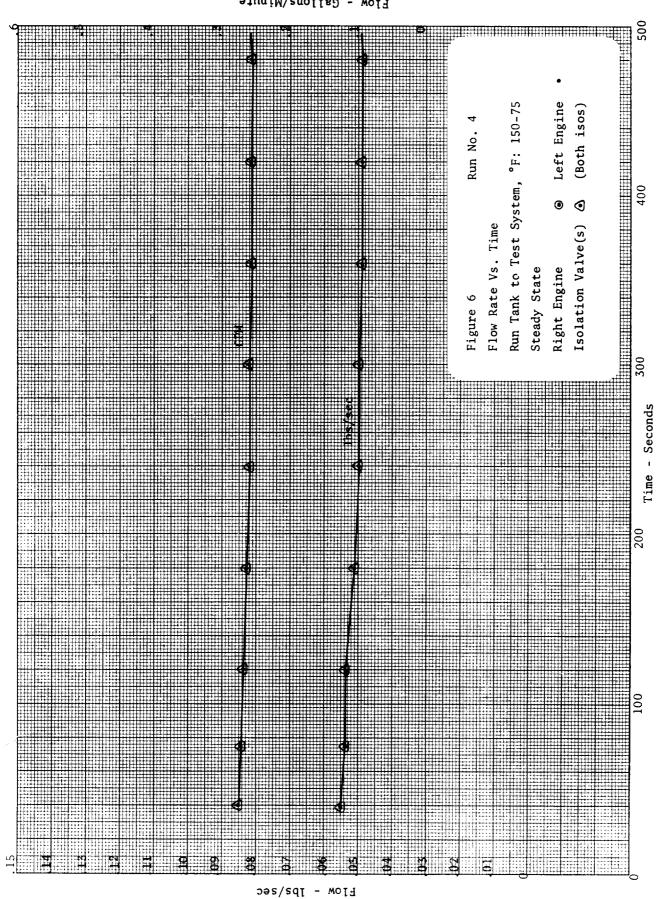


Flow - lbs/sec

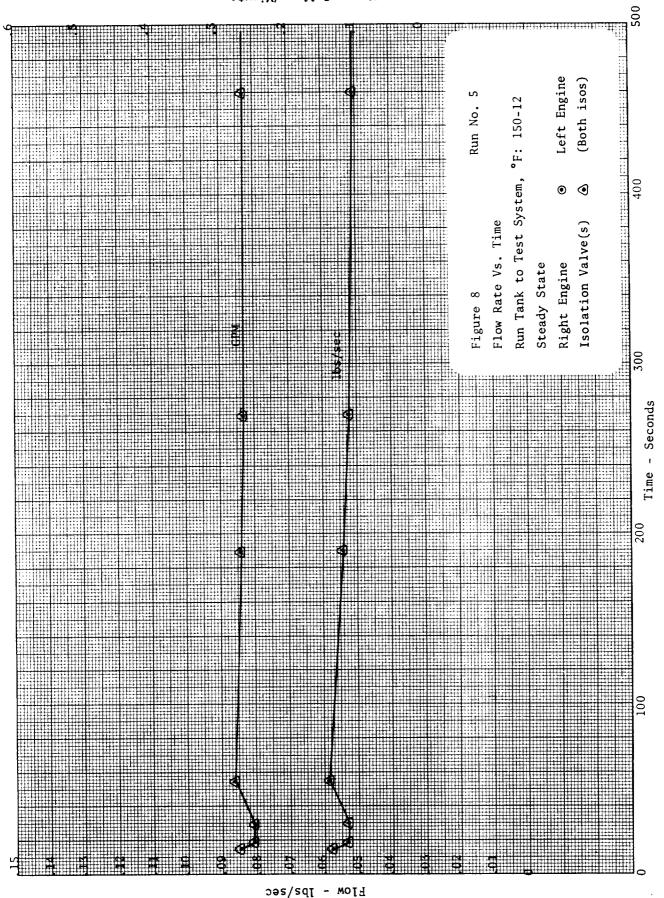


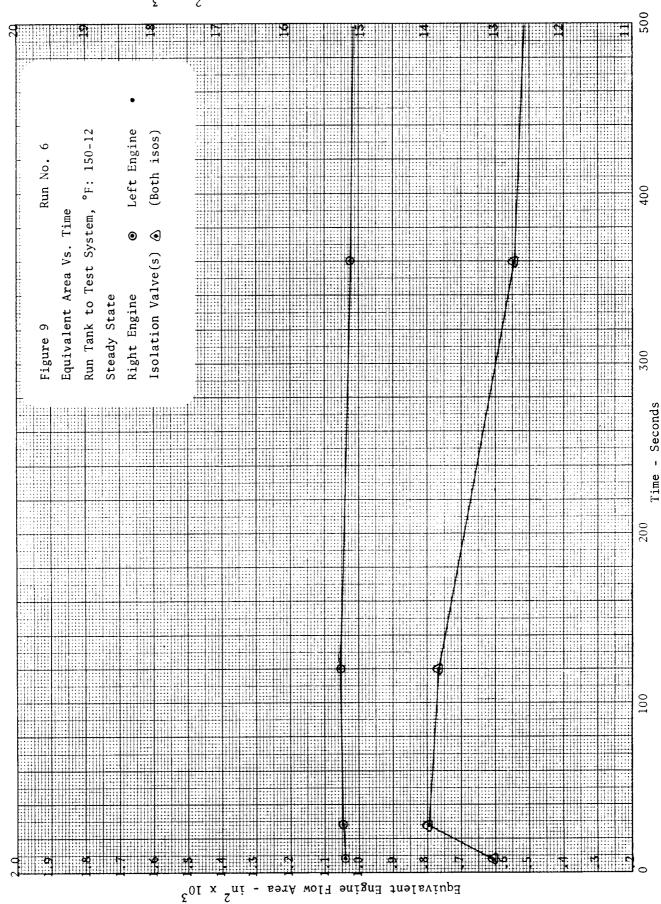
Flow - lbs/sec



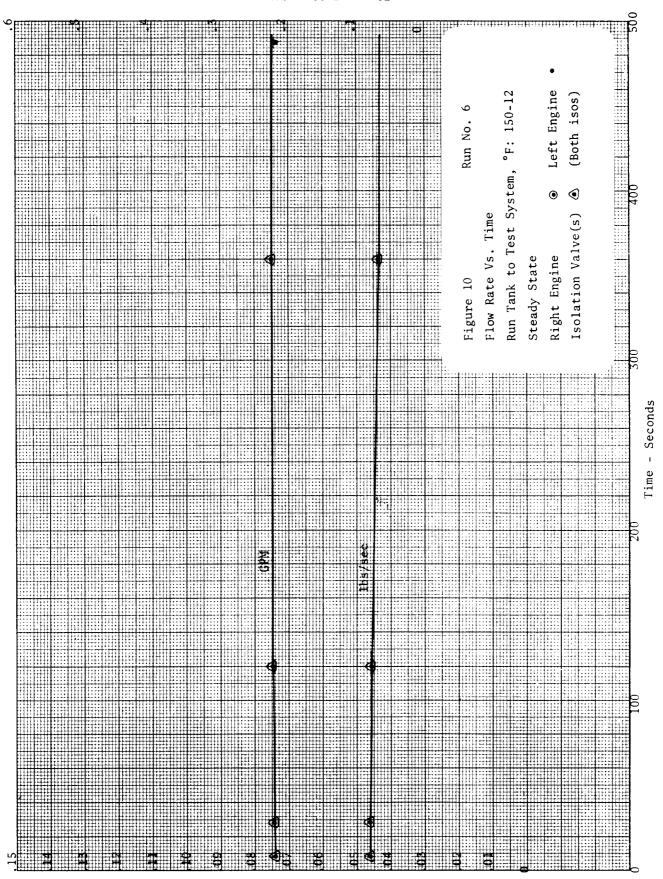


Equivalent Isolation Valve Flow Area -  $in^2 \times 10^3$ 



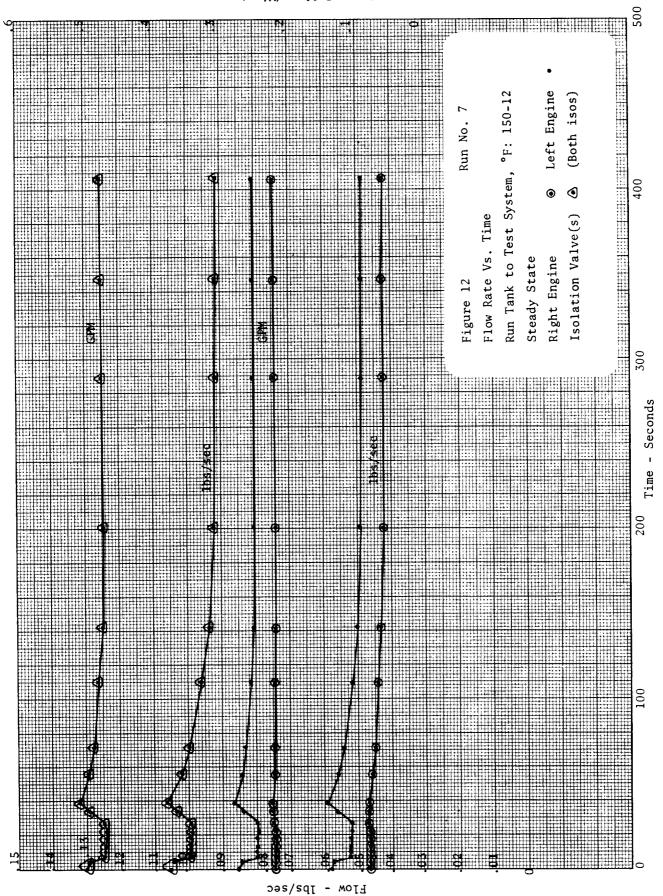


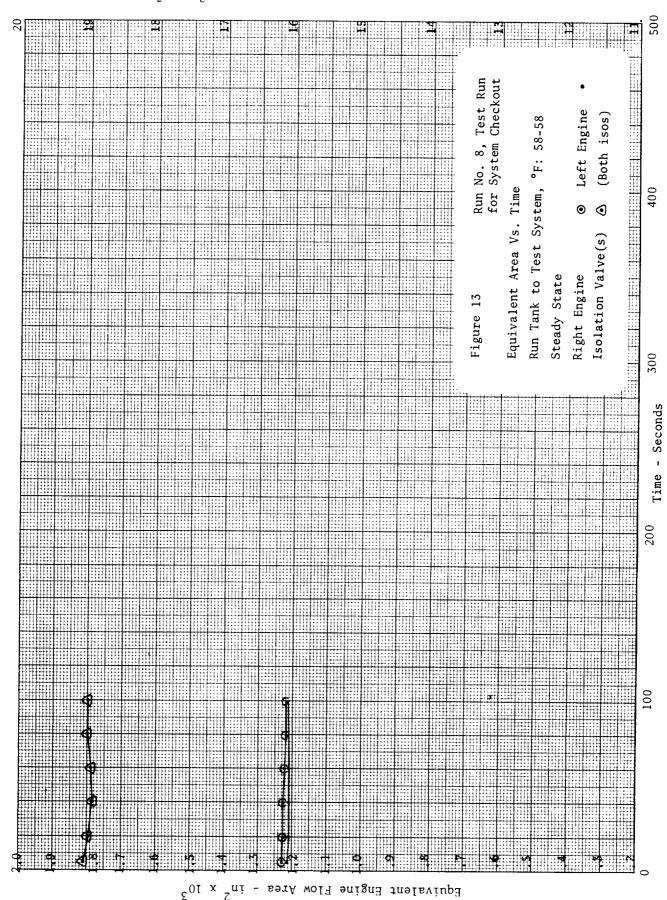
Equivalent Isolation Valve Flow Area - in  $^2$  x  $^2$ 

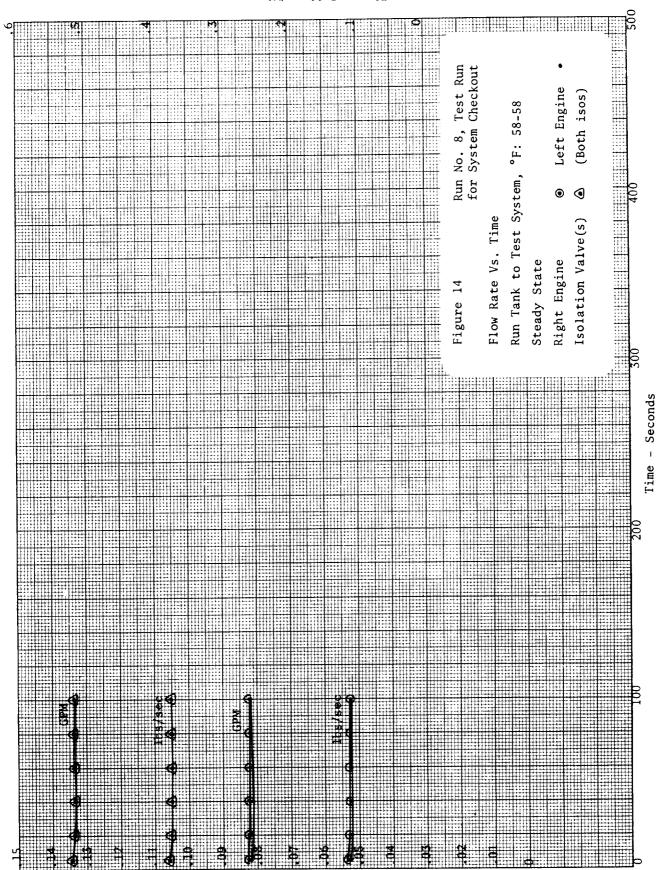


Flow - lbs/sec

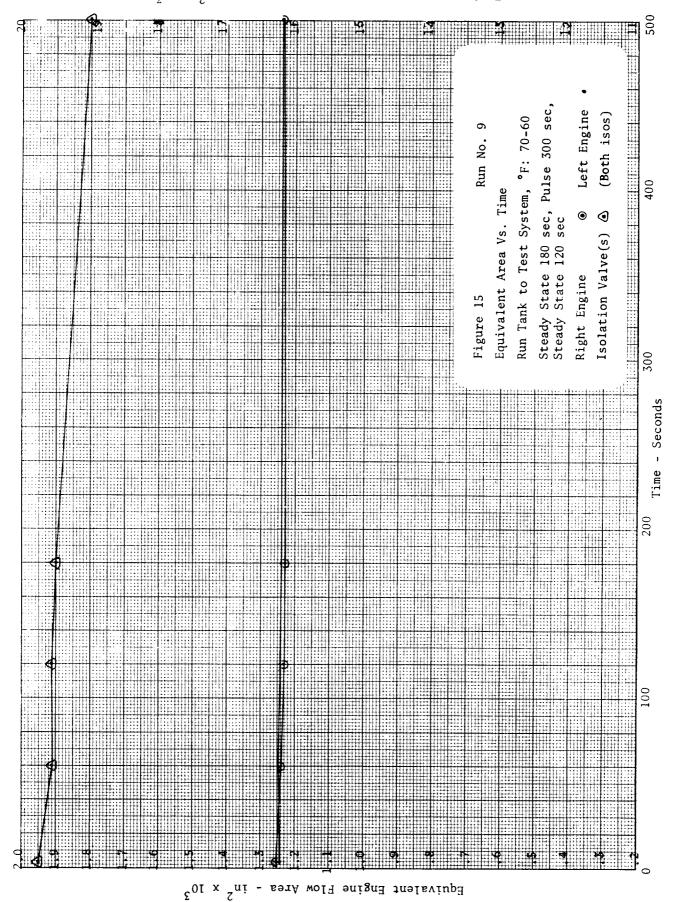
Equivalent Isolation Valve Flow Area -  $in^2 \times 10^3$ 

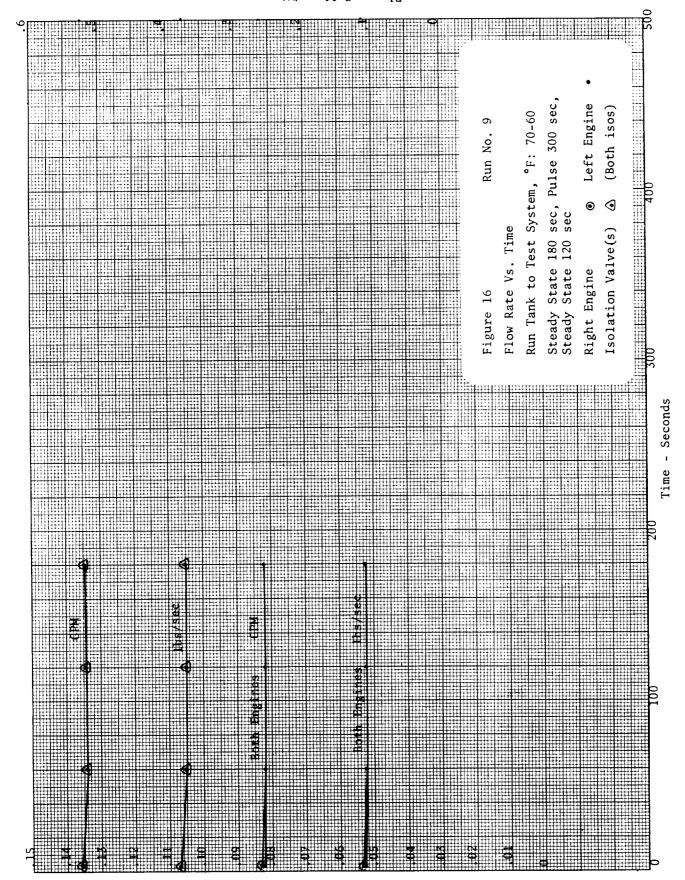






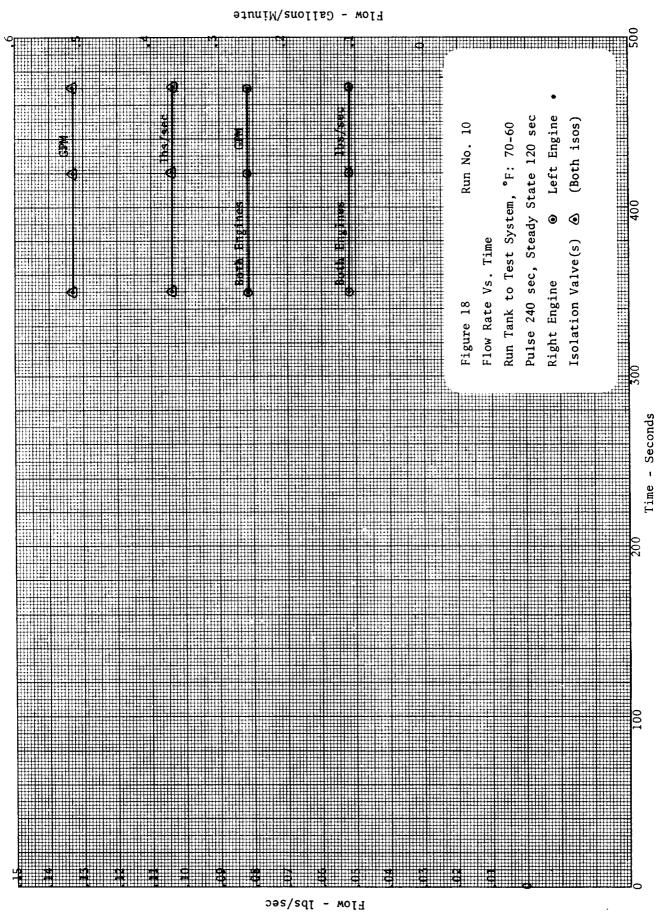
LJOM - Jp2/sec





Ljom - jps/sec

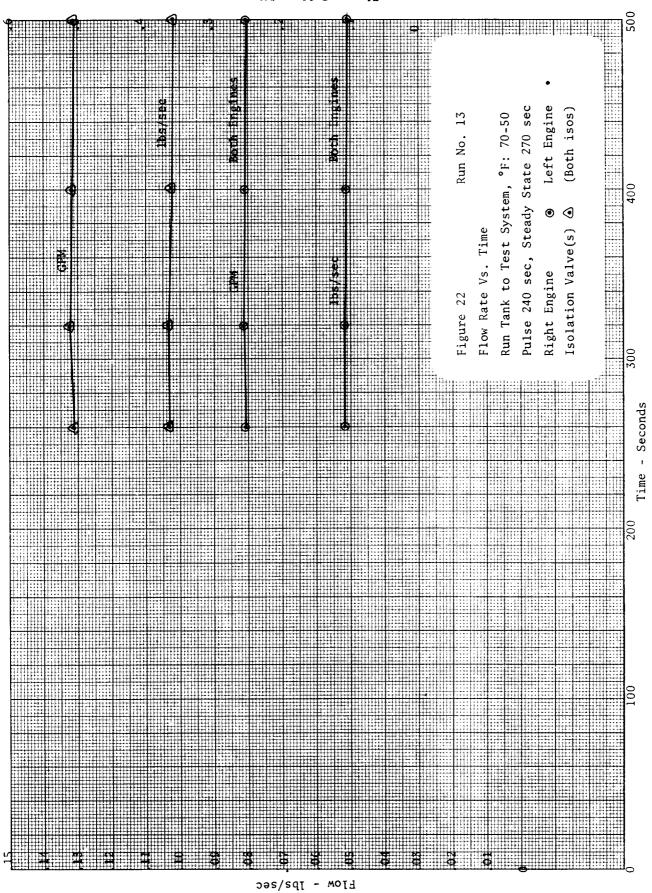
Equivalent Isolation Valve Flow Area - in  $^2$  x  $^10^5$ 

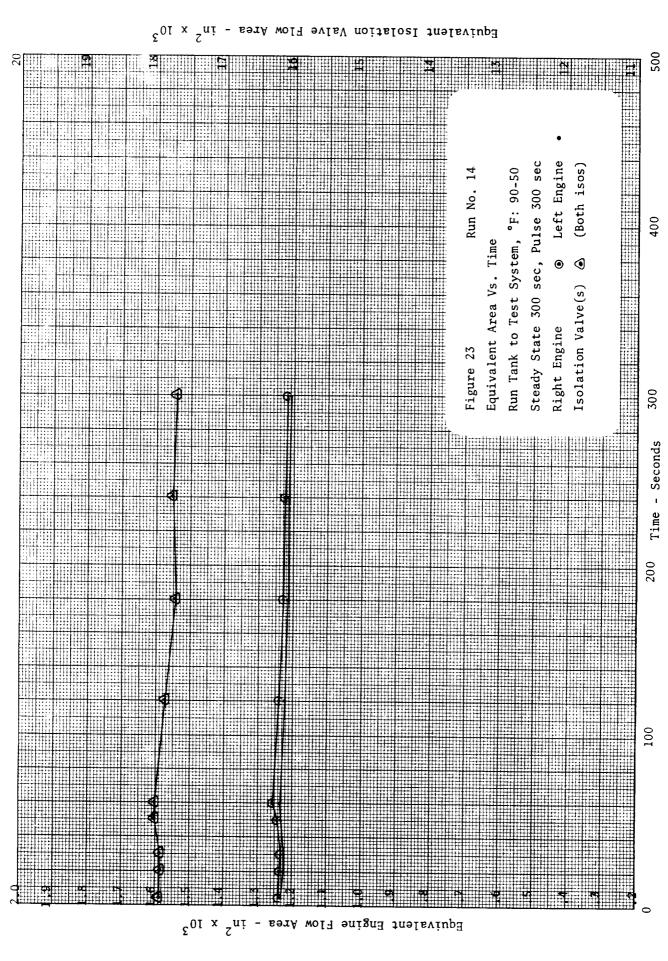


Equivalent Isolation Valve Flow Area - in  $^2$  x  $^10^3$ 

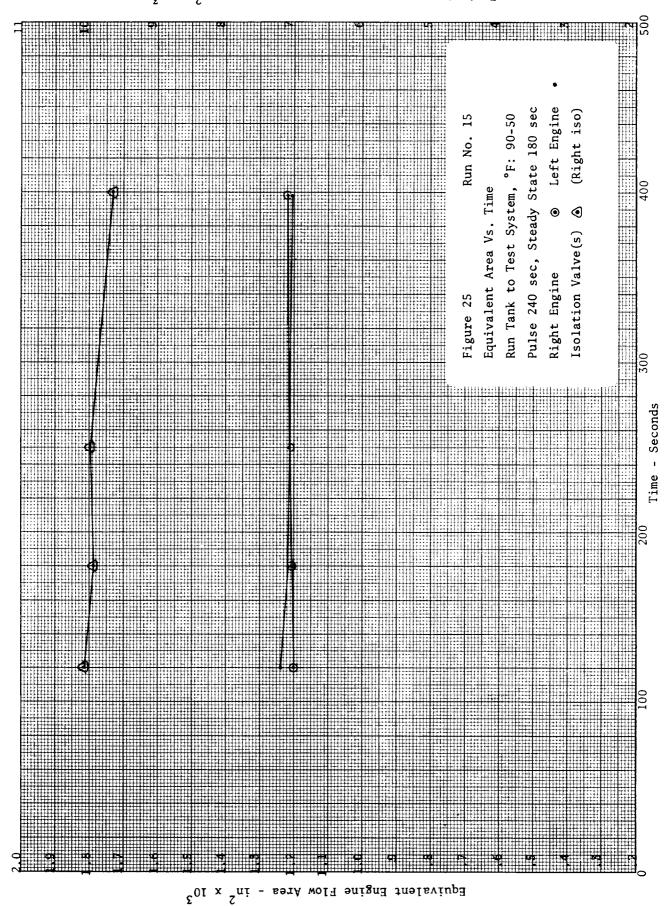
Ljom - jps/sec

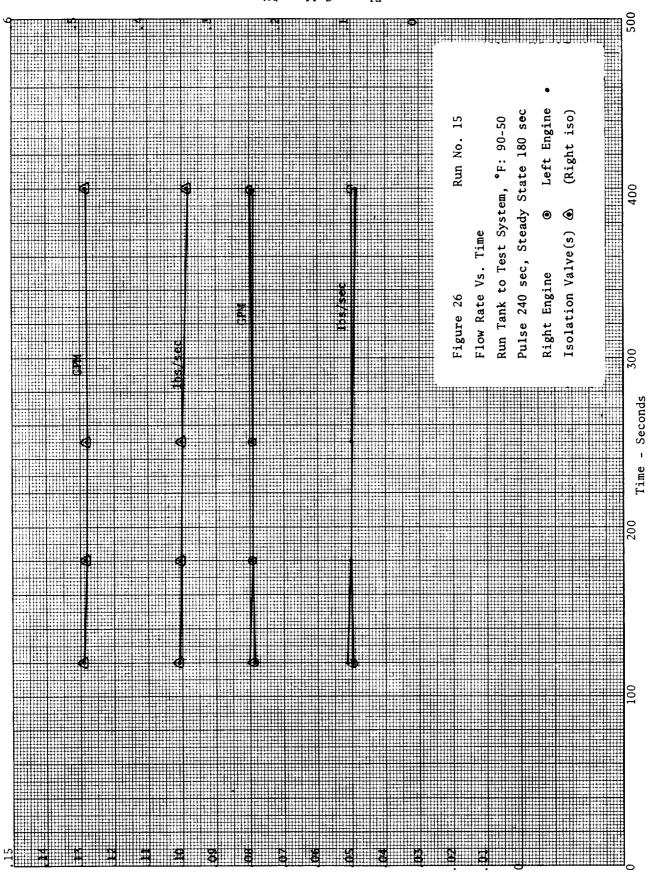
Equivalent Isolation Valve Flow Area - in  $^2$ 



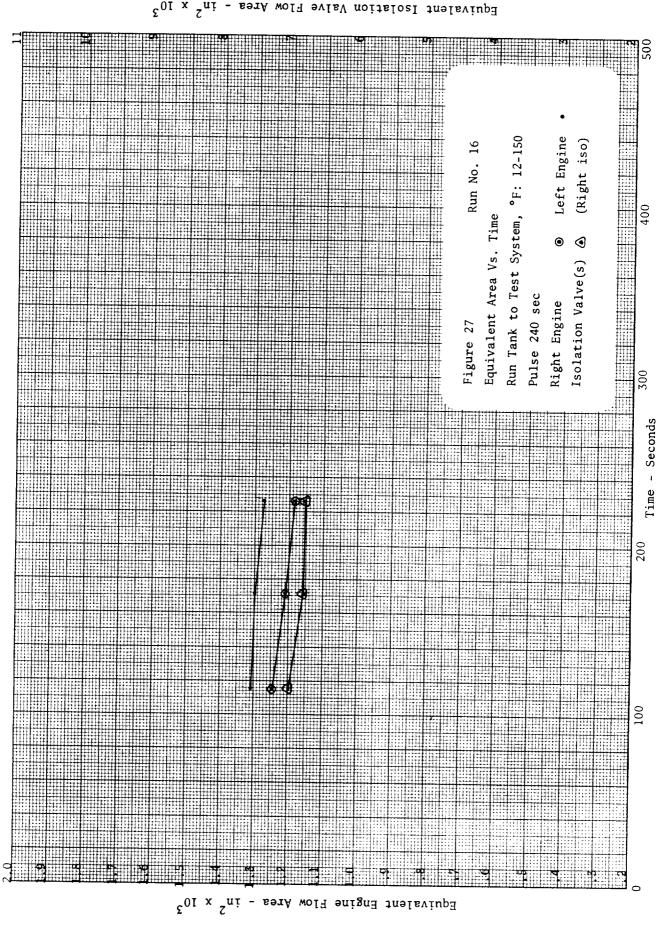


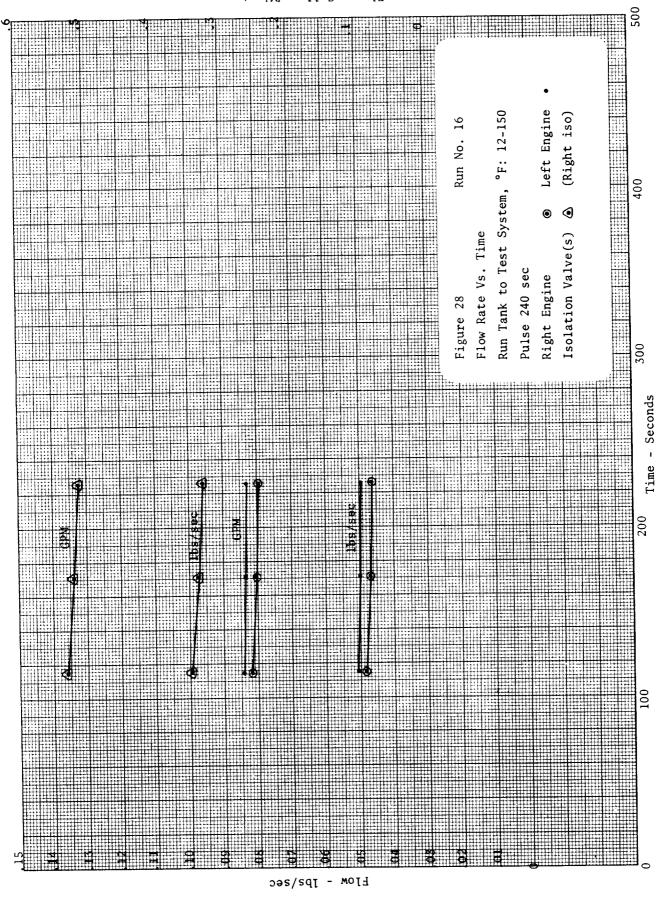
Ljom - jps/sec



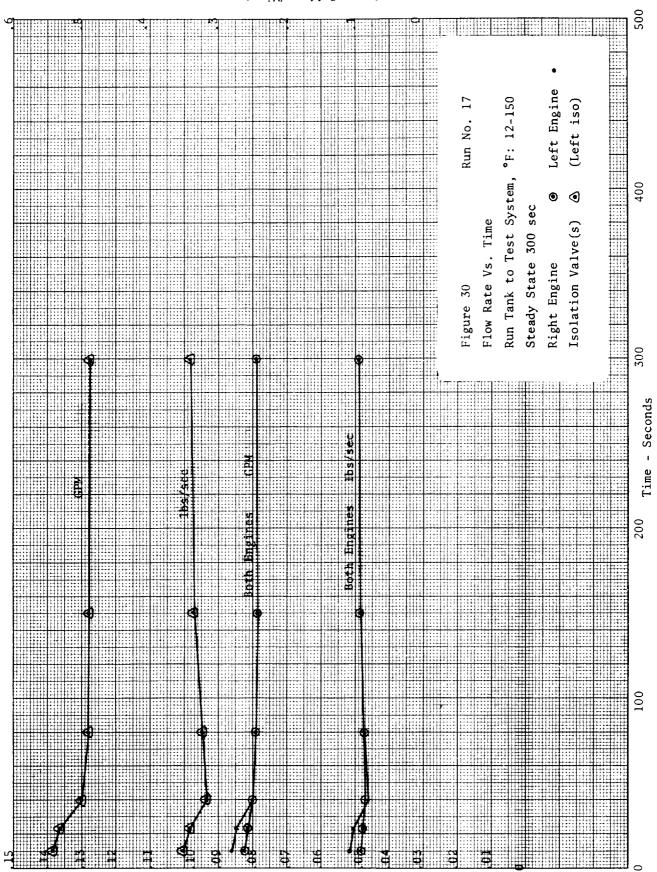


LJOM - Jps/sec

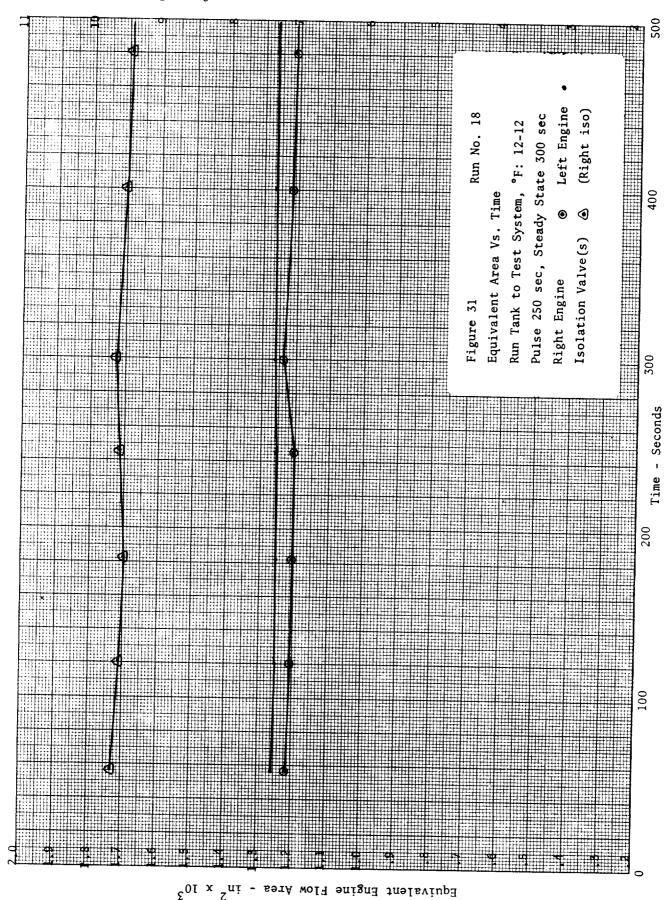


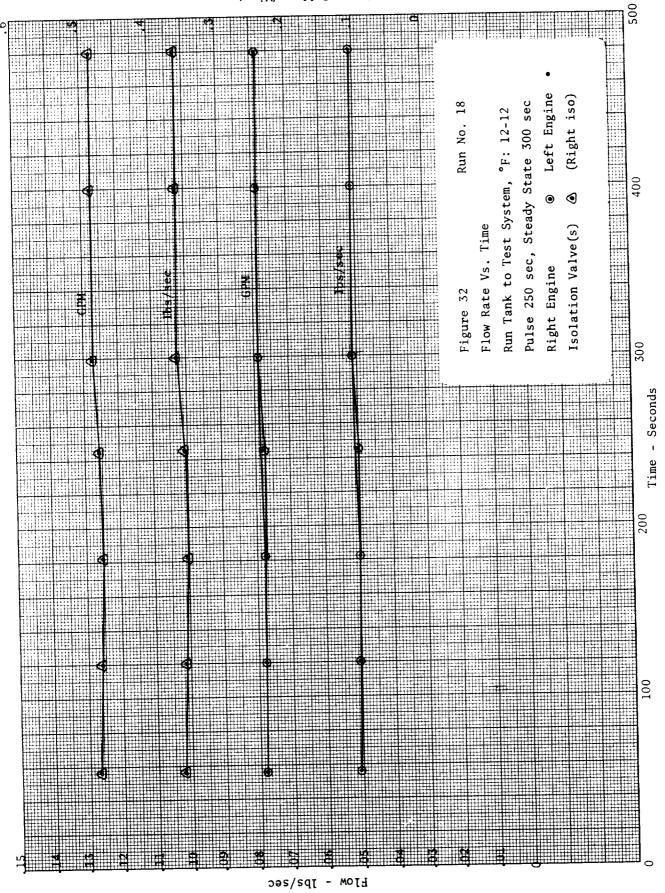


Equivalent Isolation Valve Flow Area - in  $^2$  x  $^{10}$ 

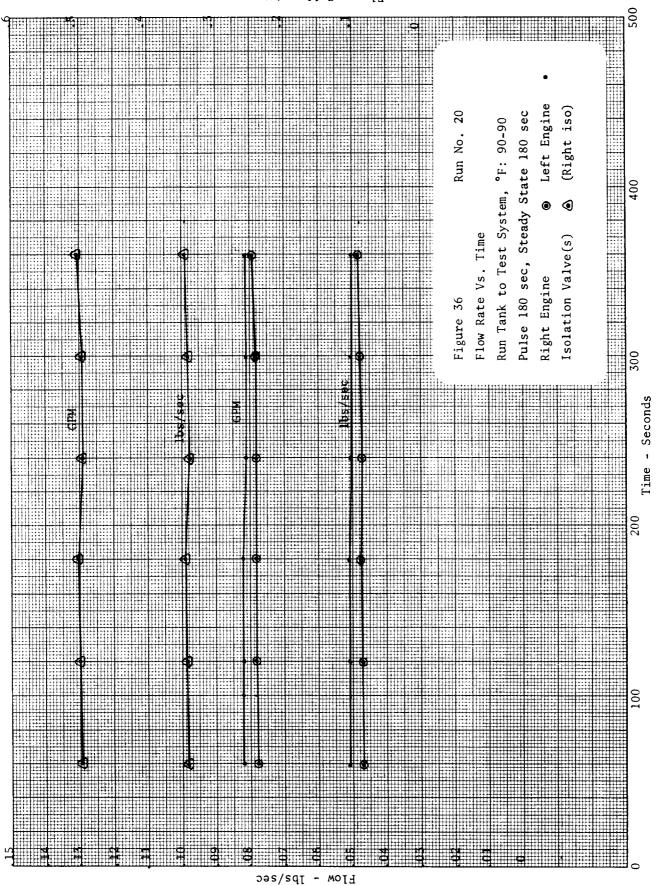


Flow - lbs/sec

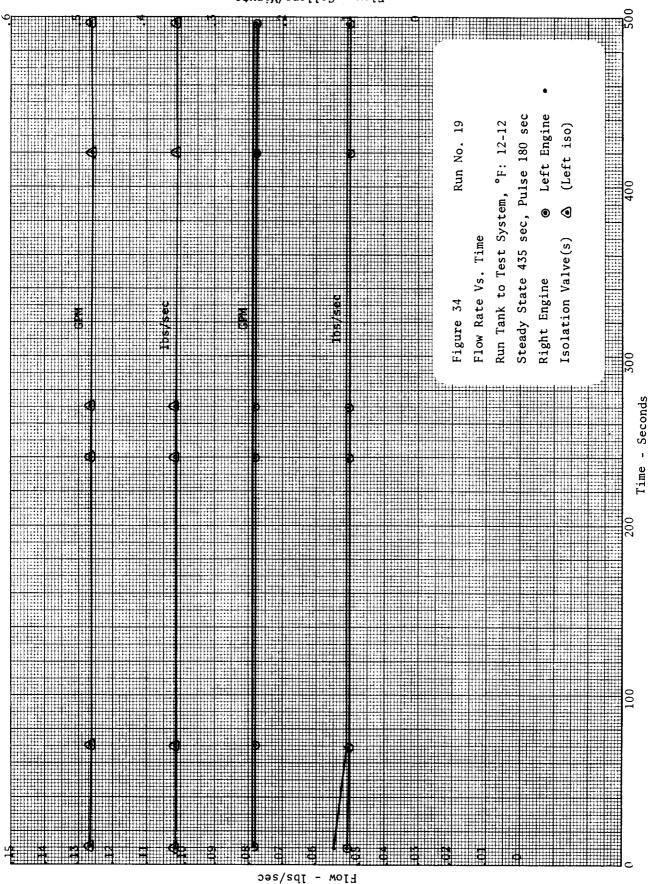


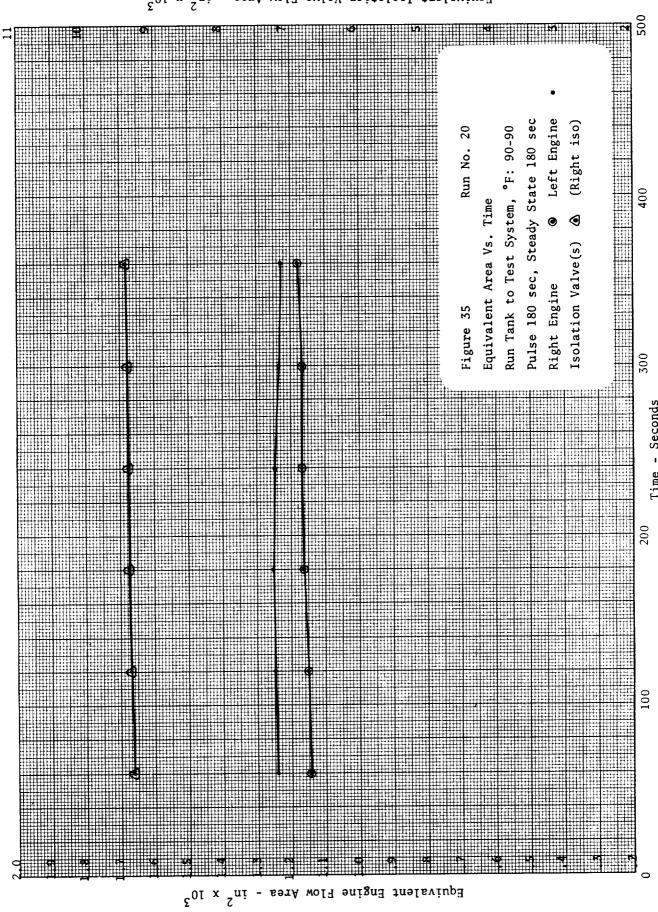


Equivalent Isolation Valve Flow Area - in  $^2$  x  $^10^5$ 

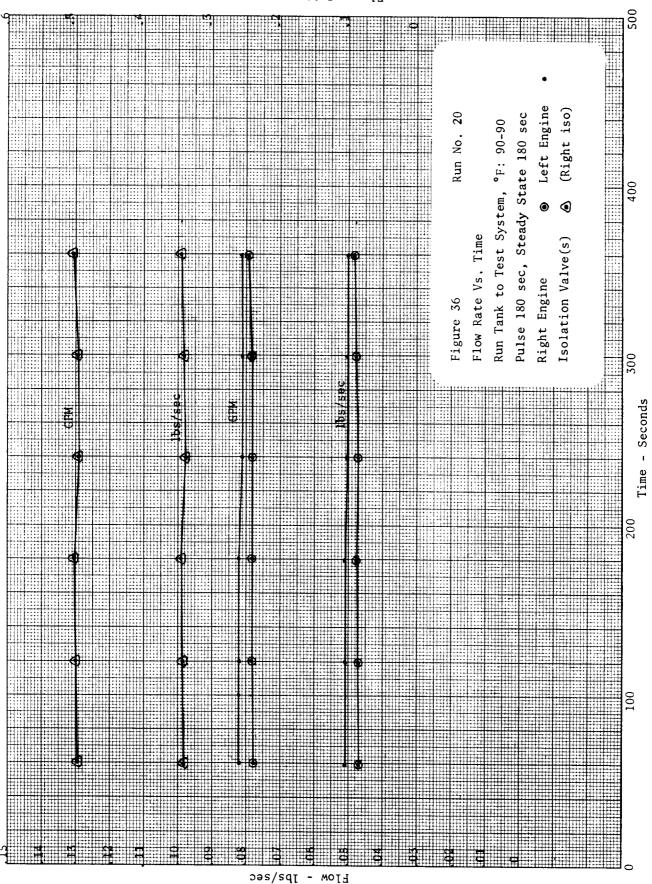


Equivalent Isolation Valve Flow Area - in  $^2$  x  $^{10}$ 

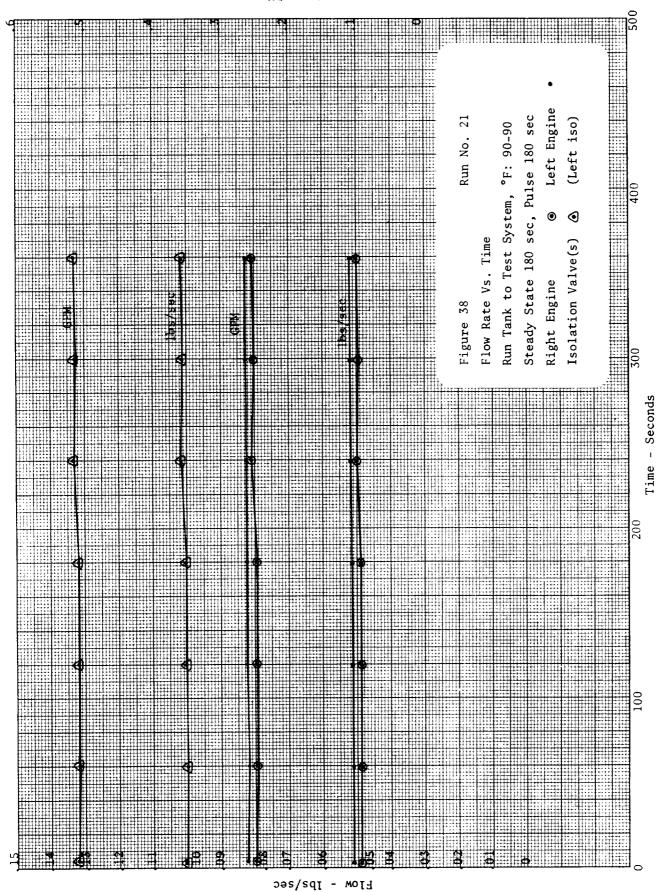




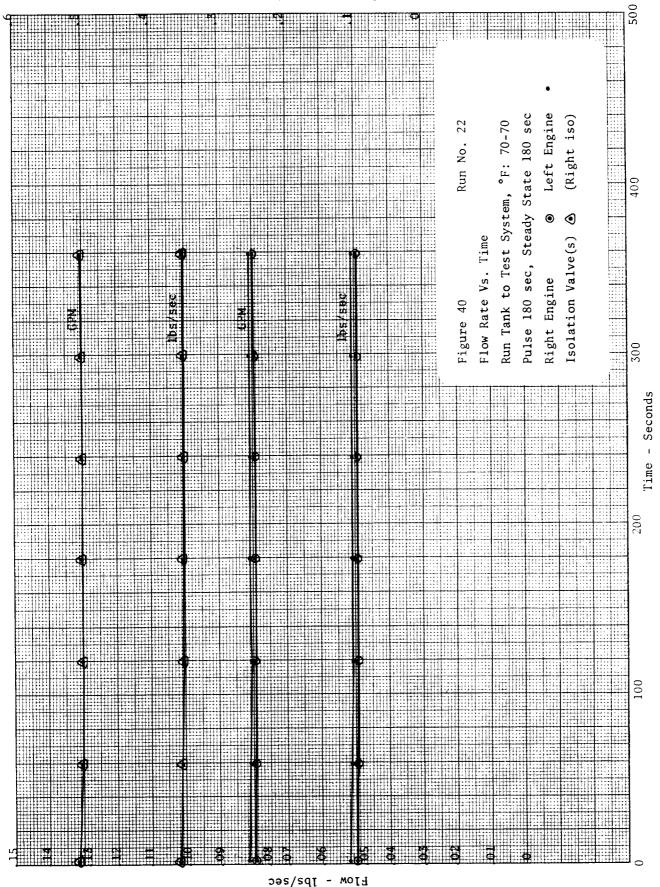
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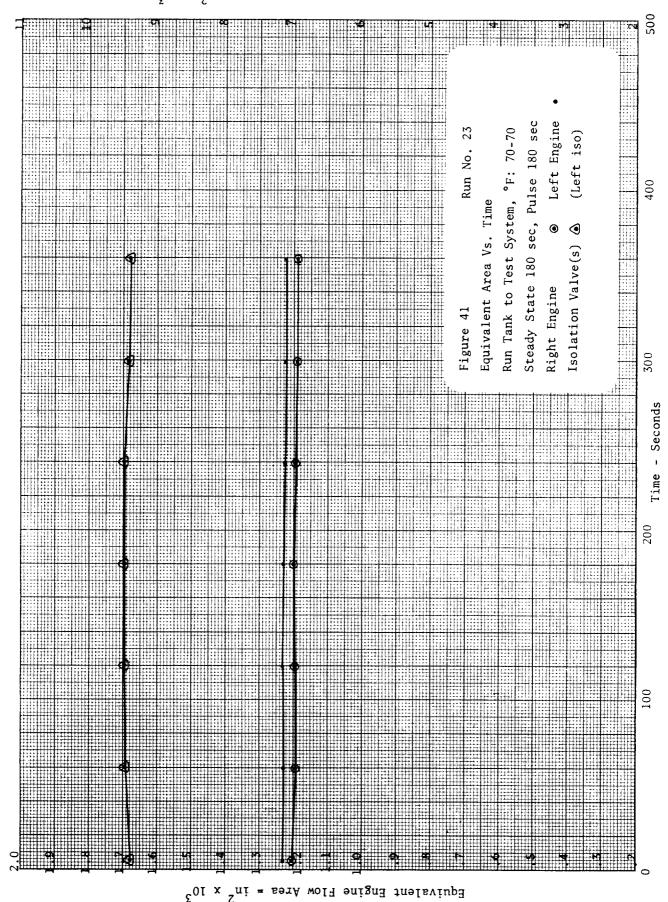


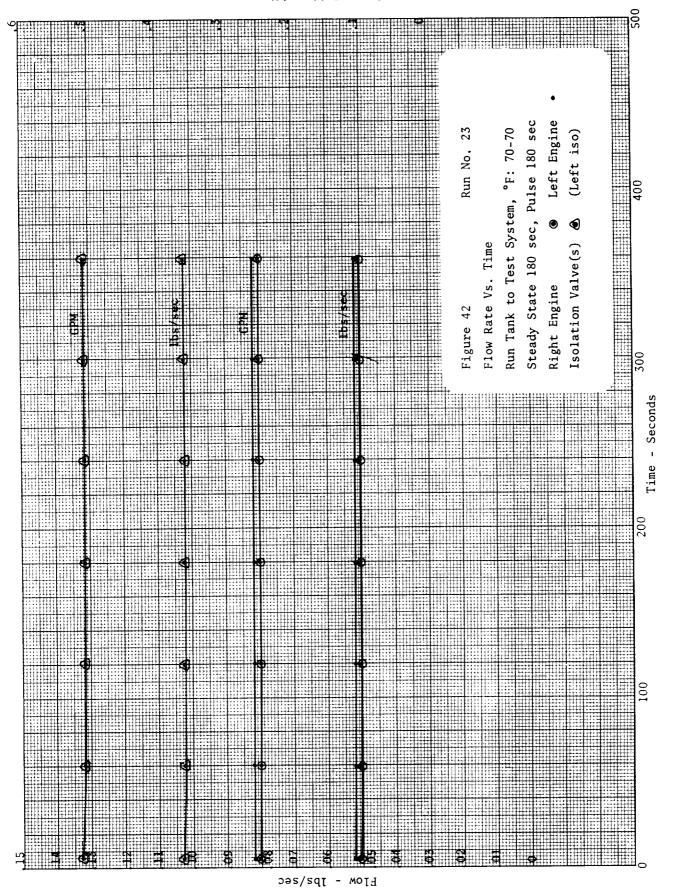
Equivalent Isolation Valve Flow Area -  $in^2 \times 10^3$ 

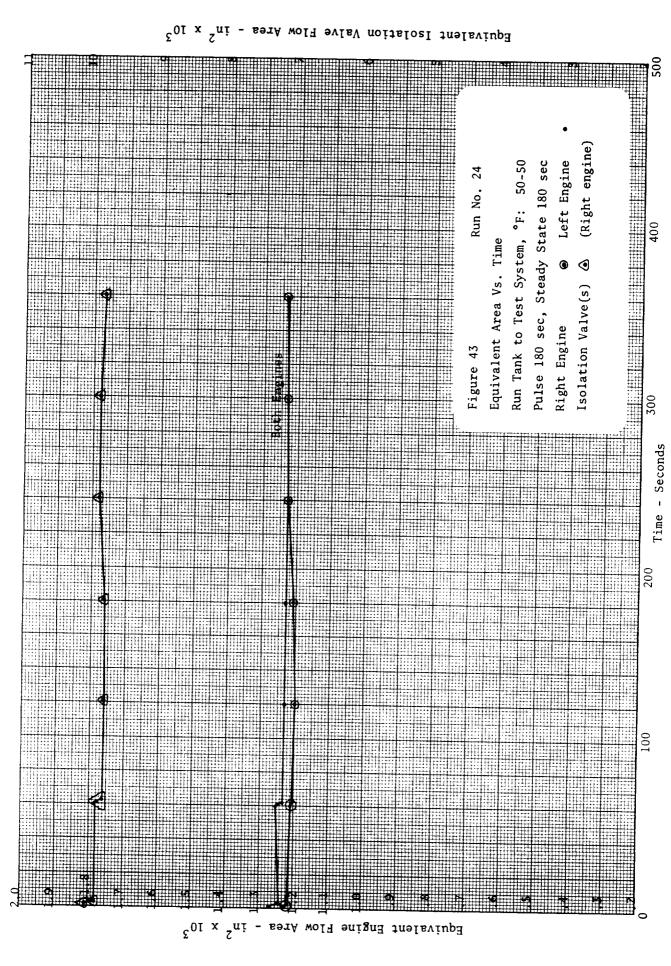


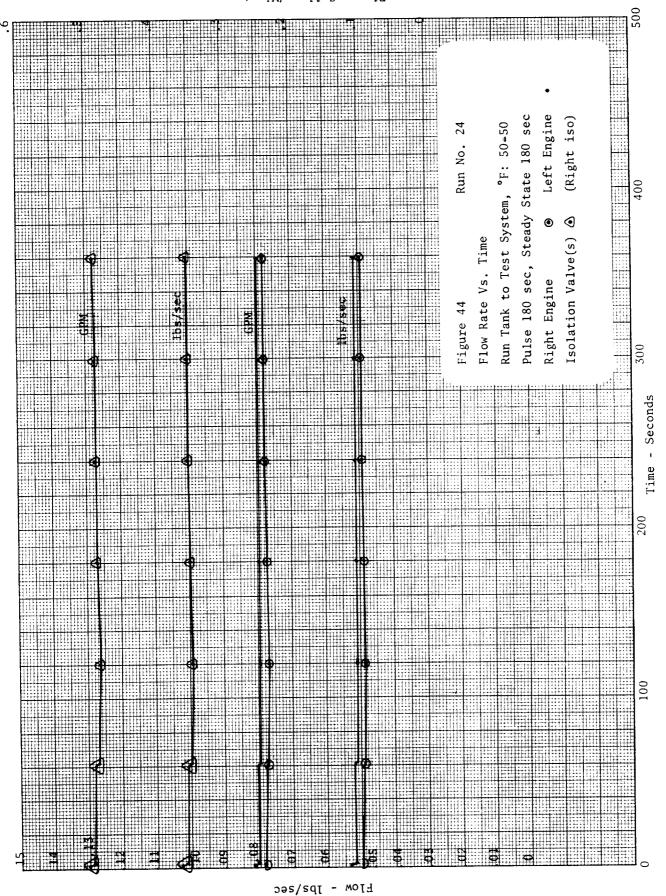
Equivalent Isolation Valve Flow Area - in  $^2$  x  $^2$  noiselent

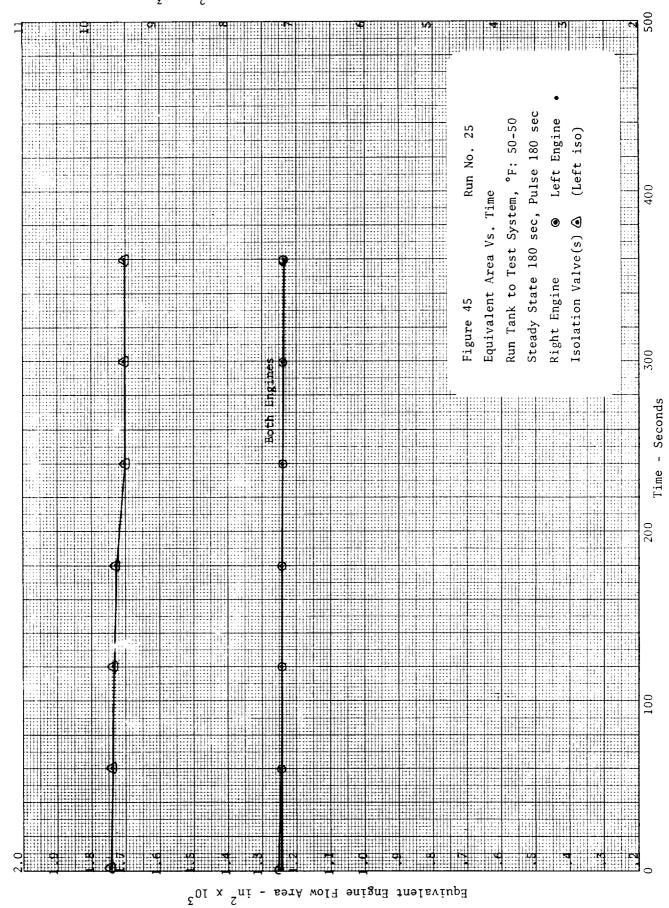


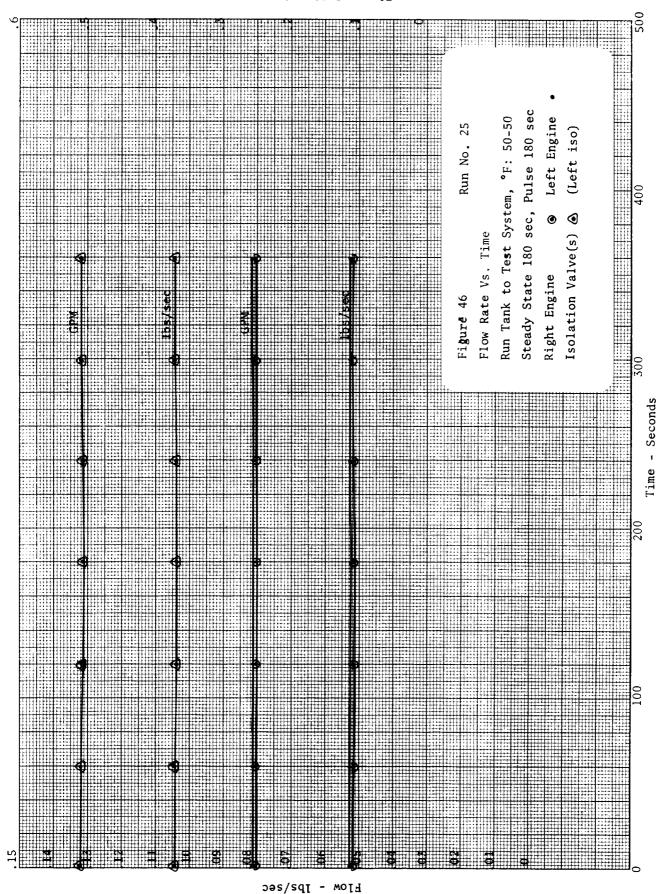


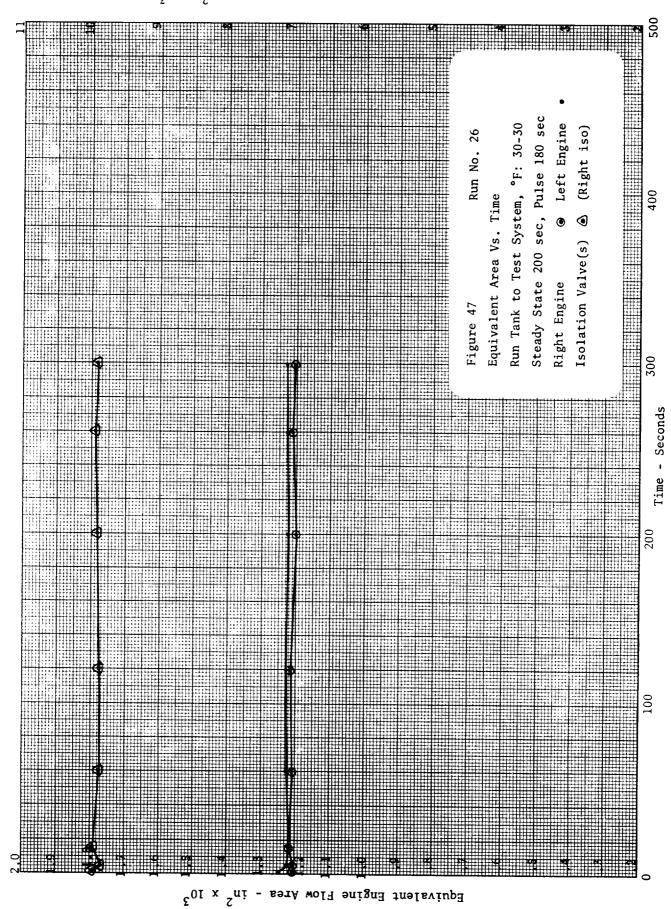


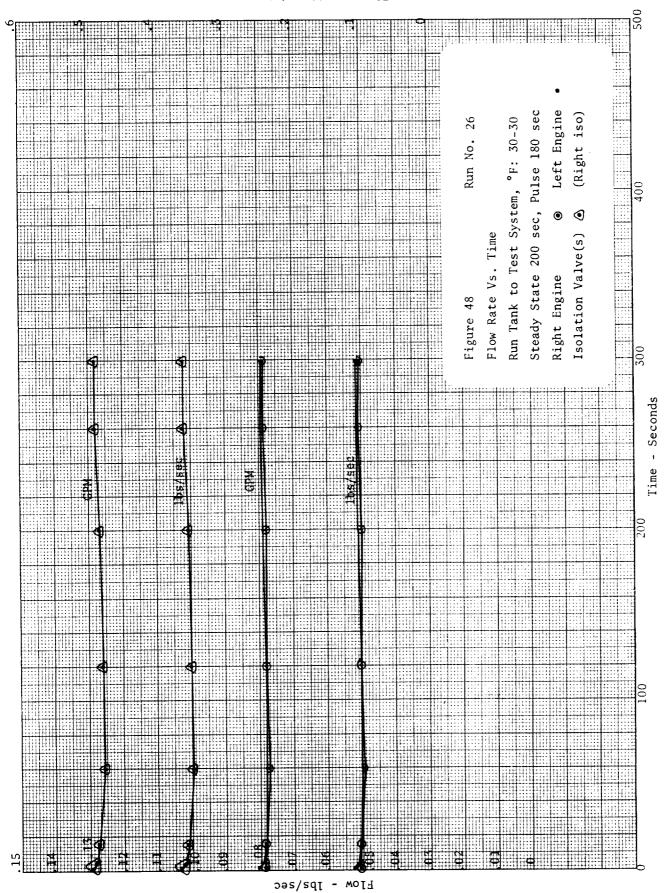




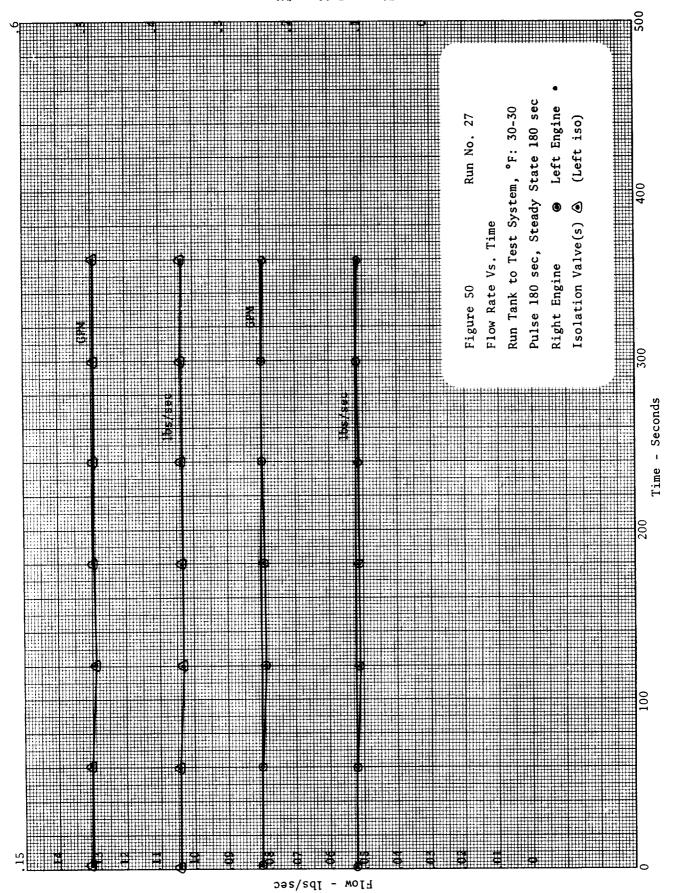




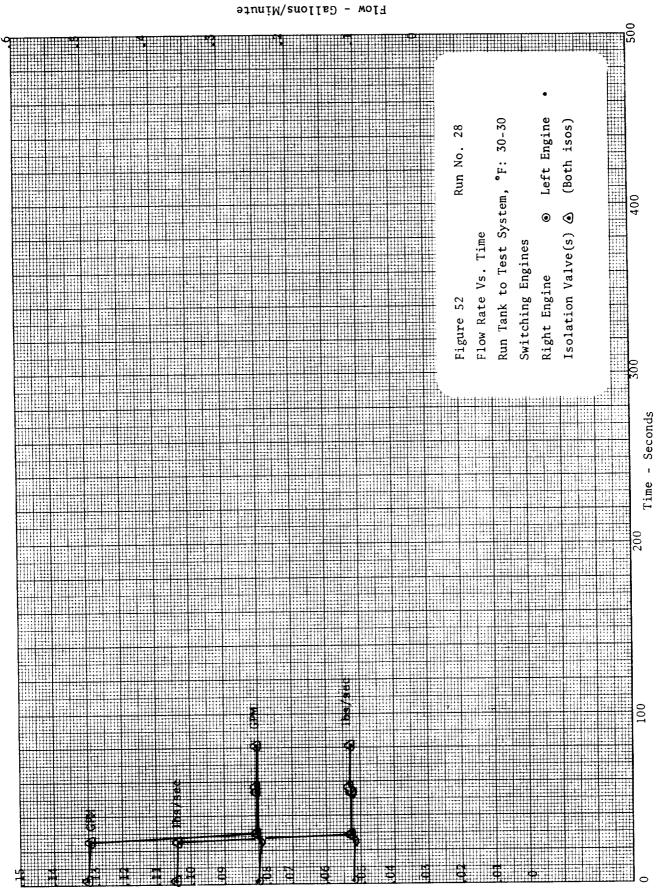




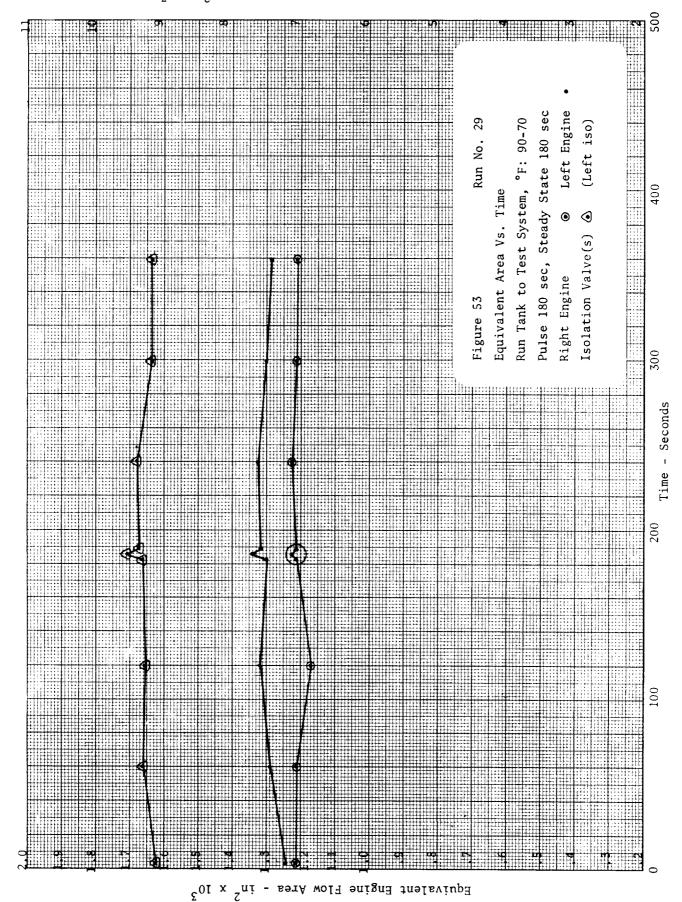
Equivalent Isolation Valve Flow Area - in  $^2$  x  $^10^5$ 

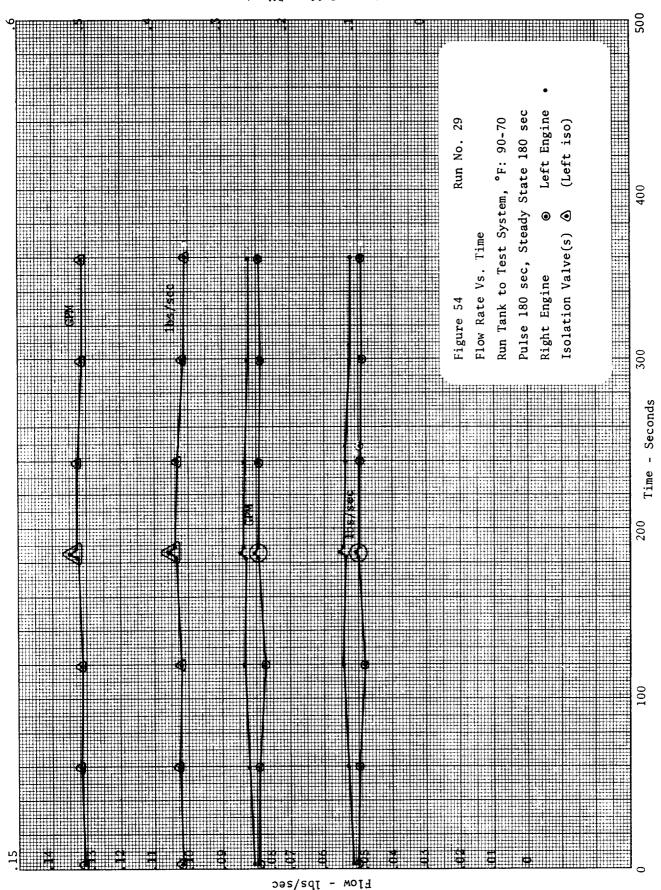


Equivalent Isolation Valve Flow Area -  $in^2 \times 10^3$ 

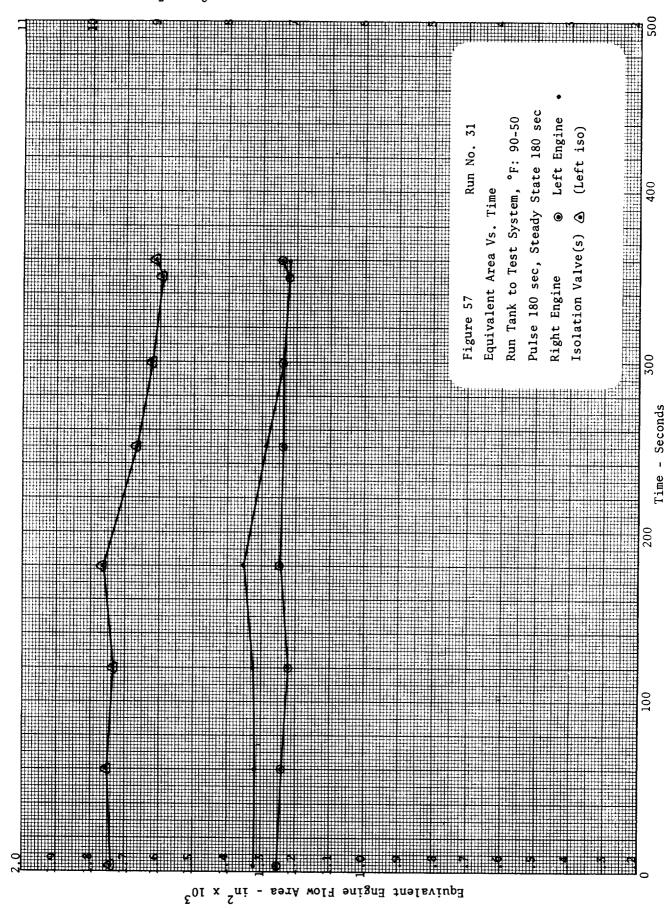


LJOM - Jps/sec

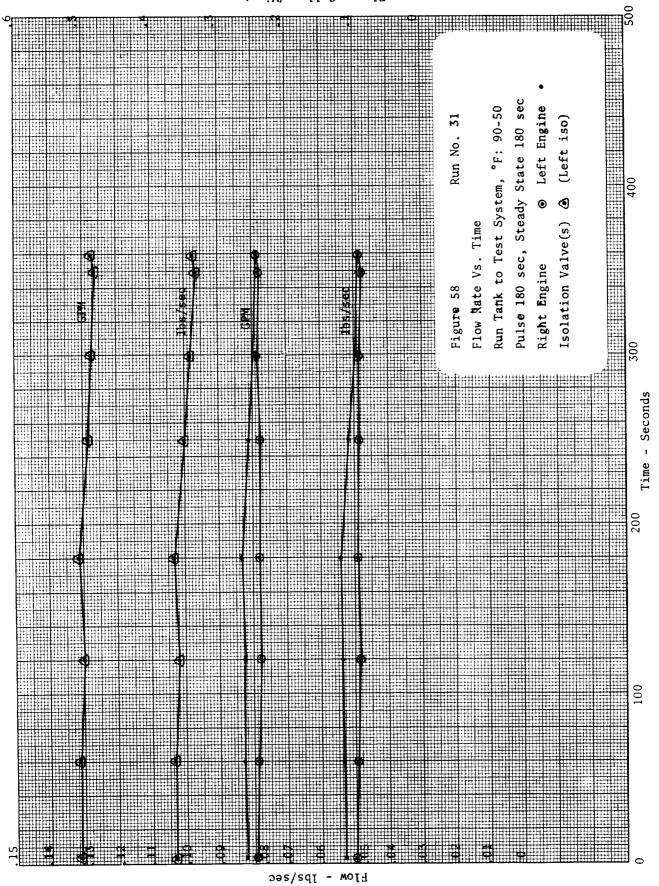


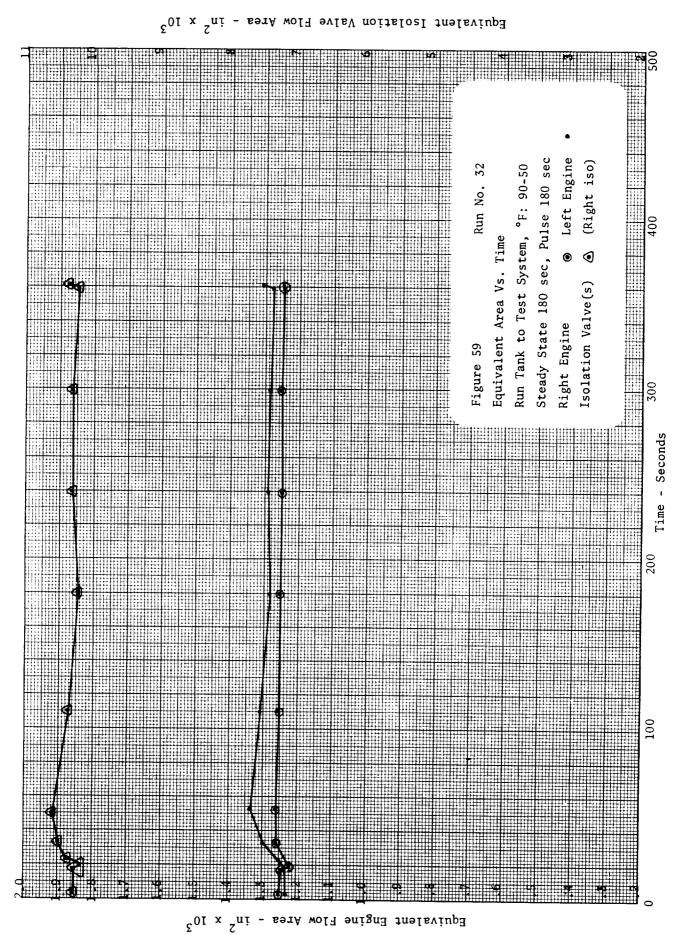


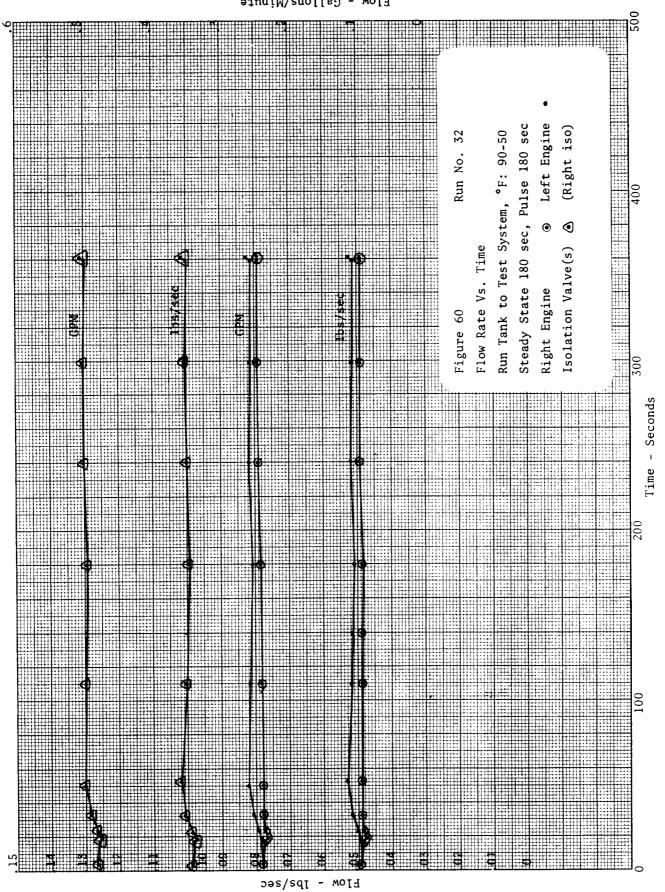
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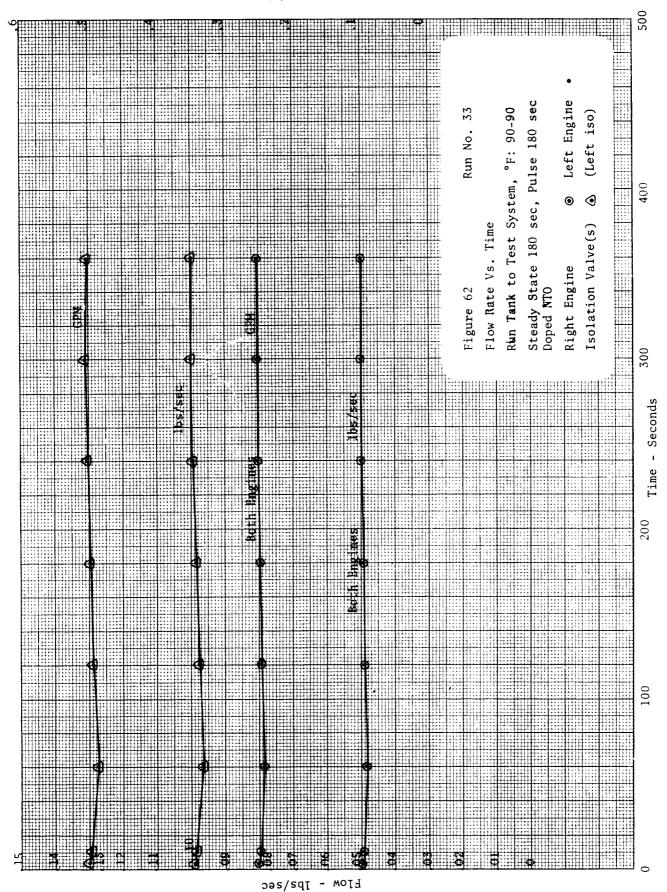
Equivalent Isolation Valve Flow Area - in  $^2$  x  $^2$ 



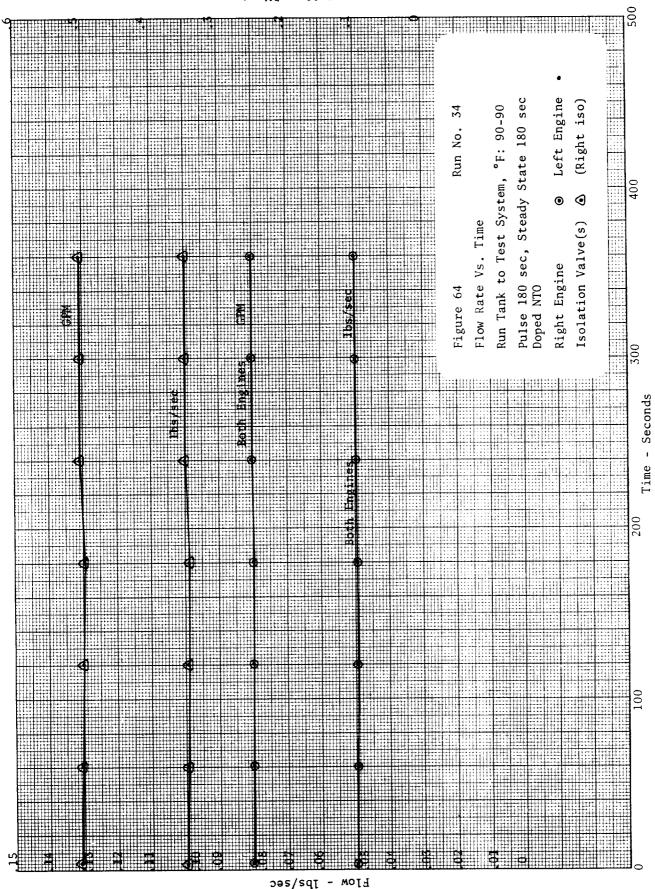


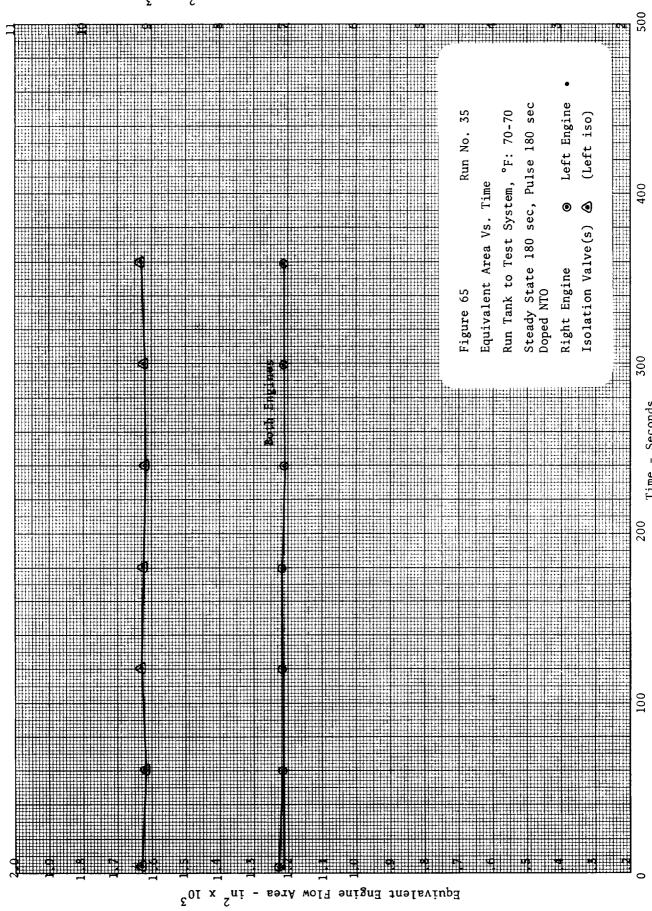


Equivalent Isolation Valve Plow Area -  $in^2 \times 10^3$ 

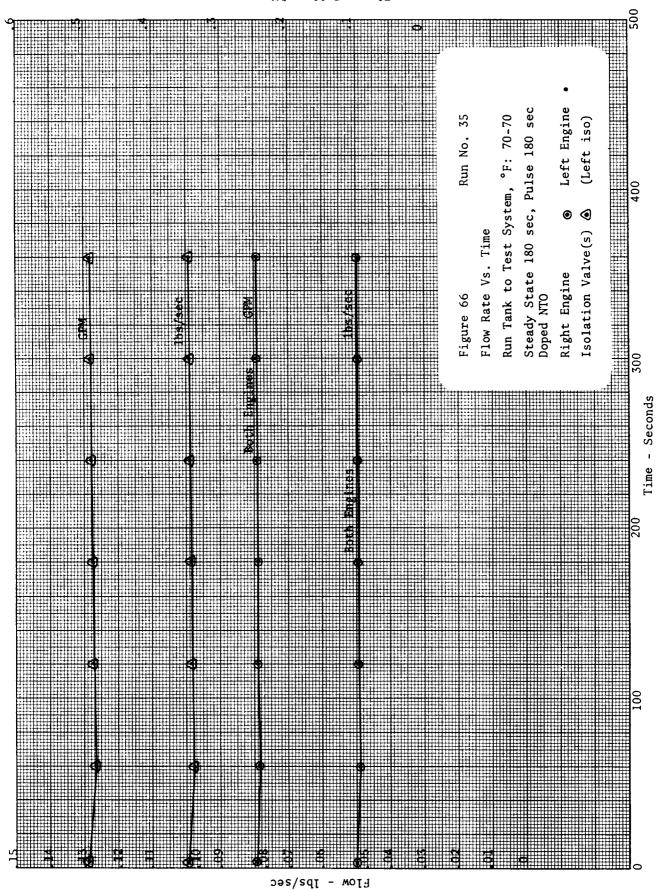


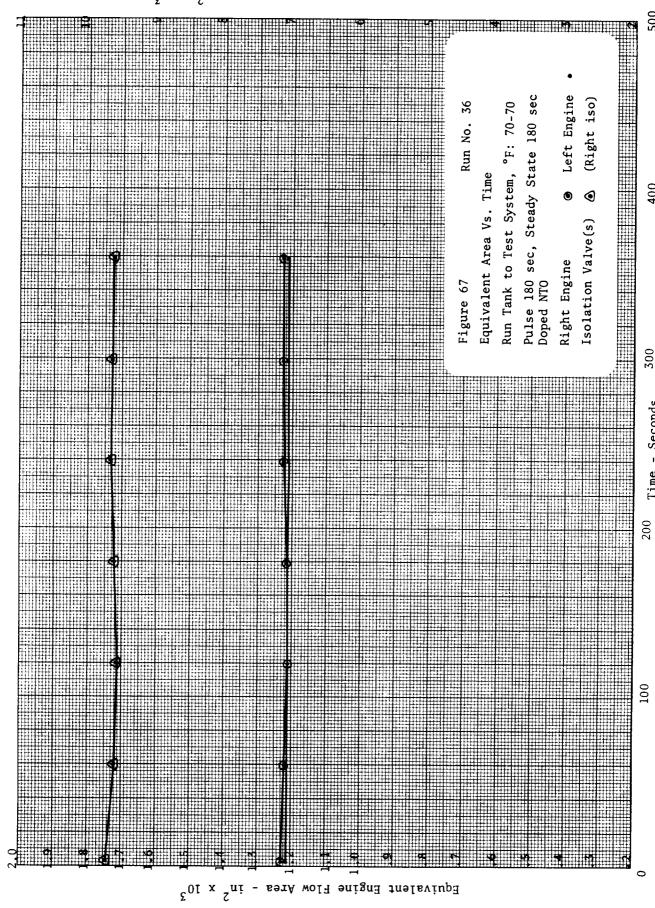
Equivalent Isolation Valve Flow Area - in  $^{\Sigma}$  x  $^{\Omega}$  is the Equivalent Isolation Valve Flow Area - in  $^{\Sigma}$ 



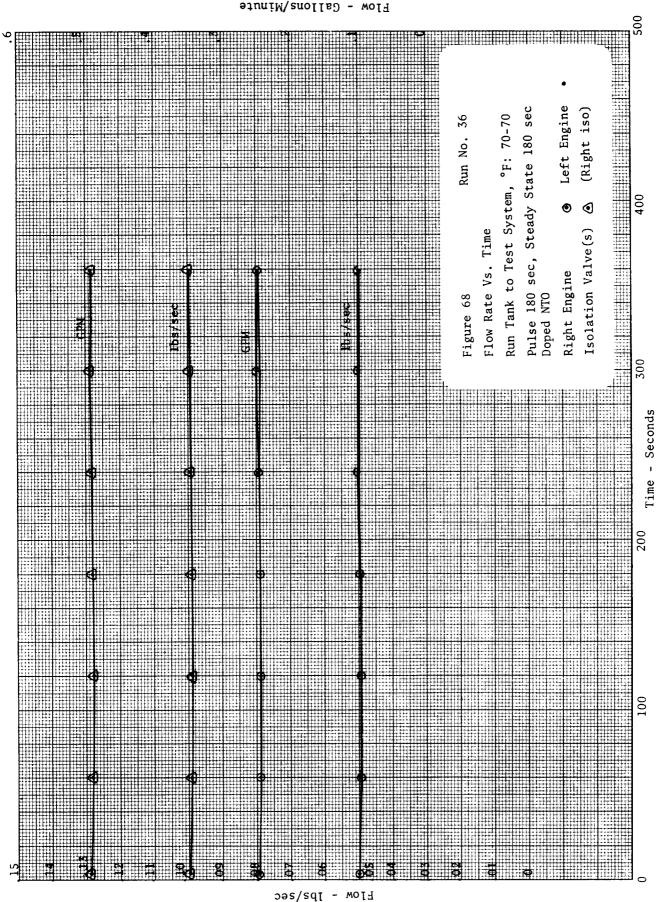


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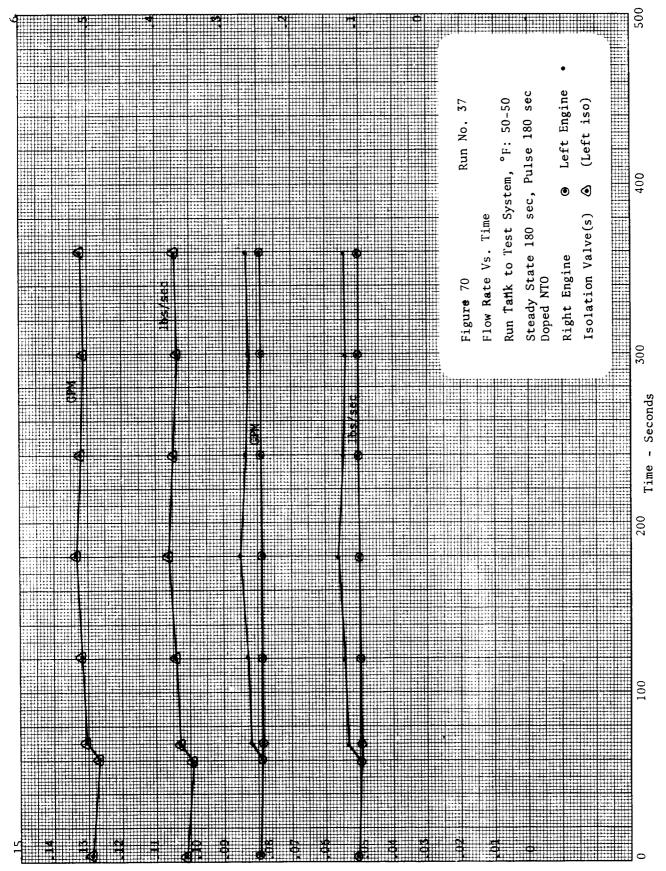




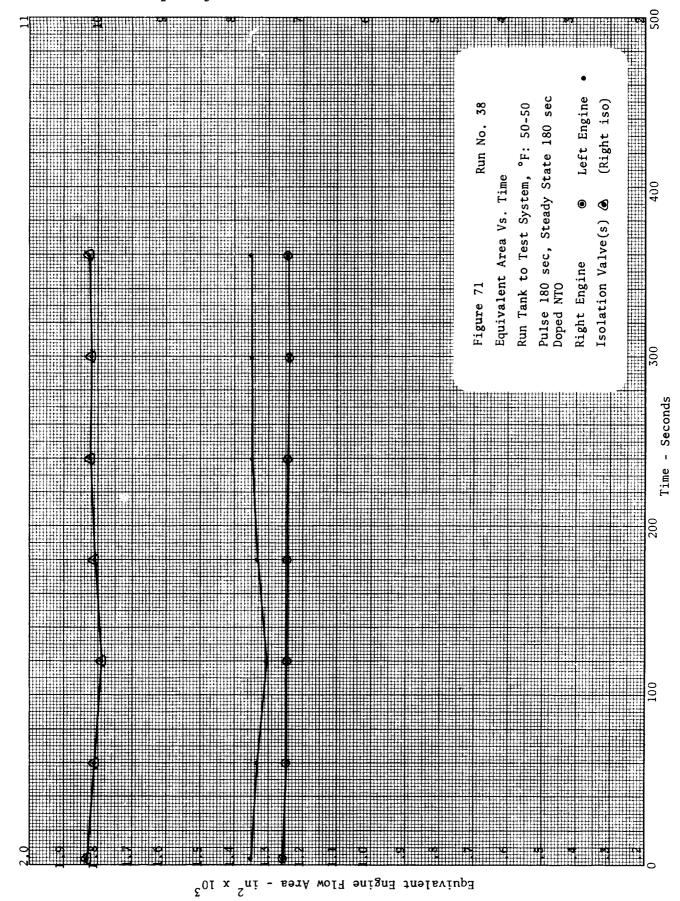
 $\epsilon_{01 \times 2}$  and - sear A wolf evinon Valve Flow Area - in Equivalent



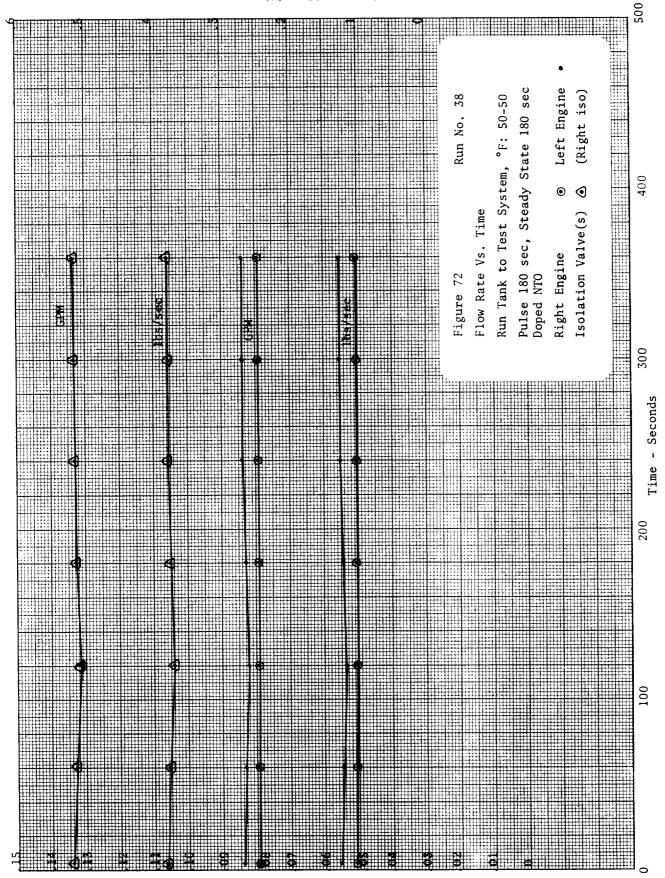
Equivalent Isolation Valve Flow Area -  $in^2 \times 10^5$ 



Flow - lbs/sec

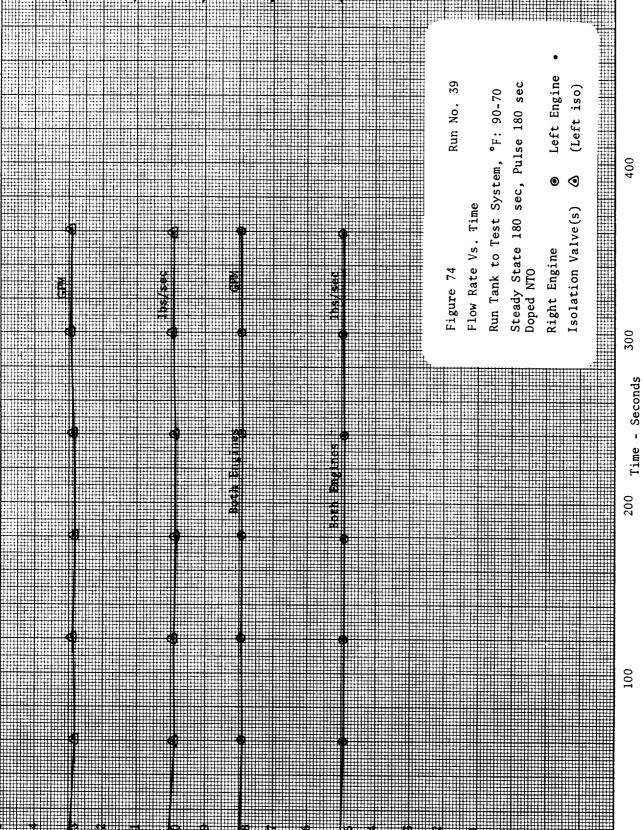


 $\epsilon_{01}$  x  $\epsilon_{01}$  and  $\epsilon_{01}$  and  $\epsilon_{01}$  solution Valve Flow Area -  $\epsilon_{01}$ 



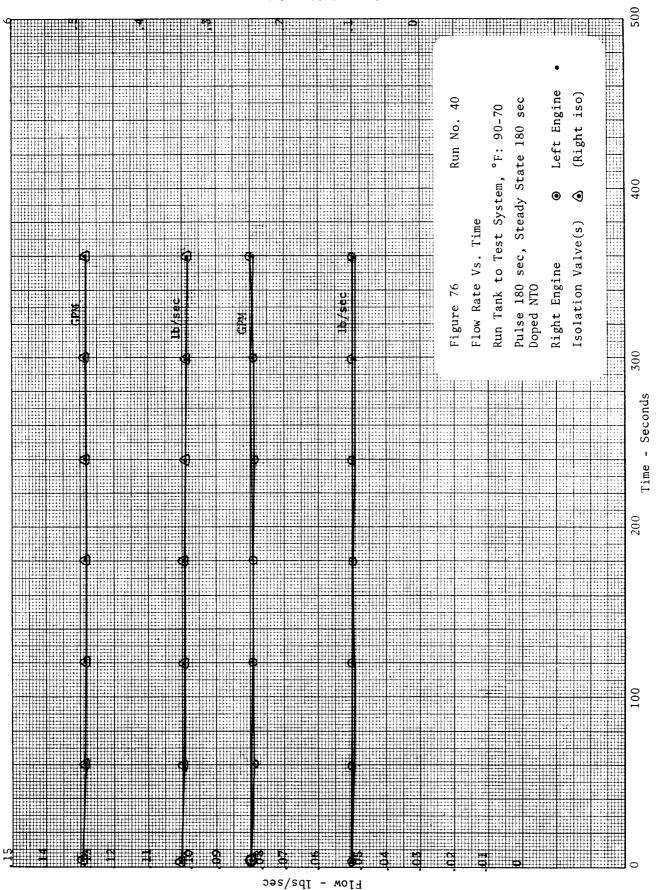
EJOM - Jps/sec

Equivalent Isolation Valve Flow Area - in  $^2$  x  $^2$ 



200

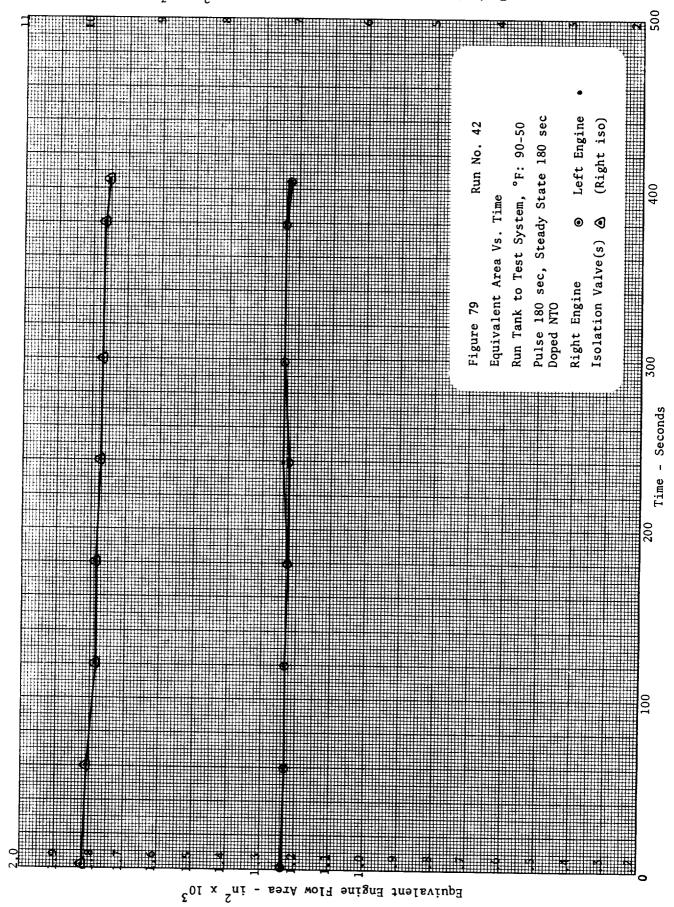
Equivalent Isolation Valve Flow Area - in  $^2$  x  $^{10}$ 

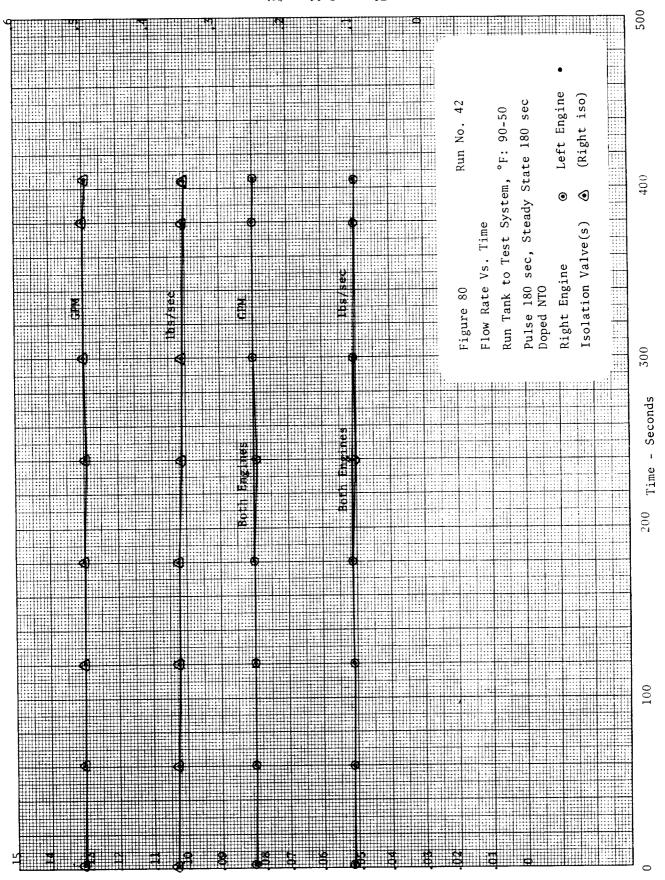


Equivalent Engine Flow Area - in  $^2$  x  $^10^5$ 

Ljow - jps/sec

Flow - Gallons/Minute





LJOM - JPS/sec

## APPENDIX V

This Appendix contains a tabular presentation of the data collected during the flow test phase of NAS 8-21489. Included are flow, pressure drop, inlet and outlet temperature, as well as calculated equivalent area in thousandths of a square inch for the isolation valves and engine. Data on the filters was not included as they did not exhibit flow degradation significantly affecting overall system flow over the test program. This tabular data was used in preparing the plots of equivalent area and flow vs. time presented in Appendix IV. While the plots may be used to examine trends, the tabulations should be used in all cases that an actual flow, or equivalent area value is desired.

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- New York

<b>Z</b>	TIME	S A A E A A E A A E A A E A E A E A E A	ი ეს და£	F G - 10 G - X - S	PRESSURE PS1	OEG F	BUTLET DEG F
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	10	15.840	•2730	• 05049	47.		
	15	5.18	30	00		) K	0 0
	80	80.9	1	517		0 0	200
	30	90.9	$\sim$	515		0	Ö
	<b>4</b> Ծ	4 . 7	ĬĊ.	8		000	Ö
	~	4.57	3	048		20	Ö
	• • •	4.5	3	0496		000	ŏ
	180	2.64	2	0510		00	Š
	~	6 • 1 4	3	0526		000	Ö
	v ·	6.97	292	0541		000	Ö
	•	6.9	9	0540	•	00	Ö
	.,,	*	9	0546	•	ò	Š
	·	3,99	50.5	0933		00	ŏ
	6	3.00	500	1941	7.	00	Ö
•	,	4.64	340	1009		ò	Ö
ALGIT FNGINE	ന	80	• 198	.0355	35,4	Ö	Ö
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	ည် က	0	9	0000•	36•0	Ö	Ö
	တ္တ (	00	00	0000•	32.0	Ö	Ö
	÷ ,	00	000	0000•	33.6	Ö	ò
	O (	8	000	0000	37,8	ò	ò
	U	00.	000	0000	39.7	ġ	ò
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	* [	900	4	)414	38.4	ò	ò
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	, (1)	919	274	507	35.4	ô	ò
	o i	• 17	ĺυ.	504	37.6	ċ	ċ
	ე ე	۲) ا	251	484	36•3	ô	ò
	0 0		277	515	36.0	ô	ċ
	ე :	0 (	_	515	35.0	ċ	ō
	ຸ. ດີ (	۳. •	٠.	8	33.6	ċ	ċ
	ဂ <b>(</b>	<b>.</b> .	4	83	37.8	ċ	ò

	TIME	A A R E A	3 0 1 0 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	г д П д	PRESSURE PS1	INCET	BUTLET DEG E
ω <i>Ζ</i>		ဂ			)	<b>)</b> J	) J
EFT E	120	-	268	96#0	39.7	50	50
	œ	•17	276	0510	40.8	50	50.
	4	920	284	0526	43.0	50.	50.
	O	•24	•2926	•05411	141.30	S	
	9	• 24	292	0540	40.5	50	50
	B	- 25	295	0546	41.3	50	50.
	0	• 22	280	0519	35.0	50	50.
	46	922	284	0526	38.4	50	50
2	<b>N</b>	•27	300	0555	<b>4</b> 2•		•
n Z							
ISBLATION VALVE	വ	3.97	262	0525	9	က်	5
	4 5	4.27	258	0516	O	16.	02.
	67	.47	8	0556	an a	9	m
	N	4.58	265	0509	a)	41.	37.
	O	4 + 23	261	0497	ത	, c	39
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	77	5.20	491	0860		5	\$5
	0	4.90	£83≠	0912		+6•	ខ្មុំ
RIGHT ENGINE		00.0	000	• 0000	1.7	75.	75.
	<del>.</del> Մ	8	0000	• 0000	1.7	75.	ū
	67	80	0000	• 0000	1.7	i	ທີ
	Ŋ	900	000	0000	1.7	10	က်
	605	00	000•	0000	1.7	75.	10
	ന	40.	224	4440	29,3	11	ů
	77	•03	227	0431	28•4	41.	29.
	0	03	226	0427	27.6	Ŏ.	*
LEFT ENGINE	Ŋ	. 13	262	0523	37.1	76.	76.
	÷ Ω	•17	258	0516	34.3		. /
	9	.27	280	0556	34.7	<u>•</u>	o.
	S	900	265	0509	30.4	30	17.
	0	.13	261	2497	29.5	36.	27.
	ന	• 18	259	0492	27.1	36.	27.
	775	1.210	• 2635	•04986	125.65	140.6	131.5
	O	18	556	0484	24.1	41.	31.

	H H E	S Fri		٠	S	ن ح	Ē
z		SQ•1N	E G O	Sdd	PS1	DEG F	DEGF
ISBLATION VALVE	4	4 • 65	76	0550	•		αc
		(')	7	538	_	ָ ה ה	7 6
	w	54.4	9	0537	•	37	, w
	180	4 • 0 9	60	0518	•	4	വ
	-र	3.85	S	8640	Uì	41.	88
	U	4 • 2	3	0497	U1	43	9
	w	4.01	257	0489	U1	43.	41.
	w	4 • 10	253	0492	u١	43.	41.
	w	3.94	256	0487	O.	₩	Ŋ
	-3	3.86	270	0512	9	43.	ţ,
1	O	3,99	• 272	.0517	Ç	43.	± Ω.
RIGHT ENGINE	4	င္ပ	0000	0000	37.6	75.	75.
	$\sim$	8	000•	0000	35.7	10	iÔ
	ณ	8	000	• 0000	36.0	10	١Ô
	90	8	000	0000	35•4	ıÔ	10
	-\$*	8	000•	0000•	33.6	in	in
	0	င္ပ	000•	0000	33.4	10	10
	vo 1	8	000	0000	31,5	10	ı.
	ณ	8	000•	• 0000	31.7	iÔ	i.o
	00	8	000	0000•	30.4	10	iÔ
	#	80	2	8	42,3	10	
	ο.	00	000.	• 0000	44.07	10	
LEFT FNGINE	+	გ	276	0220	37.6	m	
	$\sim$	ر د	271	538	35.7	97.	•
	n i	ຕຸ	269	537	36.0	14.	•
	ഹം.	20	265	3512	35.4	26.	12
	<b>+</b>	9	759	3498	33•6	31.	18
	$\circ$	9	260	1640	33.4	34.	22.
	ഹ	0	~	0489	31.5	35.	25
	<b>α</b> ι.		2539	2492	31,7	36.	27.
	m.	•	256	187	30.4	37.	27.
	54°0	1.166	•2700	.05124	142.39	37.	29
	$\sim$		272	117	# 9 e #	137.9	129.6

	TIME	AREA	M (0)	3 (D)	PRESSURE	INCE IN	BUTLET
2		<b>.</b>	Or CO	1	n	ال 5	3
ISBLATION VALVE		4 • 52	77	580	0	6	9
		4.02	257	538	0	6	<b>+</b>
		4.09	256	0537	0	* # 8	ີນ
		6.32	284	0592	Q)	10.	87.
	S	3.96	274	0546	<b>;</b>	340	23•
	~	3.69	268	0526	ô	37.	30
		37	•2653	.05131	1.09	138.5	134•6
	0	3.32	265	0510	ô	39.	35.
RIGHT ENGINE	-	00.0	000	•0000	50.0	16.	•
,		00	000	0000	32.0	•	•
		000	000	0000	33,9	•	•
	S	00.	000	• 0000	32,3	*	<b>*</b>
		90	8	0000	6.0	ě	ě
	/	900	•000	• 0000	3407	m	ě
	9	90	0000	0000	34.7	œ	9
	0	00.	000	• 0000	36.0	ô	ດໍ
LEFT ENGINE		• 22	277	0580	50.0	6	œ
		• 19	257	0538	32,0	ò	<b>.</b>
		•19	256	0537	33+9	ċ	å
		.33	284	0592	32.3	* * *	ည်
	9	• 25	274	0546	36+0	07	ċ
	~		258	0526	34.7	*8	97.
	•	•19	265	0513	34.7	ë	<b>.</b>
	900	1.182	65	510	36•	27.	15
9 Z )					•		
ISBLATION VALVE	<b>e</b> C)	3.06	220	6940	00	ċ	•
		3.99	221	0465	<u> </u>	<b>6</b> 2•	41.
	N	3.86	25	457	œ	30	14.
	360	73	225	0436	00	6	ည်
	0	2.50	23	0428	00	41.	37.
PIGHT ENGINE			.2207	•04633	130•43	00 • <del>↑</del> ==	16.0
		<b>*</b> 0	4	0465	30.8	9	•
	N	25	S	0457	31.7	6	57.
	360	29	225	9640	31.7	ည်	9
	0	0	23	<b>\$</b> 28	31,5	30	18

	<b>T</b> ME	AREA SQ.IN	F Ω ⊃U 3 Σ	ir α ⊐ α α α	PRESSURE PS1		OUTLET OFG F
6 U 9 N D	<i>7</i>	<u></u>			•	<b>)</b>	<b>)</b>
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	9	8	000	00000	31.7	00	00
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	13	90.9	7	9660	Å	່ານ	ิ้
	<b>6</b> 7	15.907	• 4741	7660	-	ō	ā
	S S	5.71	2	2660	œ	0	. <b>.</b>
	27	5.62	76	99	S.	m	ó
	34	5.73	<u>س</u>	1040	7	18	Š
	99 9	5.75	515	1066	4	21.	0
	25	9 34 9	498	1023	Ŋ	32	202
		5.19	491	200	7	35	23
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	3	5.12	475	0940	00	41.	35
	O	5,05	475	0922	Č	43	39.
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	348	5.17	478	0917	Ž	4 4	•
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	0	60 ·	• 477	.0911	õ	10.	· (F)
ALCHI ENGINE	<del>s (</del> B	င္ပ	ဝ္ဂ	8	ŏ	11.	13.
	ο.	-	なりな	0471	94.5	•	÷
	<b>3</b> 1	• 90	200	0471	49.1	*	~
	<b>\</b> ;	0.	ないの	0471	26.3		•
	0	00	4	0471	25,8	•	0
	<b>ε</b>	000	\$	0470	25.2		
	oo •••	80	4	70	24.5		•
	22	90	4	0470	24.1	•	
	27	• 10	9	74	23.4		•
	t M		9	,73	22.0	•	
	33	• 11	~	1	122.61	2 % 0 % 0 %	27.3

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IGHT ENGIN		1.10	23	0461	22.3	*	
	~	60	4	4555	22.1	03	œ
	-	604	40	0440	₹93°	SO	ë
	45	•	.2219	•04362	121.74	125.8	9.46
	0	40	2	429	23,2	31.	11.
	00	<b>†</b> 0•	83	0428	24.3	9₩•	18.
	4	10	ţ	0428	24.1	36•	÷
	0	• 0	4	0428	22.3	36.	23•
	O	40	224	0426	23.2	38	26.
LEFT ENGINE		00.	000	000	0	*	• 9
		.15	277	0583	67.8	*	•9
	4	• 21	274	575	49.1	ហំ	•
		• 13	52	0529	1:0	<b>.</b>	•
		• 18	251	0526	30 • 8	ċ	•
		.18	50	525	30.4	<b>:</b>	,
		• 18	249	0523	0 + OE	*	
		• 18	6	0522	29.5		<b>®</b>
	27	• 19	249	523	28.9	ċ	9
		98	7	0567	28.5	<b>'</b>	ô
		• 36	284	0592	28.2	លំ	*
		• 30	73	0561	28.5	ດໍ	-
		.27	67	0545	28.2	å	ċ
	-	-25	59	0519	29,5	14.	*
	4	• 19	254	0503	28.6	20.	*
		•17	253	0493	30.0	÷	÷
	$\infty$	• 16	34	0490	31.5	34.	<b>1</b> 5
	*	15	54	<b>4</b> 80 80	31.5	36.	16.
	0	.15	53	0487	31.5	36.	17.
	0	• 1 4	53	0484	32+3	38.	21.
∞ Z ⊃							
SOLAT	ເດ	9.07	522	090	~	7	-
		9.00	518	1052	0	<u>`</u>	-
		8 • 95	517	1049	Ö		-
	09	18+975	.5176	•10508	60•2	57.7	57.7
		9.01	518	1053	0	7	-
		9 • 00	518	1052	Ò	7•	. /

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∞ <i>Z</i> ⊃	<i>Z</i> ⊷	E D				i J	1
RIGHT ENGINE		N	63	534	28,8		. ′
		22	61	530	27,7	<b>.</b> ′	<u>'</u>
	9	2 S	50	529	56+9	<u>`</u>	7.
		22	60	529	27.6	7.	-
		S	60	529	28,3	7.	
		22	60	529	27.8		7.
LEFT ENGINE	വ	2	• 2590	• 05259		57.7	57.7
		8	5	0521	56.9		7.
		ដូ	56	0520	26.0	7.	7
		겂	57	0521	56.6		-
	80	2	50	524	27.3	1	. 7
		-	37	0523	56.	/	7.
<b>¬</b>							
ISBLATIBN VALVE	ო	9.75	9	072	0	ò	-
		9.56	2	054	0	6	00
	S	9.26	22	053	9	ô	ċ
	00	9.50	3	054	Ç	ċ	ò
	0	9.00	S S	052	7	9	•9
		• 95	S S	055	7	ô	-
	S	8 • 95	23	1052	7	ò	-
RIGHT ENGINE		• 25	99	539	27.3	ċ	ö
		• გე	80	0527	5406	3	ດໍ
	S	• 23	61	0526	26.0	6	•
	180	42	61	0526	26.9	ô	
	0	• 23	62	0527	26∙3	<b>:</b>	<b>•</b>
	9	• 23	62	0528	56.6	-	9
	S	• 23	261	0526	25,6	÷	Ö
LEFT ENGINE	ന	• N	62	0532	26∙1	ċ	ò
		* 0.	60	526	2343	ŝ	å
	S	, ,	61	527	9.42	6	•9
	Ø	• ಬಿ	62	50 50 50 50	25,3	ċ	7
	200	1.240	•2623	• 05276	124•85	71•1	9 • 8 9
	9	13	<b>5</b> 5	527	25.1	-	6
	Q	62	61	522	5 t . 3	<b>.</b>	•

	TIME	AREA	3 O J L	FLOX	PRESSURE	INLET	BUTLET
		-	α	α.	ഗ	E C	S W
0 7 2							
ISBLATION VALVE	Ŋ	7.56	13	040	<b>*</b>	ċ	6
	a	40	513	038	*	9	9
	~	44.6	13	1036	*	6	•
RIGHT ENGINE	ហ	80	257	0522	29.65	*	ċ
	N	S	257	0521	28.6	•	ດ້
	~	20	257	520	28.8	6	*
LEFT ENGINE	350	1 • 198	• 2558	.05183	128.08	62•3	0.09
	S	80	255	0517	27.5	•9	ຄໍ
	1	5	55	516	27.6	•	4
z J							
ISOLATION VALVE	ന	8.58	512	047	•	ċ	ċ
:		72	7	1045	∹	ຜູ້	က်
		8.91	512	046	Ç	-	•
		9.15	16	052	0	•	ស្វ
	S	60.6	516	1048	0	9	6
		8.96	515	041	0	6	9
PIGHT ENGINE		23	57	0525	22.5	6	•
		23	257	0525	22,5	9	6
		23	257	0525	22.3	6	6
	9	1.247	.2597	•05297	123,31	0.09	52.0
	S	25	59	0527	22.4	•9	•9
		4	259	0523	22.5	•	ë
LEFT ENGINE		22	S	0521	21.9	6	6
		2	34	0520	21.8	9	9
		25	₩ 40	0550	21.6	6	•
		ന	56	0522	22.5	•	ů
	N	3	256	520	21.6	ហ	•
	180	33	56	0518	21.6	·	ě
ET Z O							
SOLATI	260	9	506	1034	C		O
	S	8 • 17	Ξ	1038	S	6	6
	0	0.8	•5081	•10256	•	69•1	69•1
	0	7.95	05	1018	ů	6	6

	TIME	A A E A	3 H	F (	PRESSURE	INCET	BUTLET
N 13	Z ₩ ►	3 W	1	<b>1</b>	S	ы С	(U)
IGHT ENGINE	260	1.22	53	0518	21.4	ċ	•
	350	ΩI.	• 2568	.05213	122.12	8,99	57.7
	0	S S	35	0514	20.9	6	. +
	Ó	2	53	0510	20.6	6	•
	Ø.	25	252	0515	20.3	ċ	6
	ũ	ე ე	57	0516	20.8	9	
	Ö	N)	253	0510	19.7	9	. 4
:	Õ	20	57	508	19:4	6	• 9
		č			•		)
	<b>*</b> (	7	-	40	•	ŏ	õ
	000	6	501	033	•	Ň	Ğ
	0 <b>6</b>	7.9	က်	034	`*	9	ū
	ည်	င္	ö	037	`*	ŏ	į
	w.	7.99	ö	036		ŏ	~
	U	7.86	ဂ	926	·"	ம	
	w	7.7	ထ	017	"	Š	٠.
	240	7.75	ដ	015	(')	_	
	$\mathbf{c}$	7.70	5	013	•	. ~	
ALGHI ENGINE	<b>.</b>	Ç.	36	0526	23•3		
	80	CO.	10	0523	2107	Š	
	30	m N	(1)	0519	20.8	<u>_</u>	
	ည	1 • 2 4 2	• 2556	.05218	21.0		
	<b>O</b>	ຸດ	S	0521	20.5	•	•
	N (	CO I	256	0517	2106	•	
	0 0 0	22	9	0512	22.0	å	
	<b>*</b> (	ָט פּ	256	0513	23.0	•	. 0
	0	N N	ດຄວ	0509	22.3		•
	<b>+</b> (	S	<b>2014</b>	0522	22,5	. ^	
	0 N	20	7	516	20.8	. ^	
	0	200	251	0514	0.08	~	
	20	S S	Š	0515	20.0	*	•
	9	ر س	ű	0515	19.6	•	•
	V	S	ű	609	20.7	•	•
	×00	2	ű	0.5	21.0	•	•
	0 <del>1</del> 0	<del>ظ</del> ا	m	909	22.0	•	•
	0	o O	(U	03	•	85.9	78•3

	Σ F	A D	•	_	S	N L	UTU
	•	Z	Σ 1 α. 	Sdd	PSI	DEGF	DEG F
Z							
ISBLATION VALVE	S	.05	464	011	œ	ô	ë
	00	9.93	491	1005	φ	ô	ຜ
	S	96	490	1001	6	•	*
	0	•64	491	0983	7	ີວ	
RIGHT ENGINE	S	0	244	6640	16,9	œ	9
	00	8	245	0502	16,9	9	9
	S	2	245	0501	16.1	ů	ċ
	0	S	247	0495	15.0	•	សំ
LEFT ENGINE	S CU	1.238	• 2504	•05120	115,77	48.6	49.1
	00	2	246	0503	15,7	9	6
	2	2	242	0200	15,0	က်	ö
	004	8	243	0487	14.0	‡	ຄ
Z							
ISBLATION VALVE	++	10.	530	0998	4 • 00	32.	47.
•	~	8	519	0973	4.7	19	39.
	ิณ	80	513	0960	4 • 1	03	29.
RIGHT ENGINE	-	• 24 4	59	489	15,0	43.	35.
 	~	2	25.1	0472	13,3	43.	37.
	C	8	247	1940	14.6	430	39•
LEFT BNGINE	**	30	271	0509	3.0	143.8	137.5
	~	S	30	501	11.1	43.	41.
	226	1.272	.2653	040	12.	43.	42.
C Z 17							
ISBLATION VALVE		; ;	542	1005	1.7	ċ	ċ
		97	531	9860	4.0	ċ	83
		55	664	9860	* 0	00	• 9
		65	490	6460	۳. ٥	4	ល
	S	m	490	4760	0.3	7	•
		82	487	0983	*	*	31.
RIGHT ENGINE	-	25	262	0487	18.6	50.	<b>₽</b>
		100	257	6440	19.2	<b>•</b>	+
		S	250	0471	18.6	6	32
	$\infty$	S	242	0476	16.6	6	80
	150	1 • 173	• 2455	.04891	117.69	78.6	80•0
	0		544	<b>#6#0</b>	18.0	6	ŝ

	⊒ M E	Z Z S S S S S S S S S S S S S S S S S S	₽ Ω 9 Σ 3	r σ ⊐ σ ο ο	PAESSURE PS1	INCET	BUTLET DFG F
U N 17 C B		Δ				ı J	i
EFT EN		30	SO OCI	0518	17.6	50.	50
		5	274	0507	18.0	39.	50
		15	549	4940	17,3	-	m
		16	243	0472	15.3	77.	13.
	S	•17	<b>t</b>	<b>¥</b> 805	16,2	ູ່	* *
	300	17	243	O	116.62	0.04 4.0	68•0
2 7 S							
SOLATI	ഥ	•64	486	1024	4.	à	ด้
	U	• 54	82	1015	*	ึ้	์
	00	• 49	77	1005	<del>د</del>	ณ	ů
	4	• 56	81	013	<b>₽</b>	ò	å
	0	• 62	8	030	លិ	å	ด้
	0	• 50	80	028	9	ด้	ิล
	∞	• 45	486	024		å	Ġ
	S	• 45	85	021	•	å	ิด
	~	• 46	85	023	•	ė	ė
RIGHT ENGINE	ഗ	• ? 1	242	509	15.6	å	ė
	N	90	239	504	15.2	ė	è
	$\infty$	920	37	499	13.1	ė	å
	#	90	238	0502	14.6	ė	ė
	0	• 23	245	0517	15.0	å	ė
	00	1.217	• 2432	•05121	116.38	å	ů
	∞ :	÷2	いたり	0203	16.5	ໍ່	ů
	n.	90	0	0507	16.0	ů	ė
i	$\sim$ 1	• 21	₩ 10 10 10 10 10 10 10 10 10 10 10 10 10	0509	16.6	ŝ	å
LEFT ENGINE	Ω	20 20	N 4 4	0514	10.9	å	ໍ່
	N.	• 10 4	Ų.	0511	10.2	å	ė
	$\infty$	• 24	240	0506	08.50	ė	å
	4	- 25	242	0511	4.60	ů	å
	O	• 20 50	243	0513	9.60	å	å
	O.	• 26	ហ្វ	516	2 60	å	å
	$\infty$	• 26	244	514	19.1	å	å
	in.	900	4	514	0.60	å	å
	^	U	243	513	2.60	12.0	12.0

	E L	Tr.	_	لــ	S	A F	
	•	Z 1 • 0 S	Σ 1 Ω 0	PPS	1Sd	DEG F	
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ISBLATION VALVE	10	.27	80	017	ο	å	ů
	20	•17	8	015	0	å	å
	*	000	ζÚ O	017	0	ů	ů
	270	920	82	017	ô	å	ູ້
	, Qu	• 1 4	80	010	o	å	ດໍ
	g	• 19	50	014	Ç	å	å
	9	• 16	<b>60</b>	1014	ô	ů	å
		90	3	1013	Û	ů	ດ້
RIGHT ENGINE	-	• 30	239	0504	8 , 6	ė	ů
· ·	~	<b>.</b>	•2396	• 02046	69*16	12.0	12.0
	*	.31	239	0504	7,5	ຄໍ	ູ້
	~	98	39	0504	9,3	ຄໍ	ċ
	C	٠ 28	238	0502	01.1	Š	ů
	g	• 26	238	0502	03.0	ė	ė
	560	.26	238	0502	03.6	ູ້	ė
	-	74.	239	0504	03.6	ໍ້	ໍ້
LEFT ENGINE	-	.22	<b>#</b> 3	512	4 00	ณ์	ė
	~	• 22	242	0511	1401	ů	ů
	4	• 23	243	0512	13.7	ė	ů
	/	• 23	243	0512	13.7	å	ຸ້
	G	• 22	241	0508	1306	Ġ	ວໍ
	Ð	• 23	243	0512	13.7	ດໍ	้
	9	.23	243	0512	13,6	ດໍ	ด้
	610	S	241	0508	13,3	å	ů
N N					•		
ISBLATION VALVE		• 30	98	0983	00	ċ	Ö
			• 5002	• 09872	7 005	000	000
	œ	•37	9	0993	0	•	• •
	4	• 36	96	0979	9	ċ	
	O	.37	ф <b>20</b>	0983	/•	ċ	ċ
	•	4.	၉၀	0993	<b>•</b>	ċ	ċ
RIGHT ENGINE	9	• 1 4	39	0473	19,5	ċ	ċ
	S	15	40	0475	18.9	ċ	ċ
	00	•16	<del>1</del> 3	0480	18,9	ċ	ċ
	4	•17	0	475	<b>\</b>	ċ	ô
	0	• 16	43	0480	18,3	ô	ċ
	360	•	*	0488	19.9	ċ	ċ

	TIME	A A B B A B A B A B A B A B A B A B A B	3 ⊕ Σ .⊒ û	Г 0 П 0 З	PRESSURE PRI	1	BUTLET
U N 20	<b>-</b>	E C		-	)	ט ט	ם ט
EFT EN		4	258	0510	18.0	ċ	ô
	S	4	259	0511	18.0	ċ	ċ
	00	25	259	513	17.9	ò	Ô
	240	S T	•2525	•05037	114.85	0.06	0.06
	0	23	255	0503	17.3	ċ	Ö
	9	22	252	504	19.0	ô	ò
U N 01							,
SOLATI	m	• 22	509	003	m.	ċ	Ô
	9	•17	507	00	(L)	ô	ō
	U	សួល	509	000	'n	ં	Ö
	180	9 • 237	• 5092	• 10050	8.31	0.06	0.06
	4	• 34	516	013	e,	ô	Ö
	O	• 11	512	012	•	ô	ò
1	Q		515	017	*	ô	ō
RIGHT ENGINE	m	•16	249	492	54.6	ô	Ö
	Q	• 16	248	689	0	ô	Ô
	N	•16	248	0489	24.1	ċ	ċ
	$\infty$	•16	4 00	0489	24.1	ċ	ò
	240	• 19	200	0502	0 * * 2	ò	Ô
	0	•17	251	0495	23.9	ô	ô
	9	• 19	253	0200	24.5	ô	ô
LEFT ENGINE		• 22	99	513	23,3	ô	Ô
	9	ლ ი	259	0511	21.3	•	Ö
	120	გე	261	0515	22.7	ċ	Ô
	00	ტ ტ	261	0515	22.7	ô	ċ
	4	გე	261	0516	22.6	ċ	ċ
	0		261	0516	55.6	÷	ċ
:	9	• 23	251	0516	22.8	ċ	ċ
N N N							
SBLATI	cu ِ	9.799	ហ	1021	4	œ	œ
	9	• 87	502	1011	ດ	œ	00
	120	•81	$\frac{1}{2}$	.10087	'n	œ	00
	∞	• 76	501	1009	<b>ب</b>	œ	·
	4	• 68	500	1001	<b>+</b>	00	· ∞
	0	* 00	501	1008	•	68•0	68.0

	TIME	AREA SO. IN	3 ΦΣ 1	г д П д	PRESSURE	. I C	BUTLET
U N 22	<b>-</b>	Ē	-		)	3	ם ט
VALV	360	82	8	007	ď	∞	×
IGHT ENGIN	ณ	-	*S*8*	• 05019	117.38	0.89	68.0
	Ø	٠ 0	47	0498	17:0	·	80
	120	00.	47	0497	17.2	00	00
	œ	0 0 •	247	0497	17.8	00	00
	-\$	9 8 9	247	0498	17,3	00	00
	O	-20	247	1640	17.7	00	80
1	Q	02.	247	7640	17,3	80	٠ 00
LEFT ENGINE	N	• P.	258	0519	19.6	80	00
	9	• 23	55	0513	18.4	œ	00
	N	<b>.</b> 23	254	0511	18.4	80	00
	∞	<b>€</b> 23	254	0512	18.9	·	00
	240	a	50	508	7	· 🚓	. 00
	0	• 23	254	0511	18.8	80	•
	9	23	253	0510	18,2	m	•
2 23					ı	,	
SOLATI	Ŋ	• 39	-	) E Q	10	œ	00
	W	• 46	9	024	Ç	· œ	00
	U	.47	80	023	9	•	00
	w	.47	507	022	9	00	00
	•	9 † •	6	200	0	00	•
	300	$\mathbf{O}$	507	028	7	ထိ	00
	<b>v</b>	• 38	507	1028	7	00	• 000
RIGHT ENGINE	വ	920	Ω,	0508	22.0	oC	· •
	Ø	• 19	250	0503	21.6	တိ	· 00
	N	800	250	0503	21.1	on on	00
	180	90	250	0503	20.7	80	00
	4	9	250	0503	21.4	ő	m
	0	61.	250	0203	55.6	00	·
í	9	• 19	230	0503	22•6		*
LEFT ENGINE		23	259	0522	23.6	~	~
	9	• 23	258	0550	23.0	~	
	C	~	258	519	22.4	*	•
	∞	~	257	0518	22.0	~	*
	4	<b>^</b> .	257	317	22.3	*	*
	300	1 • 224	•2576	.05184	123.46	*	. ~
	9	^ .	257	1 8	23	0-89	68.0

	<u>Σ</u>	AREA SQ•IN	Ε Θ Θ Σ Θ Σ	F 0 □ 0 © 0	PAESSURE PSI	N I I I I I I I I I I I I I I I I I I I	BUTLET DEG F
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RIGHT ENGINE			/ OD → → D OD  0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0 0 0	0000000	0000000	
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	00000000000000000000000000000000000000		0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	. 05153 . 05092 . 05092 . 05092 . 05092			

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ISBLATION VALVE	1	•71	509	041	7	ò	ċ
•	09	•		.10411		50•0	20•0
	N	•66	507	037	00	ċ	ċ
	00	• 63	507	036	00	ċ	ô
	0 <del>1</del> 0	.50	508	038	0	ċ	ô
	0	•51	510	1042	∵	ċ	ċ
	9	•51	509	041	8.1	ċ	ċ
RIGHT ENGINE		.25	252	0516	15.3	ċ	ċ
			252	0516	15,9	ċ	ċ
	S	* C.	251	513	5.7	ċ	ċ
	œ	• 24 •	251	0513	15,4	ċ	ċ
	4	• 23	251	0514	16.7	ċ	ċ
		• 24 4	253	517	18.0	ċ	ô
	9	• 23	252	0516	18.0	ċ	ċ
LEFT ENGINE		• 24	257	0525	21.0	ċ	ċ
		• 10.	257	525	21.1	ċ	ċ
	a	• •	256	523	20.8	ô	ċ
	00	.23	255	522	50.02	ċ	ċ
	4	<b>6</b> 0	256	0523	21.12	ô	ò
	0	€23	57	525	22.3	ċ	ċ
	360	23	257	0525	22.	ċ	ċ
z o							
ISBLATION VALVE		• 93	φ 00	934	S.	ċ	
	<b>.</b>	.83	493	1023	S.	ċ	ċ
		• 93	4 80 80	1014	0	ċ	ô
	<b>9</b>	.87	80	966	00	ċ	ô
	S	.87	83	1003	00	ô	ċ
	0	• 90	486	1009	Q.	ċ	ċ
		• 93	93	023	0	ċ	ċ
	0	•91	491	1021	0.7	ċ	ċ
RIGHT ENGINE		99	242	0508	18,0	ċ	ċ
	<b>.</b>	• 20	245	0508	18.6	ô	ċ
		•21	24	506	16.0	ċ	ċ
		-20	238	495	11.9	Ô	ċ
	S	.21	240	<b>4</b> 99	12.7	ċ	ċ
	200		.2411	• 05005	115,92	30•0	ċ
	9	•	245	0508	17.7	ò	ċ

	TIME	ARE A	π.Ω Πα Φ Σ.	7 0 7 0 8 0	PRESSURE PSI	INCET	OUTLET DEG E
U N 26 C B	<i>Z</i> ⊢ <i>Z</i>			-	)	ם ט	ל ע
RIGHT ENGINE		8	<b>6</b>	0505	17.3	ċ	ô
EFF BNGIN	<b>+</b>	4	9	526	18.8	ċ	Ö
	4	22	248	0515	18.6	ò	ò
		S	244	0507	16.0	ò	ō
	9	22	241	0501	1119	ô	ò
	S	25	242	0503	12.7	å	ċ
	200	Ñ	.2451	.05088	115.92	30•0	30.08
	9	22	248	0515	17.7	ò	ô
	0	S	240	515	17.3	ò	ċ
N Z					)	•	•
ISBLATIBN VALVE	H	• 57	O	042	O.	Č	ċ
	9	• 10.	5	040	9	Ö	
	ฒ	• 49	95	029	00	Ö	Ċ
	œ	• #	97	035	0	Ö	Č
	3	10.	80	934	œ	Ö	Ċ
	O	• 53	90	980	00	å	Ô
	360	• 49	97	031	00	Ö	ô
RIGHT ENGINE		-22	51	521	21.4	ဲ	Ô
	Q	32	င္သ	519	20.6	ô	Ö
	N	• 19	ឃុំ	509	20.6	Ô	Ô
	∞	• 19	242	0510	22.52	ô	Ô
	4	•16	247	0514	29.62	ċ	ô
	300	9	<b>+</b>	514	21.3	ဲ	ô
	9	o o	247	0513	20.7	ċ	Ô
LEFT ENGINE		้า	251	0521	21.4	ċ	ċ
	9	22.	251	0521	20.6	ċ	
	N	20.0	250	0519	50.6	÷	ċ
	∞	•25°	10	0522	22.23	÷	÷
	4	Ų.	0	0519	21.5	÷	•
	000	1.219	• 2504	•05199	121.38	÷	•
	9	ผู	249	0518	20.7	30•0	30.0

	T I ME	A B B B B B B B B B B B B B B B B B B B	7 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	F 0 T 0 S 00	PRESSURE PSI	INCET	BUTLET DEG F
N Z		•				İ	
ISBLATION VALVE	N	7.73	502	045	ന	ċ	О
		7.84	498	035	ď	ċ	ċ
		6.50	253	525	9	ċ	ô
		6.50	53	0525	9	ċ	ċ
		6 • 63	255	0529	•	ċ	ċ
	8	• 51	253	0526	9	ò	ċ
RIGHT ENGINE		1.22	250	0520	19.7	ċ	ċ
		- 22	249	0517	18.5	ċ	ċ
		22	253	0525	22,8	ċ	ċ
		.22	253	.0525	23.2	ô	ô
		000	000	0000	21.5	ċ	ċ
	8	00.	0000•0	00000 • 0	121,62	30•0	30.0
LEFT ENGINE		• 23	.251	0522	19,7	ċ	ċ
		929	249	.0517	18,5	ċ	ċ
		000	000	0000	22.8	ċ	ċ
		000	000	0000	23.2	ċ	ċ
		* C •	.255	0529	21.5	ċ	ċ
	80		253	526	21.6	ċ	ċ
80 Z							
SOLATI	m	• 13	504	015	+	9	•
		•31	60	025	E (	7	
	S	• 29	506	020	<b>ب</b>	ô	
	$\infty$	• 32	513	032	4	-	œ
	186	• 53	4	1056	*	<b>÷</b>	<b>*</b>
	œ	• 38	515	037	4	<b>.</b>	œ
	4	0 * •	514	1029	က္	ລໍ	ດໍ
	0	• 18	506	1010	<b>‡</b>	7	ល
	9	• 18	6	600	*		•
RIGHT ENGINE		•21	248	0501	17.1	• 9	•
		• 22	247	0497	15.5	7	-
	120	1.172	• 2385	• 04800	115•3g	67.7	67.7
	$\infty$	-21	248	6640	16.1	œ	œ
	00	- 22	250	0504	16.0	œ	œ
	00	• 21	47	497	15.5	•	œ
		- 22	247	4640	13.0	ů	+
	0	÷	244	0487	15.6	S.	<b>Ф</b>
	9	•21	46	± 00 €	140	•	•

	TIME	A 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	₩ 0 X	æ 60 (d 11 (d	PRESSURE	INI	BUTLET
X 0 0 62 X D X	<b>⊷</b>	E C	Į.	Ĺ	n	ם ע	<u>ب</u>
EFT ENGINE	m	1 . 24	255	514	17.4		•
	9	S.	.2623	• 05282	115,54	67.5	
	N	31	268	0540	15.3	7	
	00	9	265	533	16.1	00	00
	∞	34	274	0551	16.0	· 00	00
	00	3	258	0539	15,5	· ∞	00
	240	35	267	0534	13.0	ċ	•
	0	30	282	522	12.6		. 60
= = = = = = = = = = = = = = = = = = = =	Ö	00	261	0519	14.0	85.4	81.5
TABLATTEN VALVE	c				•		
* H C * * C + C + C + C + C + C + C + C + C	າ (	•	X) (X	ν 1 00	7	5	2
	O C	9	00	970	9	Ň	œ
	(A)	96.6	o O	900	Ç	9	ō
	36	0.15	8	200	9	ō	
	u,	0.15	8	022	မ	m	ເດ
	w	00.0	2	1008	7	•	ě
	œ	0.02	9	000	9		10
	₹	90.0	3	200	'n	ŧΩ	•
	300	10.046	.5133	•10224	7,63	*	· (m
	v)	0.19	7	1031	~	ě	ີ
ALCHI ENGINE	က	in in	<b>*</b>	0491	1204	Š	S
	O i	0	80	0481	1101	oc.	
	ee (	ผู	m ÷	0489	10.6	ċ	
	36	2	m T	689	1.5	•	
	ഗ (	60	243	0489	1102	10	
	N (	2	N + 3	0486	11.5	å	n
	180	ה ה	2 4 3	€ 85	1143	10	ċ
	3 (	รูง	00 t 00	0495	14.0	•	÷
	0	22	7 7 8	9640	13.9	m	÷
	Φ	e S	230	0499	14.2	•	÷
LEFT ENGINE	m	S.	なない	0492	12:4	•	
	O N	2	ú	0488	11:1		
		S S	256	516	10.6	•	
	36	32	ŭ	334	11.5	•	
	<b>O</b>	32	លើ	0533	11.2		•
	120	9	7	23	11.5	•	•
	00	90	Ñ	22	11,3	84•3	80.0

	T ME	∢ Z ₩ • ₩ •	3 0 10 10 10	10 10 00 3	PRESSURE PSI	INLET DEG F	OUTLET DEG F
m 2 0	-	<u>П</u>					
ENG!NE	24	1 • 30	265	0528	4		0.08
	0	•30	265	528	13.9	ů	ô
	360	C	.2671	.05319	1405	<b>:</b>	Ö
е 2							
ISBLATION VALVE	m	• 70	505	032	9	ģ	•
1		•76	90	034	9	å	6
	120	6.667	• 4993	.10203	7.60	57.7	49 • 8
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	9	• •	241	9840	9 4 50	<b>‡</b>	*
LEFT ENGINE		• 32	259	0531	09 5	6	6
		.32	262	0537	12.1	6	6
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	4	21	245	0493	14.1	ċ	ò
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			* N*	43	497	07.5	ċ	ċ
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		$\infty$	• 24 4	4	498	9.80	ċ	ċ
		4	• 40	Ω.	500	0.60	ċ	ċ
		300	1.249	• 2450	• 05005	108.85	20•0	50.0
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	TIME	& & & & & & & & & & & & & & & & & & &	Η Q 10 Σ	# 0 10 ₹ 8	PAESSURE PSI	INLET	BUTLET DEG F
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EFT EN	m	ς.	247	0505	15.0	ô	ċ
		5.	241	0493	11.3	ċ	ċ
		• €	259	0529	15,0	ċ	ċ
	ũ	• 33	265	0542	11,9	ô	ô
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LEFT ENGINE		1 • 3 4 9	•2712	.05541	114.46	50.0	50•0
	9	• 33	268	0548	14.6	ċ	ô
	120	•30	262	0535	1404	•	ô
	∞	• 33	267	0545	13.8	ċ	ô
	4	• 34	270	0552	14.0	•	ô
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SULATI		•21 •21	500	1007	Š	ŏ	œ
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RIGHT ENGINE		•25	50	503	15.7	<b>.</b>	œ
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		-22	249	964	1404	•	ċ
	9	4.22°	249	4640	1346	7.	ě
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		42	46	0495	14.0	œ	00
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	4	• 25	<b>\$</b>	0497	9.60	8	ů
		1.251	• 2481	•04970	109•77	0.08	73•3
	9	• 24	248	0497	10.2	00	ໍ່
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	4	• 22	46	0495	13,3	6	-
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	9	.27	250	0509	a,	ċ	• 9
	2	15.	250	0503	9.80		00
	$\infty$	.27	250	0501	08.5	ě	ě
	4	• 25	248	0497	9 • 60	å	ě
		• 25	\$ 00	497	09.7	ċ	÷
	9	* C.	248	0497	10.2	00	ໍ
LEFT ENGINE		• 22	248	0507	16.4	<b>*</b>	·
	Q	• го	246	0501	14.0	S S	• 9
	S	• 22	546	0495	1343	•	·
	00	• 22	246	493	13.0	•	å
	4	- 22	246	0495	13,3	6	
	300	• 22	246	4640	13.3	9	•
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	$\infty$	S	9	0511	18.0	<b>‡</b>	*
	4	S	47	503	16.7	4	4
	300	m	9	504	16.0	ċ	'n
	$\infty$	m	9	502	15,0	ů	00
	0	-22	247	497	15.0	å	ō
LEFT ENGINE		• 23	50	0518	18.0	9	•
	60	ď	•2507	.05140	118.08	45.9	45.9
	N	3	50	513	17.0	S	ហ
	00	S	50	0513	18.0	<b>†</b>	*
	4	•23	251	0511	16.7	ហ្វ	4
	О	3	50	506	16.0	oo	å
	380	•23	50	503	15.0	9	œ
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